

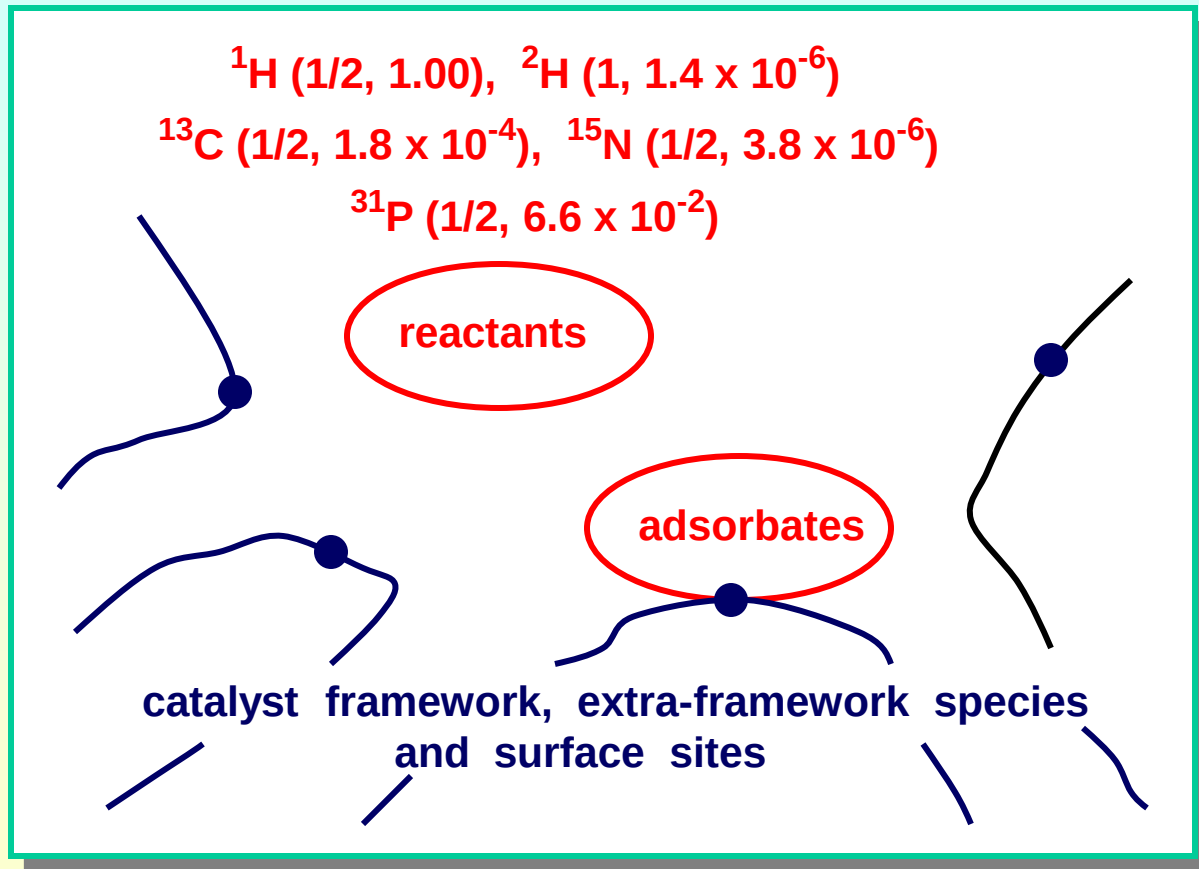
Ex Situ and In Situ Solid-State NMR Investigations of Activated Zeolite Catalysts and Heterogeneous Reaction Systems

***37th Polish Conference on Catalysis
Krakow, March 15-18, 2005***

Michael Hunger

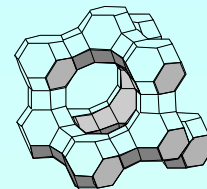
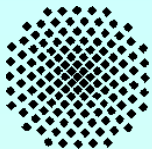
***Institute of Chemical Technology
University of Stuttgart, Germany***

Examples of Nuclei Accessible for NMR Spectroscopy



^7Li	(3/2, 0.27)
^{11}B	(3/2, 0.13)
^{17}O	(5/2, 1.1×10^{-5})
^{23}Na	(3/2, 9.2×10^{-2})
^{27}Al	(5/2, 0.21)
^{29}Si	(1/2, 3.7×10^{-4})
^{31}P	(1/2, 6.6×10^{-2})
^{51}V	(7/2, 0.38)
^{67}Zn	(5/2, 1.2×10^{-2})
^{71}Ga	(3/2, 5.6×10^{-2})
^{133}Cs	(7/2, 4.7×10^{-2})

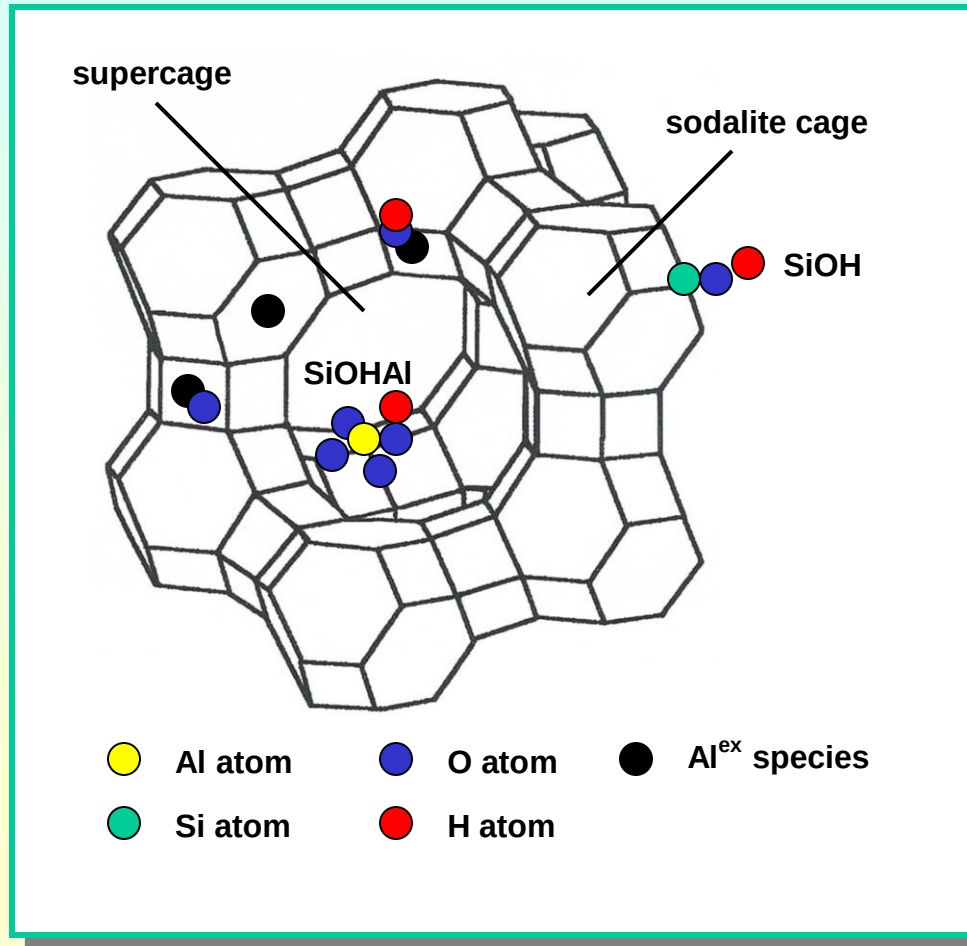
isotope (nuclear spin, relative sensitivity in comparison with ^1H)



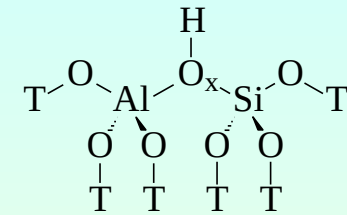
***I. NMR Investigations of
Non-Hydrated Zeolite Catalysts***

Dealumination of Zeolites

- dealuminated zeolite Y:



- Broensted-acid sites:



bridging OH group (SiOHAl)

- results of steaming:
 - dehydroxylation of SiOHAl groups
 - dealumination of the framework
 - formation of extra-framework species
 - formation of defect sites (e.g. SiOH)

NMR studies of non-hydrated zeolite catalysts:

- **possibilities and limitations of NMR spectroscopy for the study of non-hydrated solid catalysts**
- **quantitative determination of the hydroxyl coverage as a function of the steaming conditions**
- **number and coordination of framework aluminum atoms in steamed zeolite catalysts**
- **number and nature of extra-framework aluminum species in steamed zeolite catalysts**

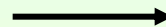
Preparation of Samples

commercial
zeolite Na-Y
($n_{\text{Si}}/n_{\text{Al}} = 2.7$)

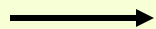
ammonium
→
exchange

NH₄-Y (exchange degree of 93 %)

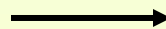
calcination and steaming at 475°C
flowing nitrogen (100 ml/min)
water vapor pressures of 3.4 to 81.5 kPa



dealuminated zeolites Y
denoted as deH-Y/ $p_{\text{H}_2\text{O}}$
 $p_{\text{H}_2\text{O}}$: water vapor pressure



transfer into gas-tight
glass tubes and
MAS NMR rotors



NMR characterization in the
non-hydrated state

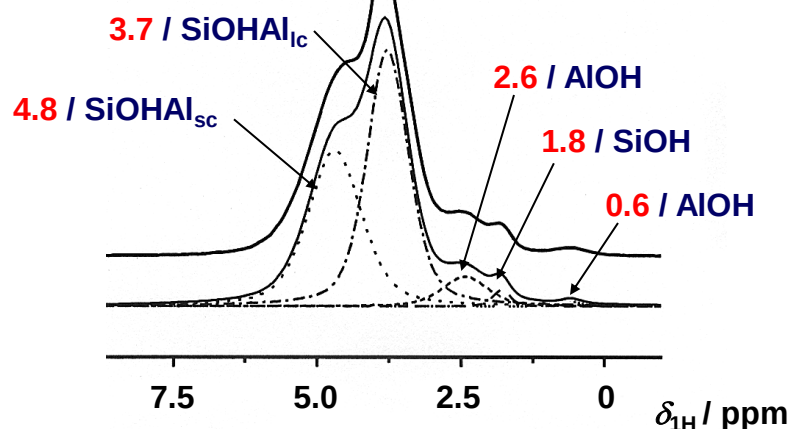
Experimental Techniques

- **AES:** Perkin Elmer Plasma 400, total numbers of atoms
- **^1H MAS NMR:** MSL 400, quantitative determination of the hydroxyl coverage
- **^{29}Si MAS NMR:** MSL 400, determination of the framework aluminum species
- **^1H and ^{27}Al CF MAS NMR:** MSL 400, adsorption of probe molecules, determination of framework aluminum species
- **^{27}Al spin-echo NMR:** MSL 400, Avance 600WB, Avance 750WB, direct characterization of framework and extra-framework aluminum species

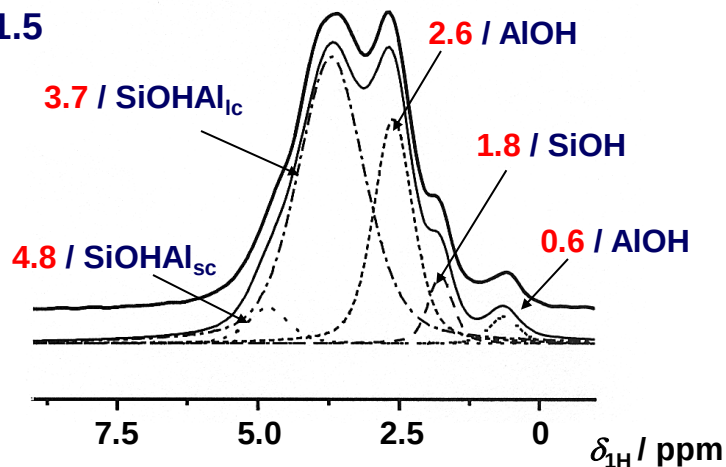
Investigation of the Hydroxyl Coverage

deH-Y/7.4

^1H MAS NMR

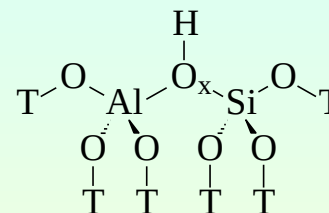


deH-Y/81.5



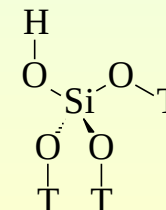
- types of hydroxyl groups:

- $\text{SiOHAl}_{\text{lc}}$: bridging OH groups in large cages (supercages)



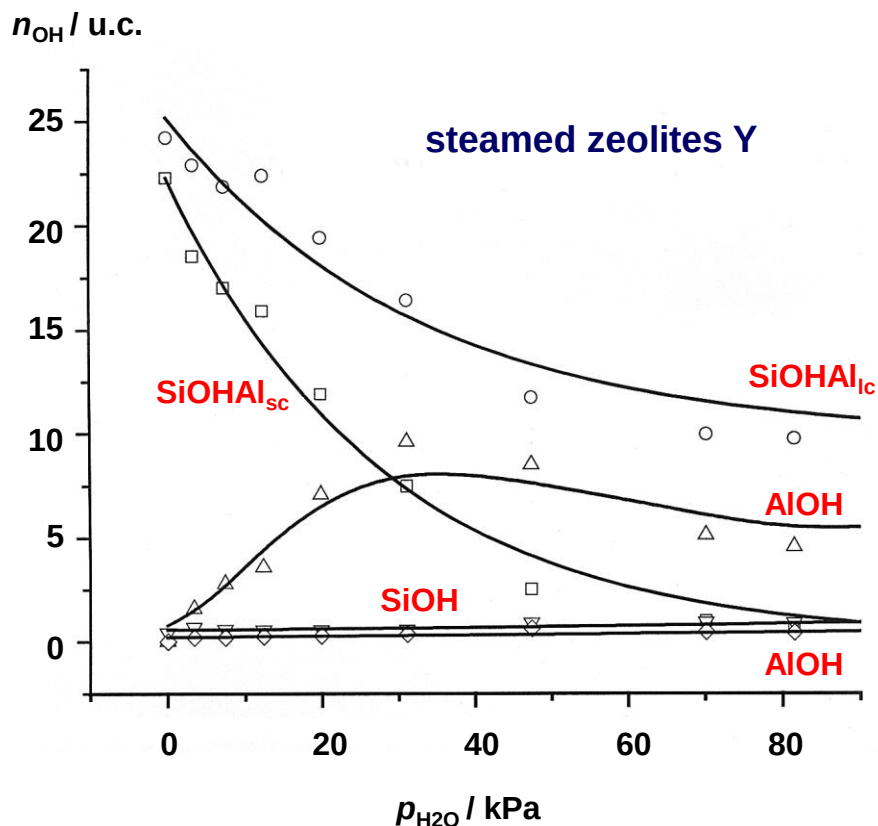
- $\text{SiOHAl}_{\text{sc}}$: bridging OH groups in sodalite cages

- SiOH : defect OH groups



- AlOH : $\text{AlO}_m(\text{OH})_n^{x+}$ species

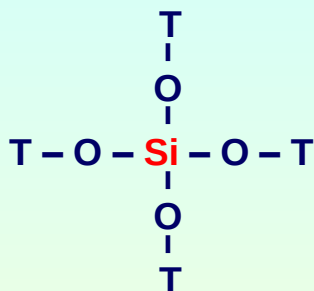
Hydroxyl Coverage as a Function of the Water Vapor Pressure



- weak steaming:
strong increase of hydrogen-bound AlOH groups at 2.6 ppm
- strong steaming:
stronger dehydroxylation of SiOHAl groups in sodalite cages than in supercages
- whole range:
only weak formation of defect SiOH groups at 1.8 ppm and AlOH groups at 0.6 ppm

Determination of the Framework Aluminum Content by ^{29}Si MAS NMR spectroscopy

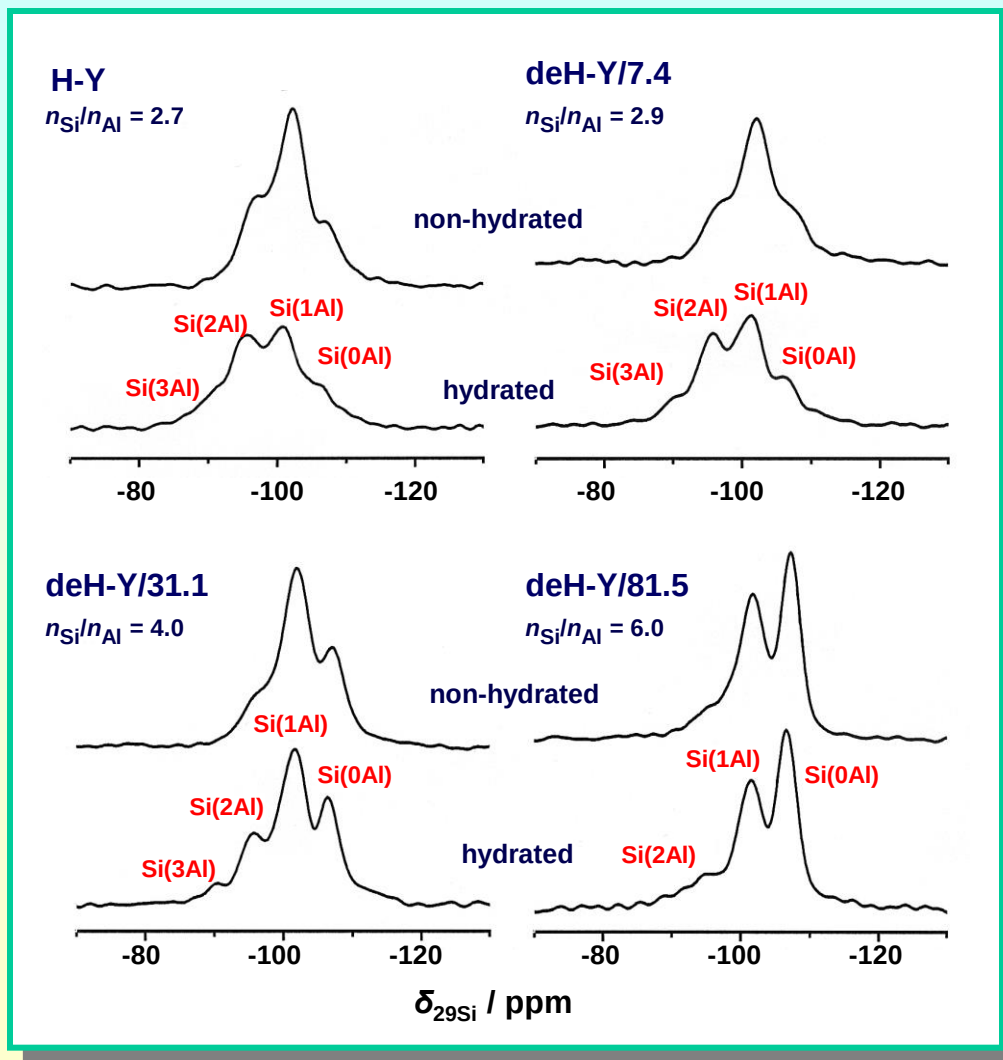
- Q⁴ silicon species:



T: Si or Al

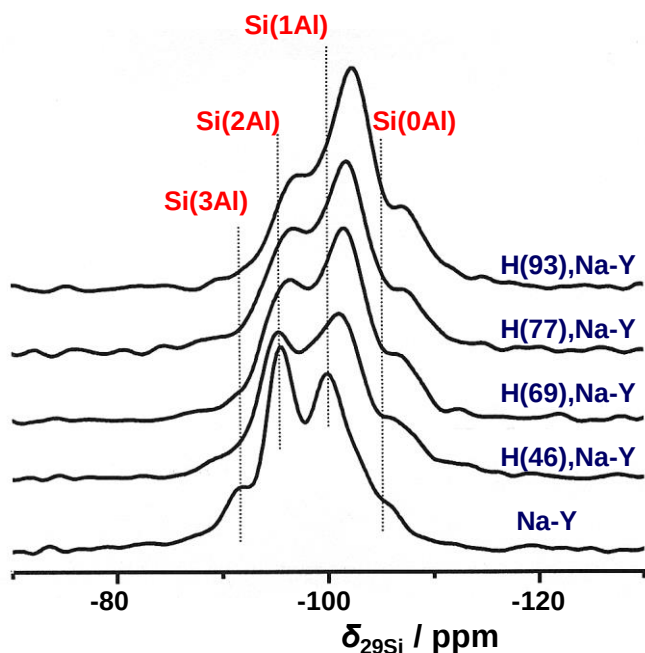
- ^{29}Si NMR signals of Q⁴ species:

-90 ppm	Si(3Al)
-95 ppm	Si(2Al)
-101 ppm	Si(1Al)
-107 ppm	Si(0Al)



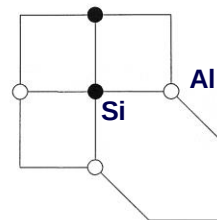
Strain of Si(*n*Al) Tetrahedra in Non-Hydrated Zeolites H,Na-Y

^{29}Si MAS NMR $n_{\text{Si}}/n_{\text{Al}} = 2.7$

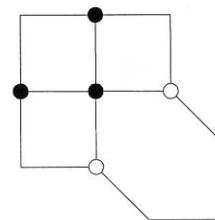


loop configuration of the FAU structure:

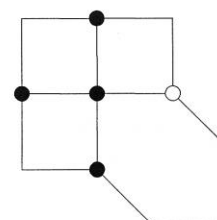
Si(3Al): $\Delta\delta_{29\text{Si}} = 5 \text{ ppm}$



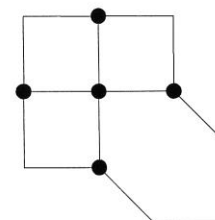
Si(2Al): $\Delta\delta_{29\text{Si}} = 2 \dots 5 \text{ ppm}$



Si(1Al): $\Delta\delta_{29\text{Si}} = 2 \text{ ppm}$



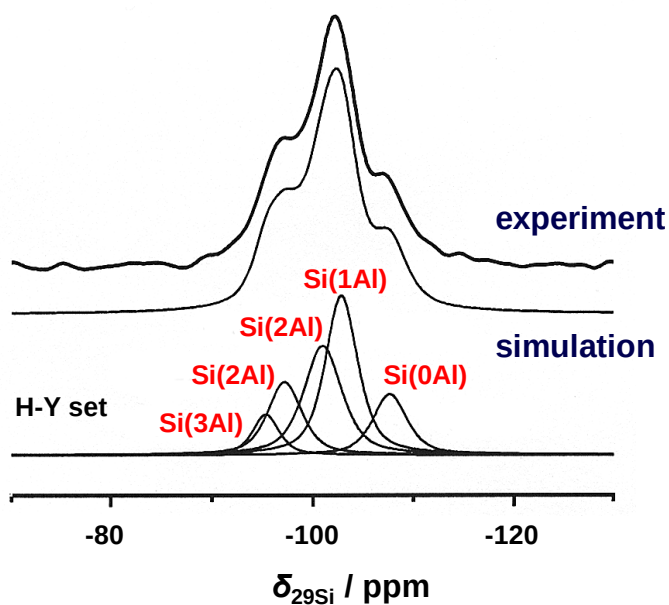
Si(0Al): $\Delta\delta_{29\text{Si}} \text{ ca. } 1 \text{ ppm}$



Simulation of ^{29}Si MAS NMR Spectra of Non-Hydrated Zeolites Y

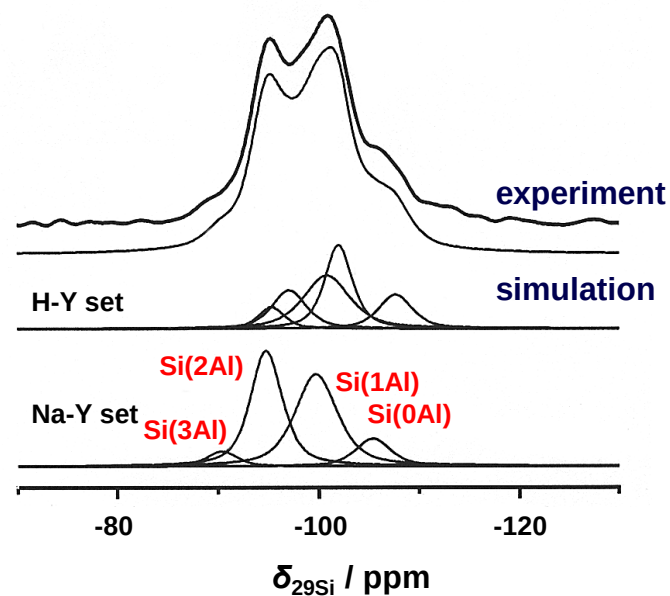
H(93),Na-Y

$n_{\text{Si}}/n_{\text{Al}} = 2.7$



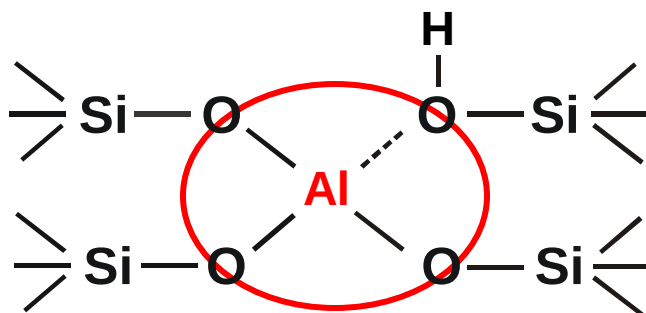
H(46),Na-Y

$n_{\text{Si}}/n_{\text{Al}} = 2.7$



Quadrupolar Interactions of Aluminum Atoms in Non-Hydrated Zeolites

^{27}Al : spin $I = 5/2$



- electric field gradient :

$$V_{zz} = eq$$

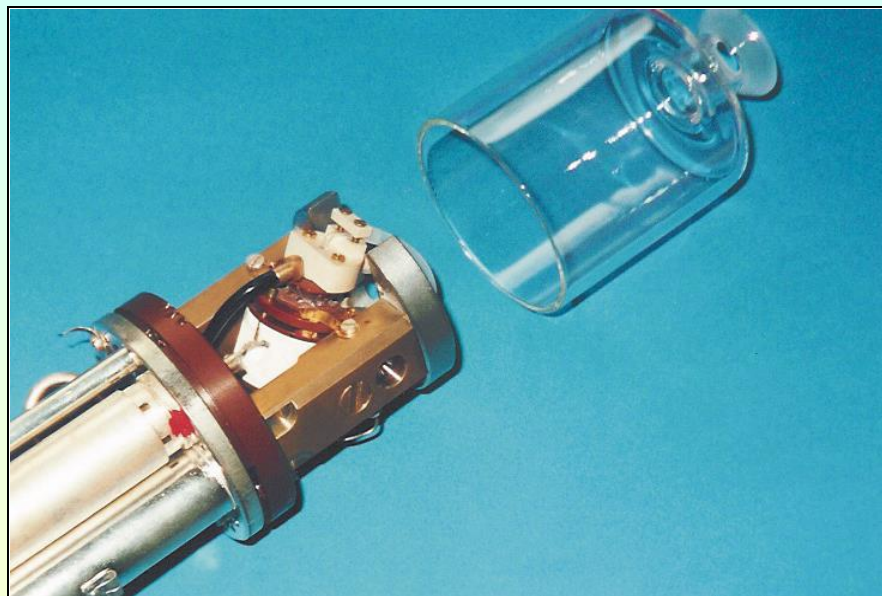
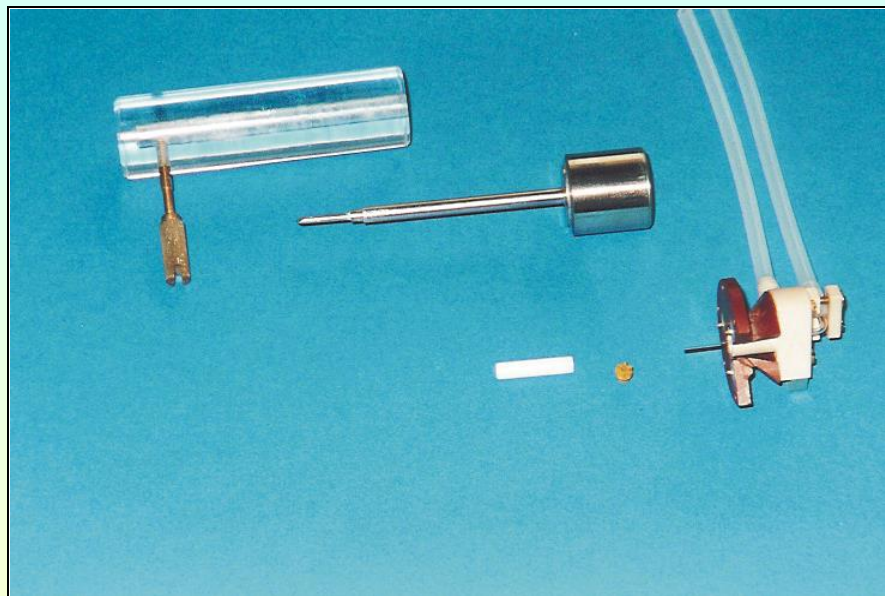
- quadrupole coupling constant:

$$QCC = \frac{e^2qQ}{h}$$

sample	QCC value	$\Delta\nu_{1/2}^{\text{MAS}^*}$
hydrated H-Y	2 MHz	0.6 kHz / 5.5 ppm
non-hydrated H-Y	15 MHz	36 kHz / 350 ppm

*) $B_0 = 9.4 \text{ T}$

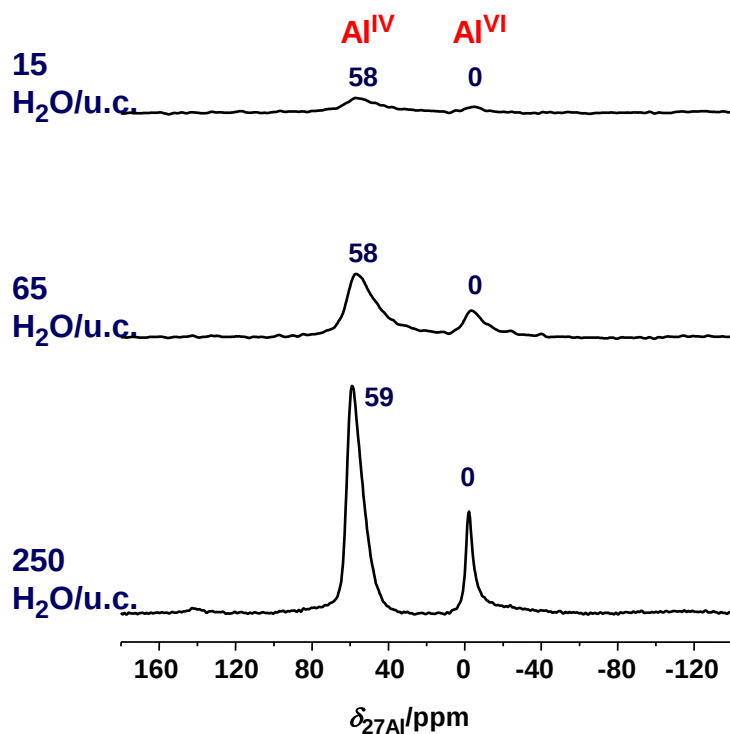
Continuous-flow (CF) MAS NMR Probe



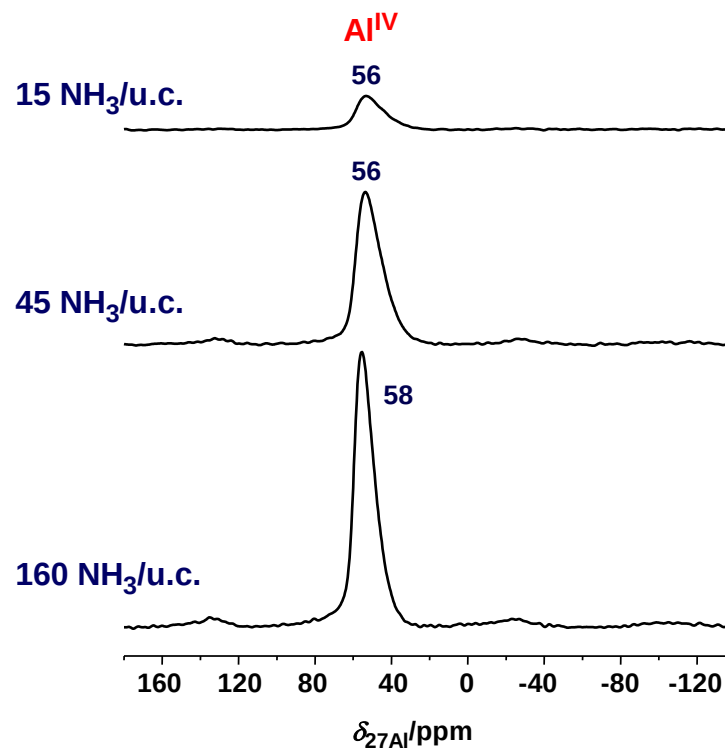
Adsorption Studied by ^{27}Al MAS NMR

- effect of the adsorption of H_2O and NH_3 on Al species in non-hydrated H-Y ($n_{\text{Si}}/n_{\text{Al}} = 2.7$)

^{27}Al MAS NMR difference spectra



^{27}Al MAS NMR difference spectra



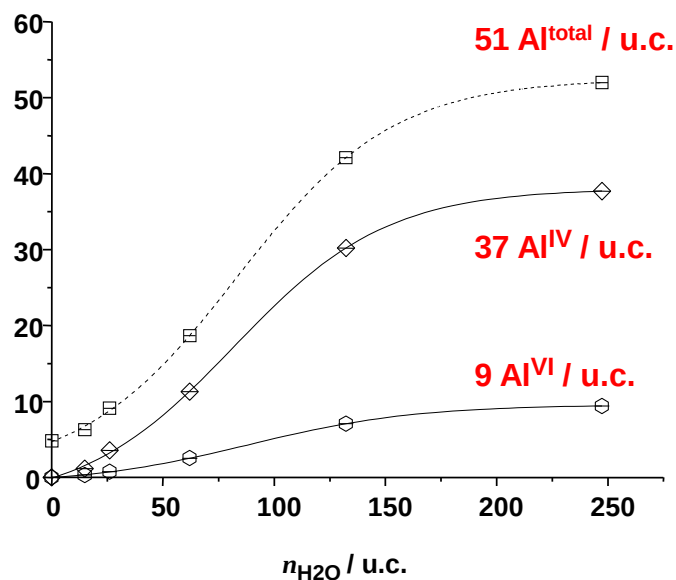
Adsorption Studied by ^{27}Al MAS NMR

- evaluation of the adsorption of H_2O and NH_3 on non-hydrated H-Y (52.0 $\text{Al}^{\text{IV}}/\text{u.c.}$)

adsorption of H_2O

^{27}Al MAS NMR

$n_{\text{Al}} / \text{u.c.}$

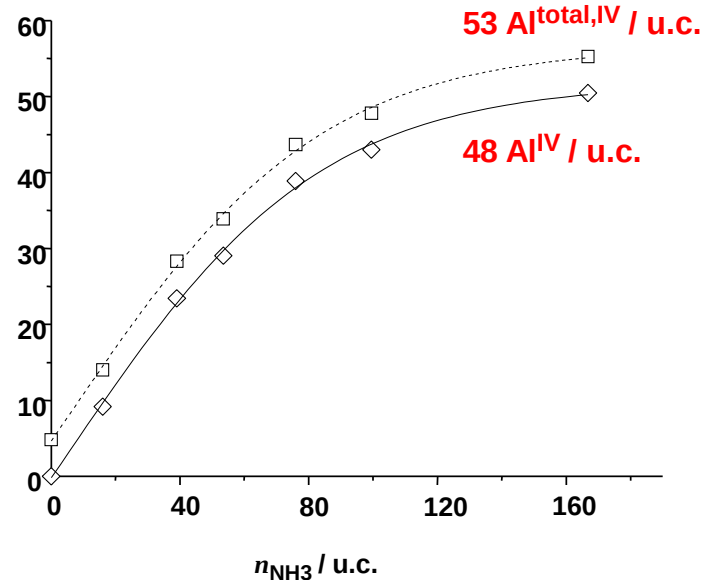


^1H MAS NMR

adsorption of NH_3

^{27}Al MAS NMR

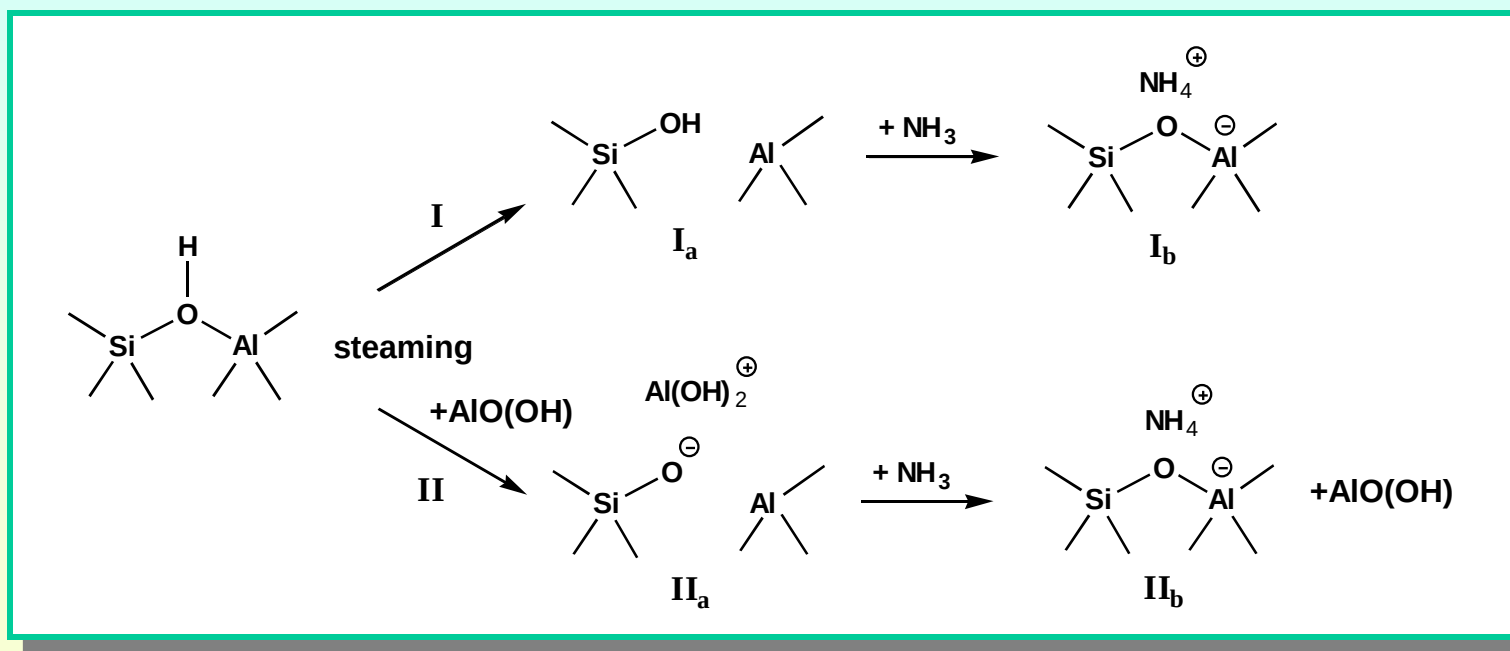
$n_{\text{Al}} / \text{u.c.}$



^1H MAS NMR

Reversible Coordination Change of Framework Aluminum Atoms

- proposed mechanism:

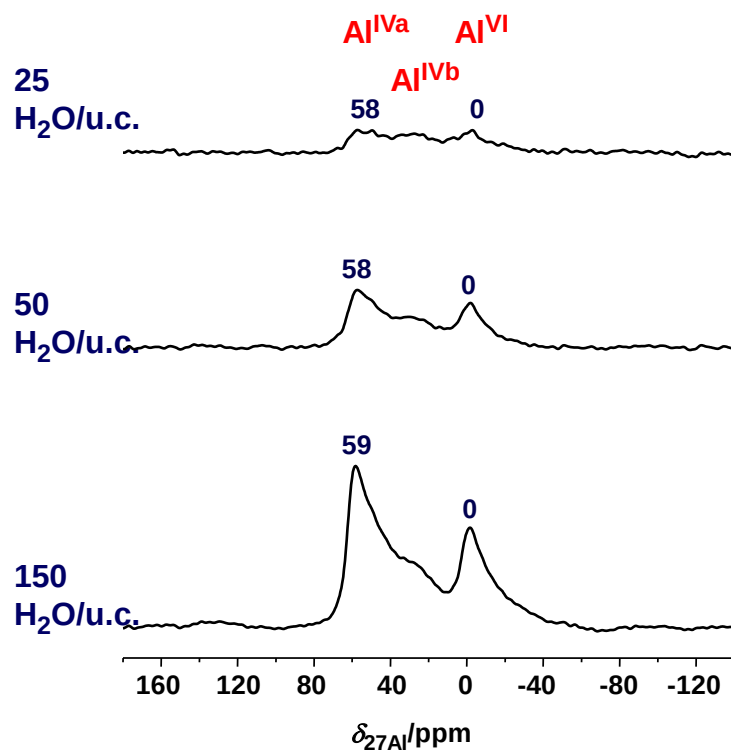


→ adsorption of ammonia transforms Al atoms at framework defects into tetrahedrally coordinated Al atoms

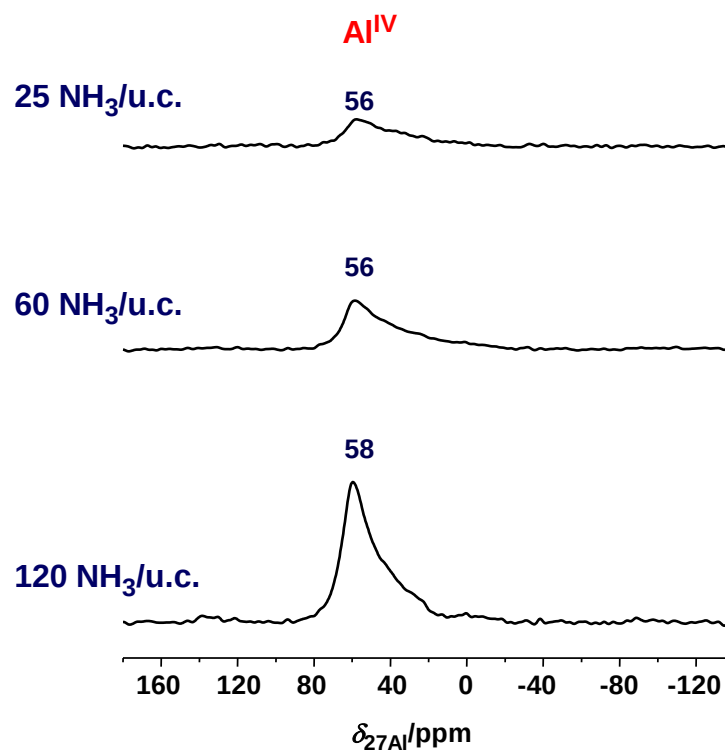
Adsorption Studied by ^{27}Al MAS NMR

- adsorption of H_2O and NH_3 on Al species in dehydrated zeolite deH-Y/81.5 ($n_{\text{Si}}/n_{\text{Al}} = 6.0$)

^{27}Al MAS NMR difference spectra



^{27}Al MAS NMR difference spectra



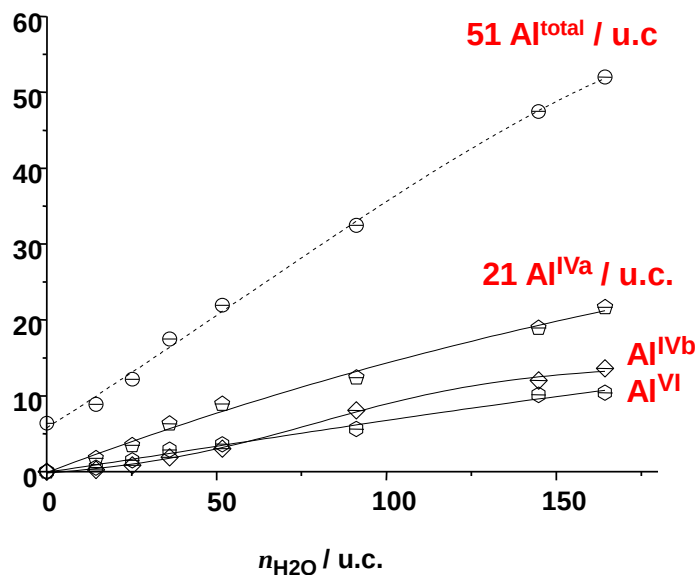
Adsorption Studied by ^{27}Al MAS NMR

- evaluation of the adsorption of NH_3 and H_2O on non-hydrated deH-Y/81.5 (27.4 Al^{IV} /u.c.)

adsorption of H_2O

^{27}Al MAS NMR

$n_{\text{Al}} / \text{u.c.}$

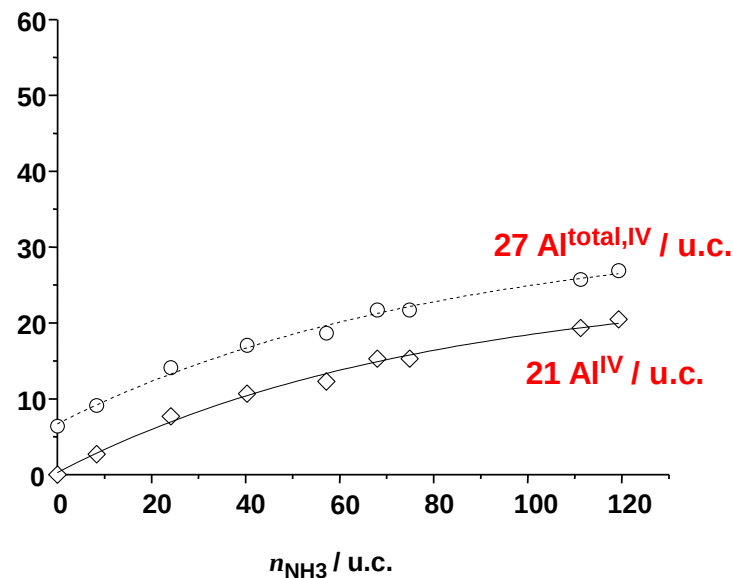


^1H MAS NMR

adsorption of NH_3

^{27}Al MAS NMR

$n_{\text{Al}} / \text{u.c.}$



^1H MAS NMR

Mean Cationic Charge of Extra-Framework Aluminum Species

- effect of steaming on zeolite H-Y (3.5 residual sodium cations per u.c.)

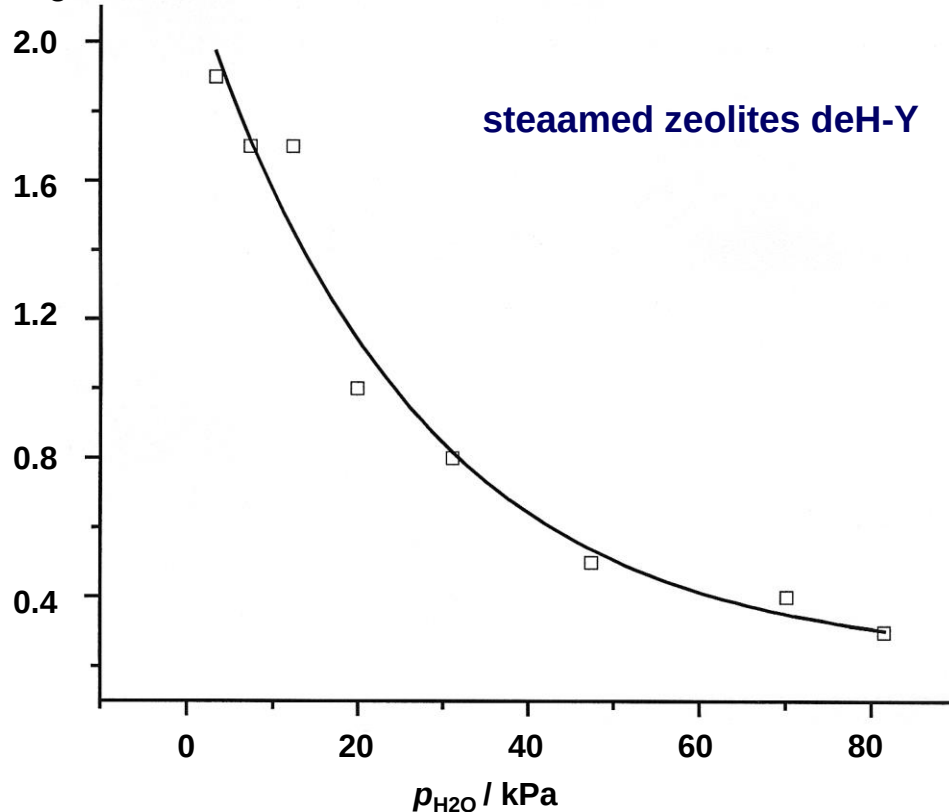
sample	$n_{\text{Si}}/n_{\text{Al}}$	$n_{\text{Al}^{\text{IV}}} / \text{u.c.}$	$n_{\text{SiOHAl}} / \text{u.c.}$	$n_{\text{Al}^{\text{ex}}} / \text{u.c.}$	x
H-Y	2.7	52.0	46.5	0	0
deH-Y/3.4	2.8	50.1	43.0	1.9	1.9+
deH-Y/7.4	2.9	48.6	39.2	3.4	1.7+
deH-Y/19.9	3.3	44.6	34.4	7.4	1.0+
deH-Y/31.1	4.0	38.4	25.7	13.6	0.7+
deH-Y/81.5	6.0	27.4	17.3	24.6	0.3+

- mean charge per extra-framework aluminum atom in non-hydrated zeolites deH-Y:

$$x = (n_{\text{Al}^{\text{IV}}} - n_{\text{Na}} - n_{\text{SiOHAl}}) / n_{\text{Al}^{\text{ex}}}$$

Mean Cationic Charge of Extra-Framework Aluminum Species

mean cationic
charge x



→ formation of:



- value x :
ca. 2 to $0.3/\text{Al}^{\text{ex}}$

- value n :
1.0 to $0.25/\text{Al}^{\text{ex}}$

→ weak steaming:

- species with mean
cationic charge of ca. 2+

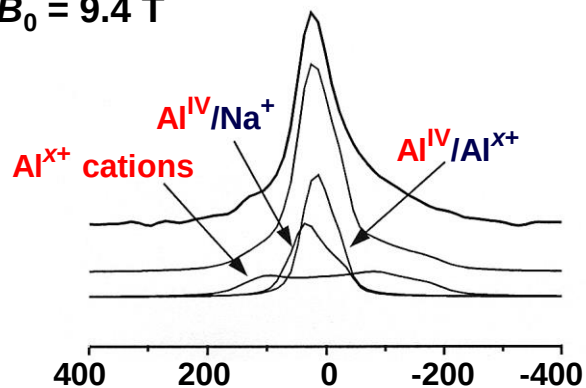
strong steaming:

- mixture of different
species

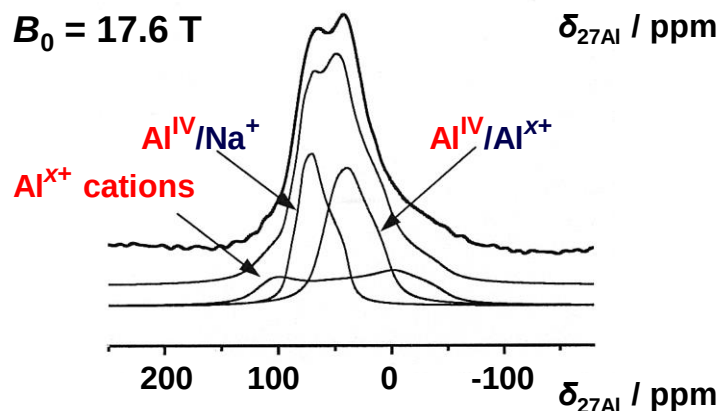
^{27}Al Spin-Echo NMR Studies of Reference Materials

Al,Na-Y

$B_0 = 9.4 \text{ T}$

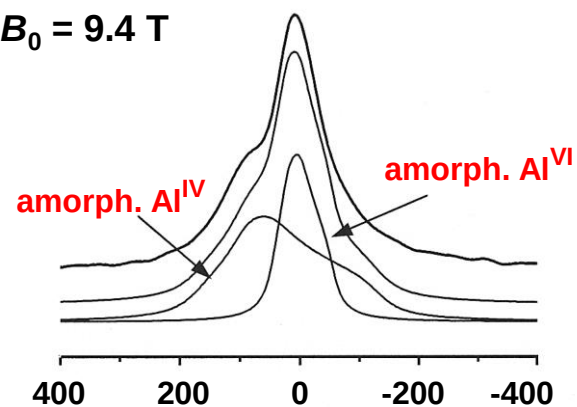


$B_0 = 17.6 \text{ T}$

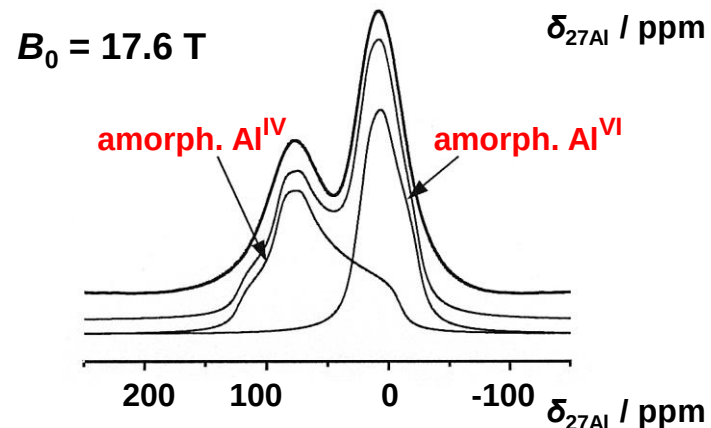


$\gamma\text{-Al}_2\text{O}_3$

$B_0 = 9.4 \text{ T}$



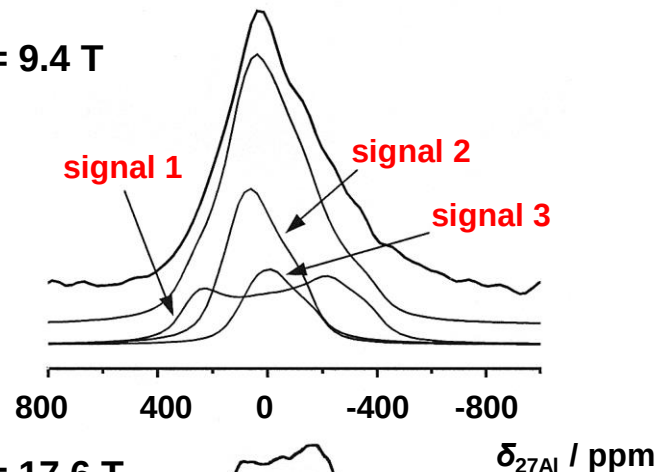
$B_0 = 17.6 \text{ T}$



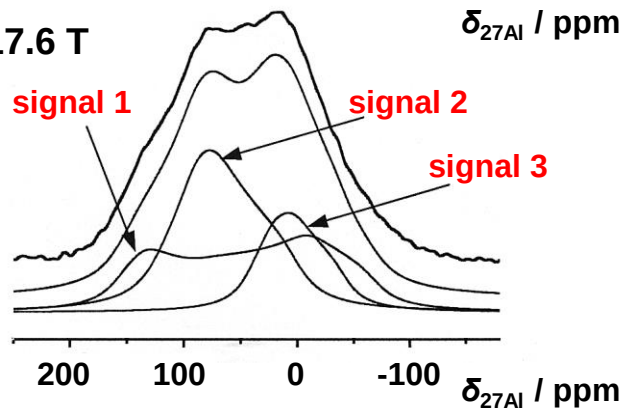
^{27}Al Spin-Echo NMR Studies of Strongly Steamed Zeolite Y

deH-Y/81.5

$B_0 = 9.4 \text{ T}$



$B_0 = 17.6 \text{ T}$

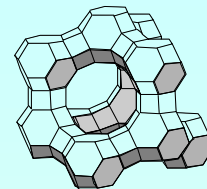
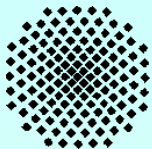


- signal 1:
 - QCC = 14.8 MHz, $\eta = 0.3$, $\delta_{\text{iso}} = 65 \pm 5 \text{ ppm}$
 - signals of $\text{Al}^{\text{IV}}/\text{H}^+$ and $\text{Al}^{\text{x+}}$ cations
 - signal 2:
 - QCC = 9.0 MHz, $\eta = 0.8$, $\delta_{\text{iso}} = 65 \pm 5 \text{ ppm}$
 - signals of $\text{Al}^{\text{IV}}/\text{Na}^+$, $\text{Al}^{\text{IV}}/\text{Al}^{\text{x+}}$, and amorph. Al^{IV}
 - signal 3:
 - QCC = 8.0 MHz, $\eta = 0.7$, $\delta_{\text{iso}} = 5 \pm 5 \text{ ppm}$
 - signal of amorph. Al^{VI}
- zeolite deH-Y/81.5 contains:
- 8 amorph. Al^{IV} per u.c.
 - 10 amorph. Al^{VI} per u.c.
 - 4.5 $\text{Al}^{\text{x+}}$ cations per u.c., $\text{Al}(\text{OH})^{2+}$

Summary I

Study of steamed zeolites Y in the non-hydrated state:

- ^1H MAS NMR:
 - preferred dehydroxylation of bridging OH groups in the sodalite cages
- ^{29}Si MAS NMR, ^1H MAS NMR, and AES:
 - formation of Al^{ex} species with a *mean* cationic charge of ca. 2+ for weakly steamed materials and 0.3+ for strongly steamed materials
- ^{27}Al MAS NMR studies of the adsorption of water and ammonia:
 - quantitative determination of the number of framework Al^{IV} species
 - Al^{VI} species in rehydrated zeolite H-Y may be due to framework aluminum atoms at defect sites
- ^{27}Al spin-echo NMR, ^1H MAS NMR, and AES:
 - Al^{ex} species in strongly steamed zeolites Y are a mixture of tetrahedrally and octahedrally coordinated Al atoms in oxidic clusters and $\text{Al}(\text{OH})^{2+}$ cations

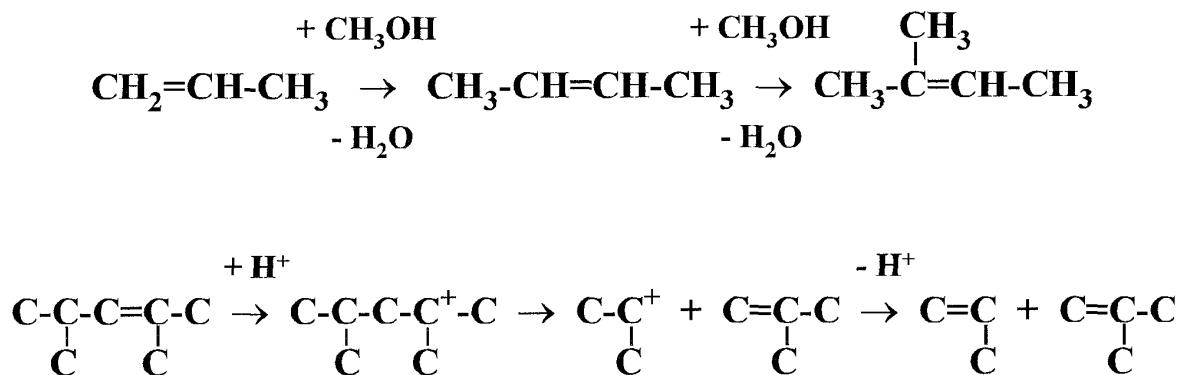


***II. NMR Investigations of the
Methanol to Hydrocarbon Conversion
on Acidic Zeolite Catalysts***

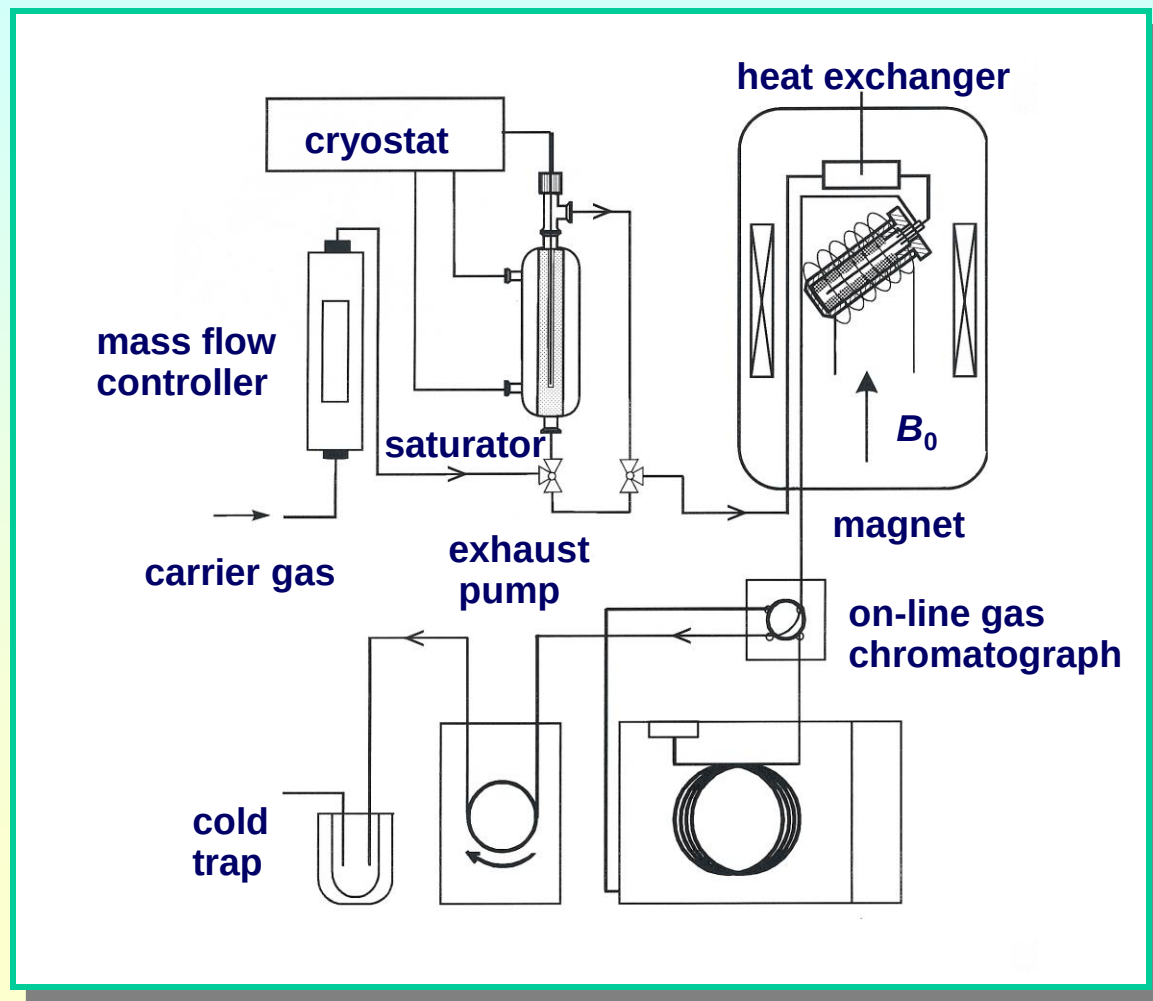
Methanol to Olefin (MTO) Conversion on Acidic Zeolite Catalysts

reaction mechanisms proposed in the literature:

- carbene mechanism (Swabb and Gates)
- oxonium ylide mechanism (Berg and Olah)
- carbon-pool mechanism (Haag, Hoelderich, Kolboe)



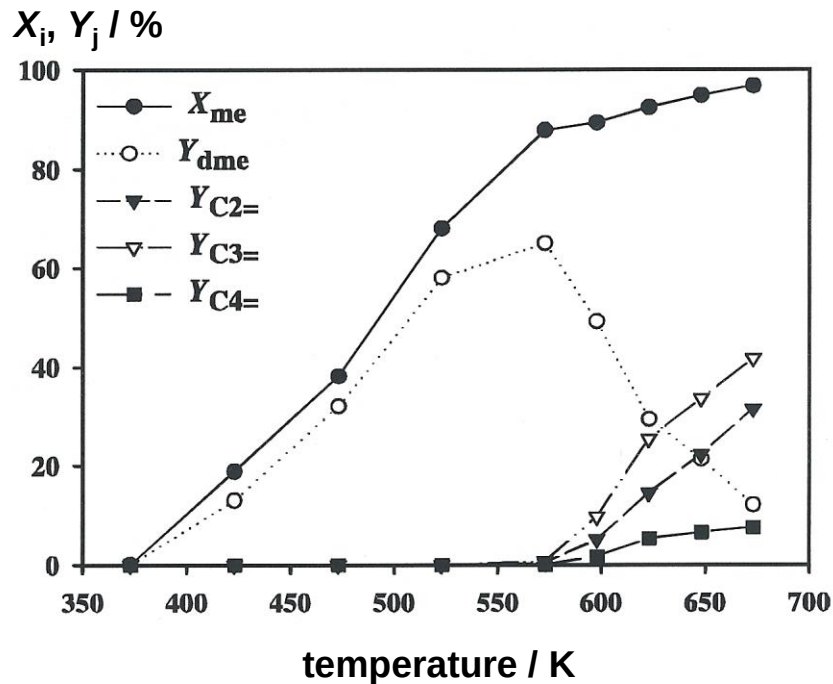
Coupling of In Situ CF MAS NMR and On-Line Gas Chromatography



Conversion of Methanol on H-ZSM-5 in a Fixed-Bed and in an MAS NMR Rotor Reactor

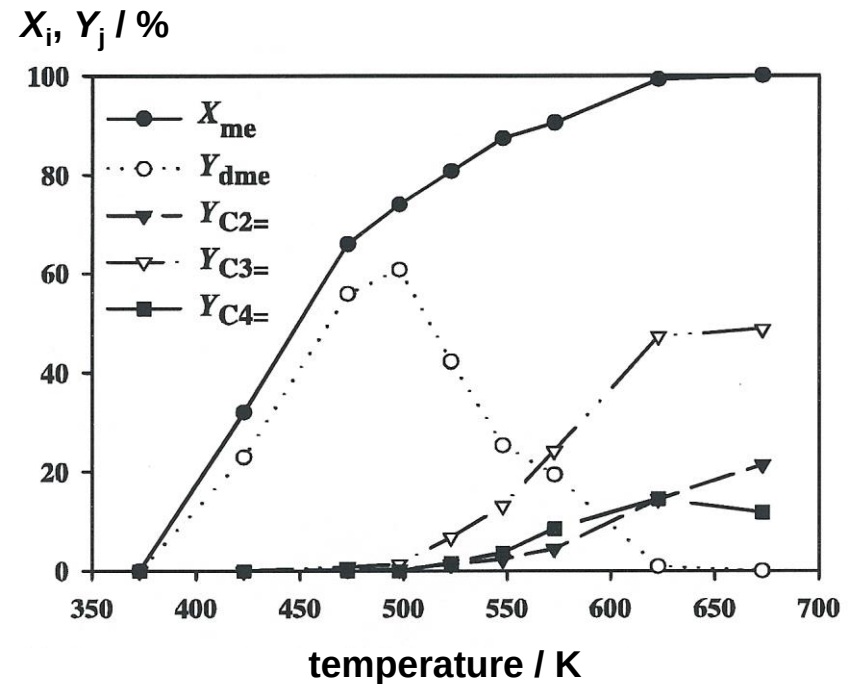
fixed-bed reactor

$W_{\text{cat}}/F_{\text{me}} = 25 \text{ gh/mol}$

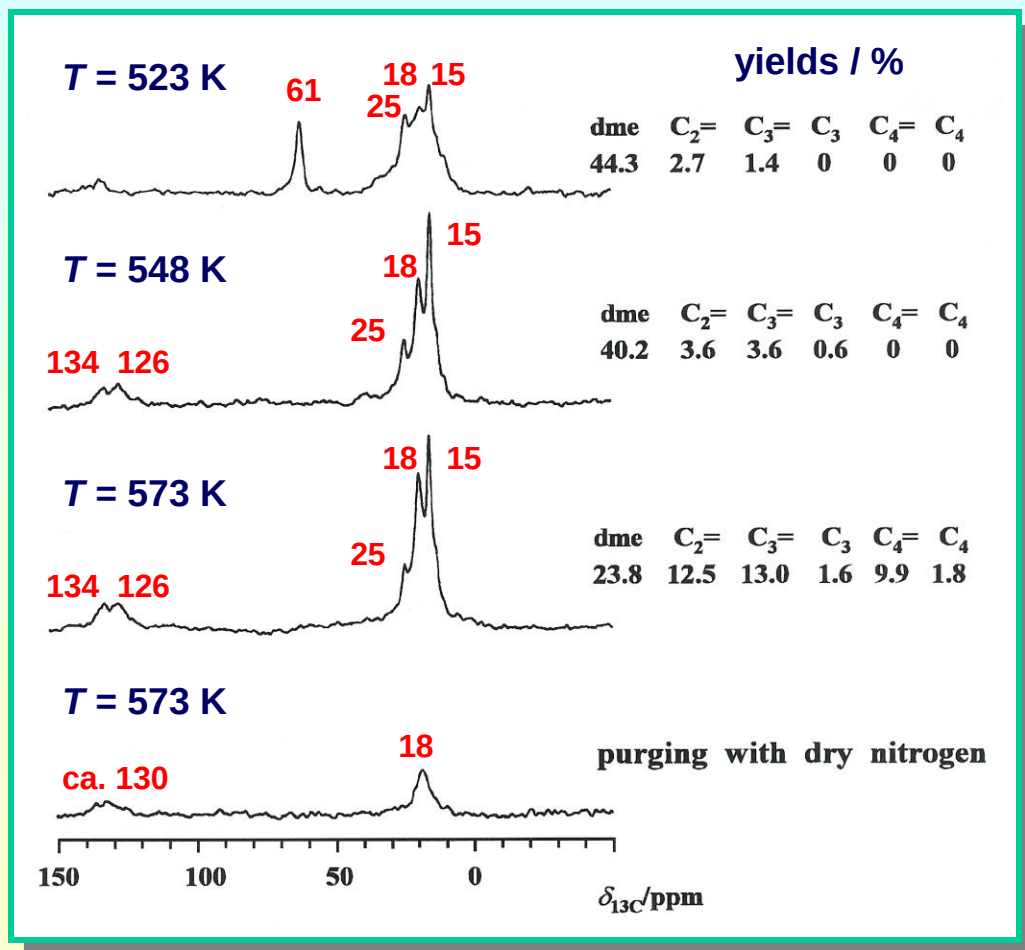


spinning (2 kHz) MAS NMR rotor reactor

$W_{\text{cat}}/F_{\text{me}} = 25 \text{ gh/mol}$

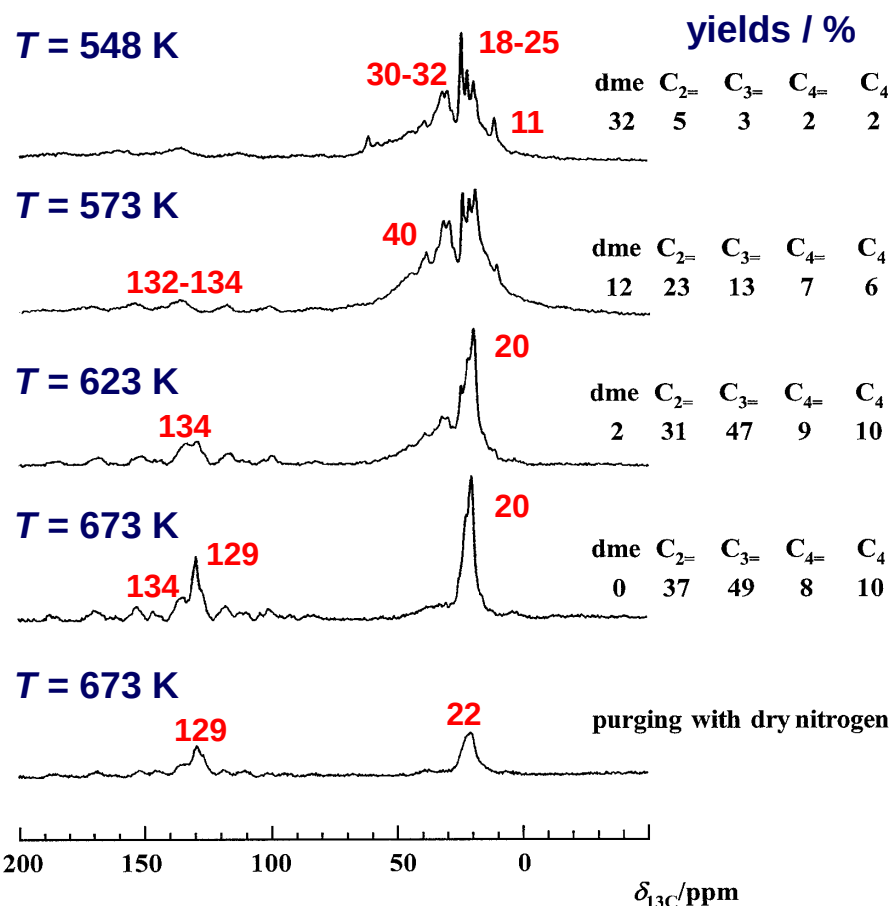


Conversion of Methanol on H-ZSM-5 Studied by In Situ ^{13}C CP MAS NMR



- olefinic deposits, e.g.:
3-hexene (14.4, 25.9, 131.2 ppm)
2,3-hexadiene (17.5, 126.2, 132.5 ppm)
....
- mixture of olefins with carbon numbers of $n > 6$
- domination of aromatics after purging with dry nitrogen:
benzene (128.6 ppm)
....
hexamethylbenzene (17.6, 132.1 ppm)

Conversion of Methanol on H-SAPO-34 Studied by In Situ ^{13}C CF MAS NMR



$T < 623 \text{ K}$:

→ mixture of olefinic compounds:
 3-hexene (14.4, 25.9, 131.2 ppm)
 2,3-hexadiene (17.5, 126.2,
 132.5 ppm)

....

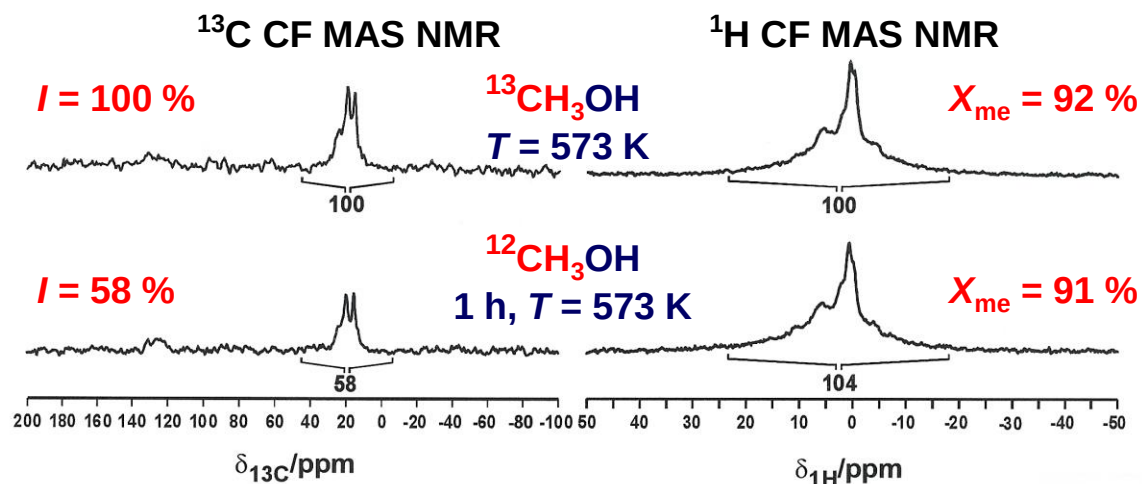
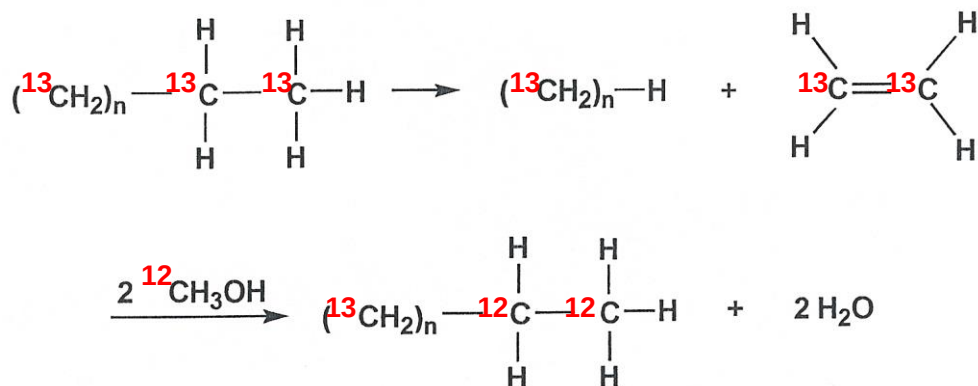
$T > 623 \text{ K}$:

→ domination of aromatic compounds:
 benzene (128.6 ppm)
 toluene (20.3, 128.5, 129.0 ppm)

....

tetramethylbenzene (18.9, 131.1,
 134 ppm)
 hexamethylbenzene (17.6,
 132.1 ppm)

Role of the Carbon Pool in the MTO Process on H-ZSM-5

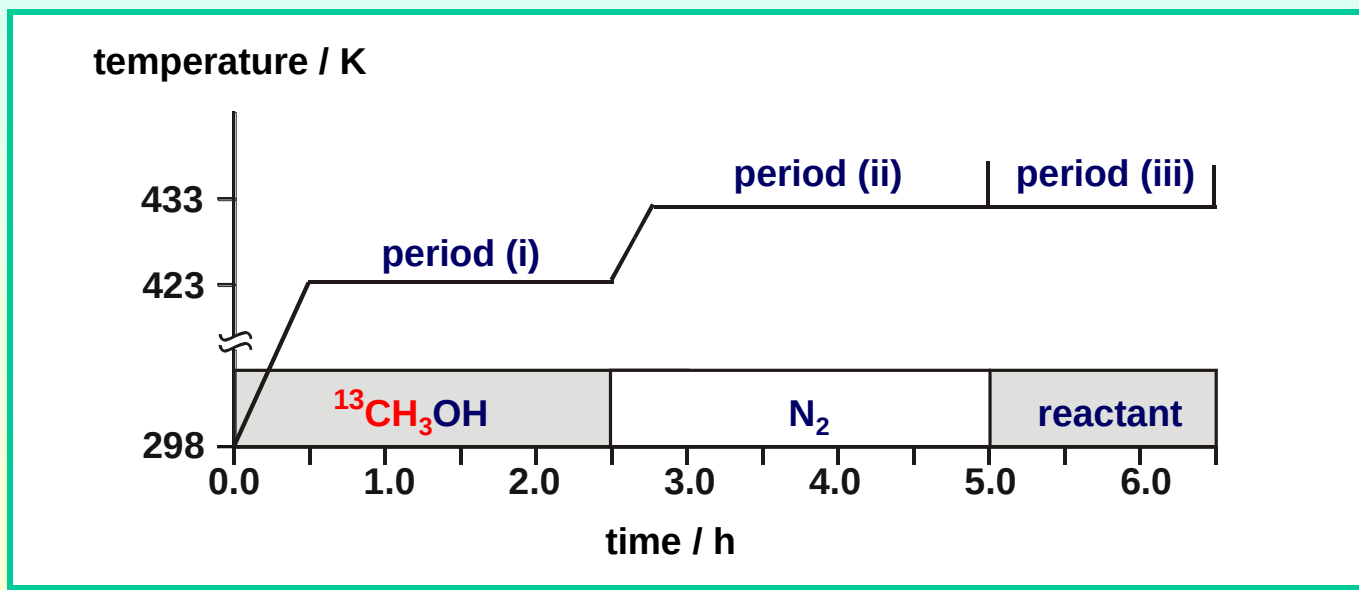


switching of the reactant flow induces a decrease of the ^{13}C -isotopes in the alkyl groups:

- alkyl groups are involved in the conversion of methanol
- the carbon pool plays an active role in the MTO process

Study of Surface Methoxy Groups by In Situ SF (Stopped-Flow) MAS NMR

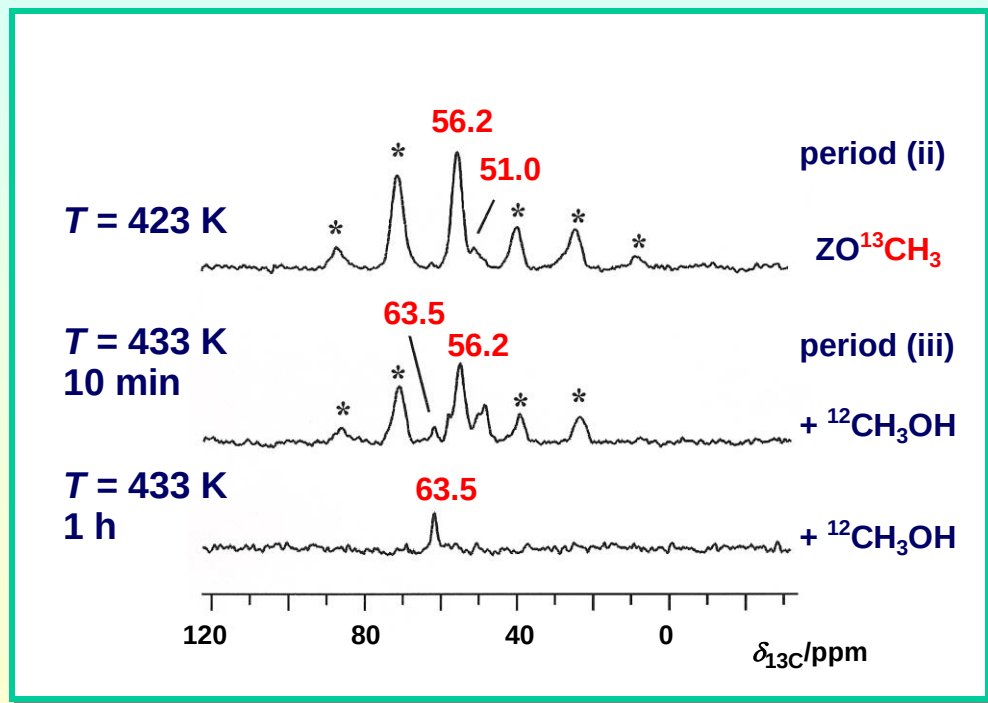
selective preparation of adsorbate complexes by purging the volatile reactants in period (ii) and study of their further reaction in period (iii)



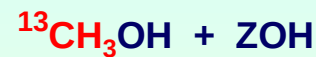
investigation of the reactivity of intermediates

Reaction of Methoxy Groups with Methanol on Acidic Zeolites

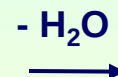
^{13}C SF MAS NMR investigation of methoxy groups on zeolite H-Y



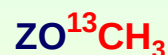
methanol



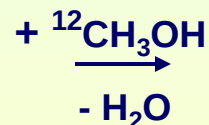
49.0 ppm



methoxy



56.2 ppm



dme

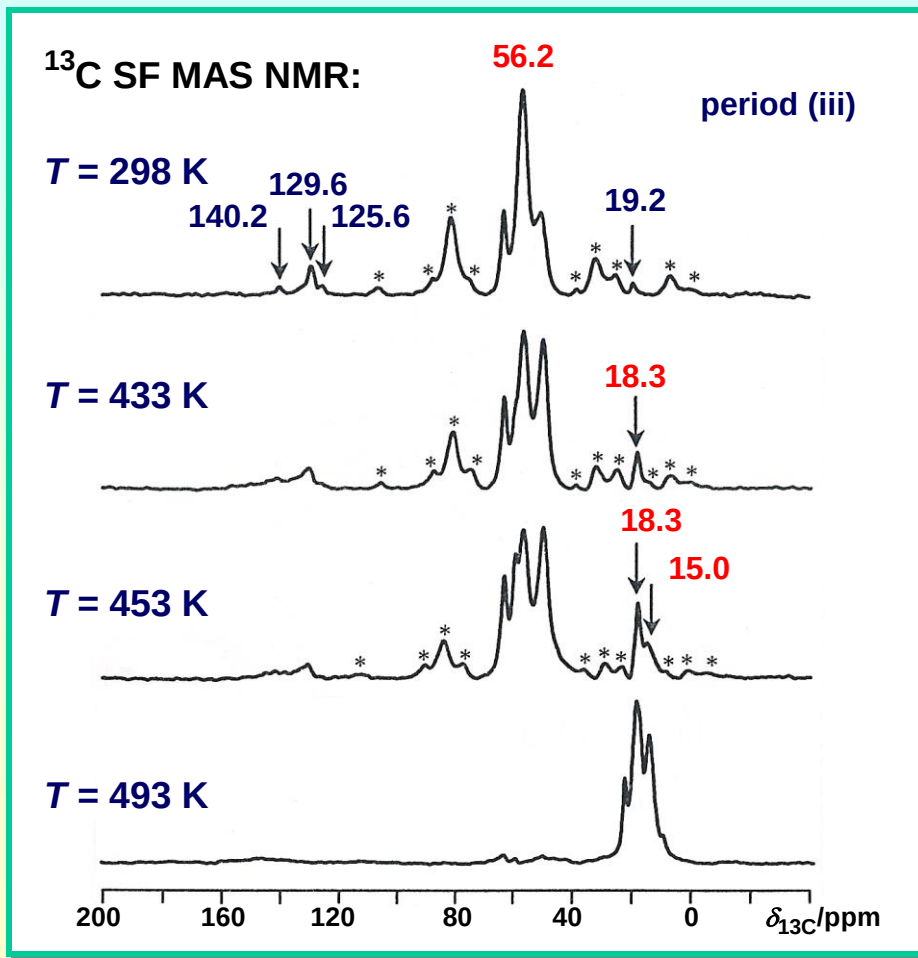


63.5 ppm

→ ^{13}C -labelled methoxy groups contribute to the formation of dimethyl ether

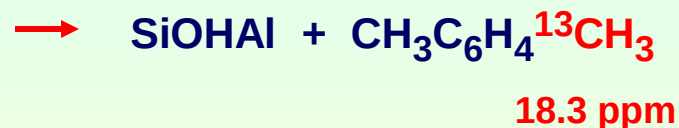
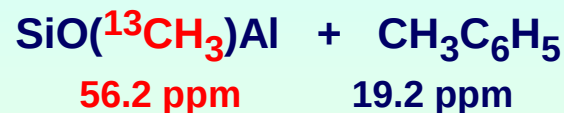
Methylation of Aromatics by Surface Methoxy Groups

reaction of methoxy groups with toluene on zeolite H-Y



methoxy

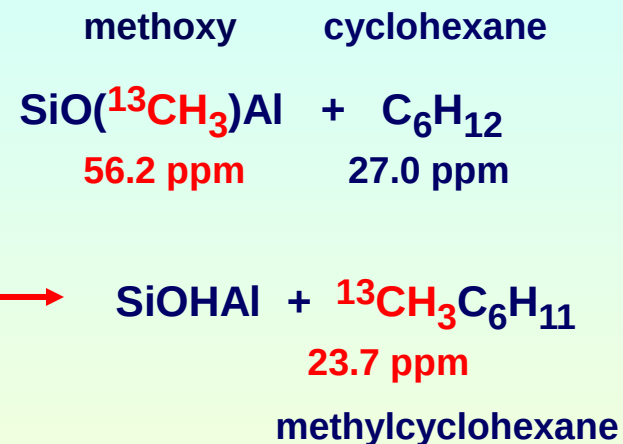
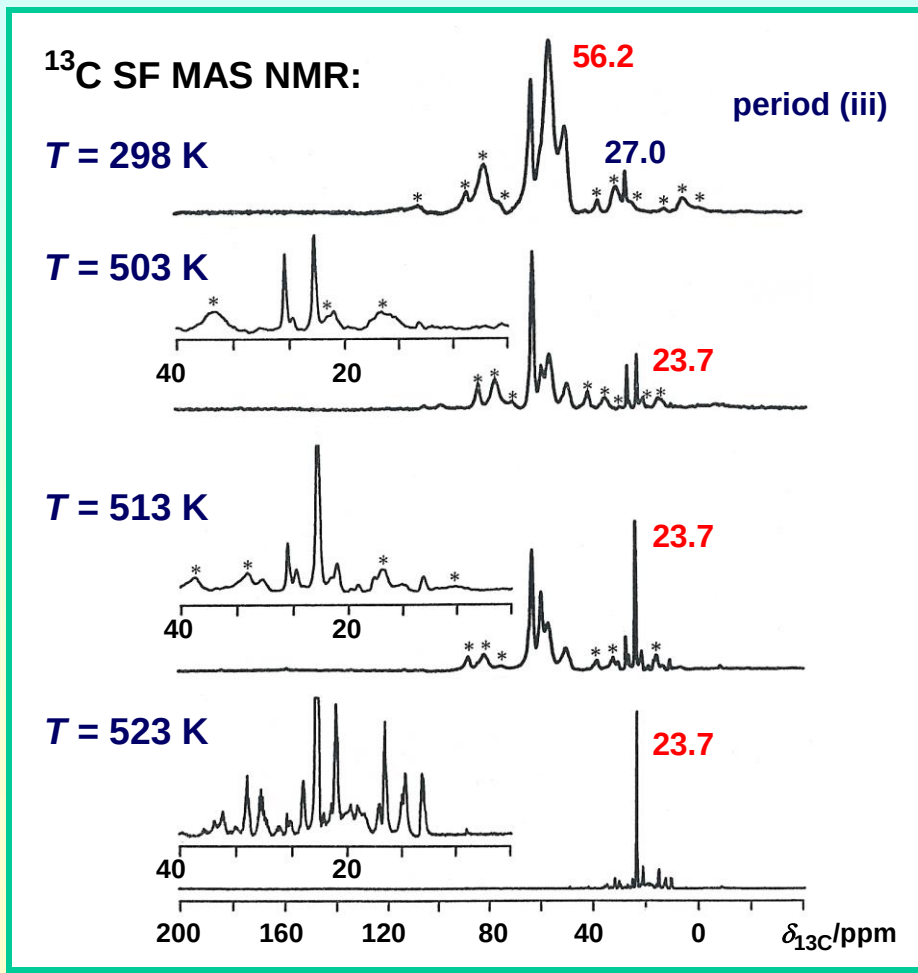
toluene



- methylation of aromatics by surface methoxy groups starts at $T = 433\text{ K}$

Methylation of Alkanes by Surface Methoxy Groups

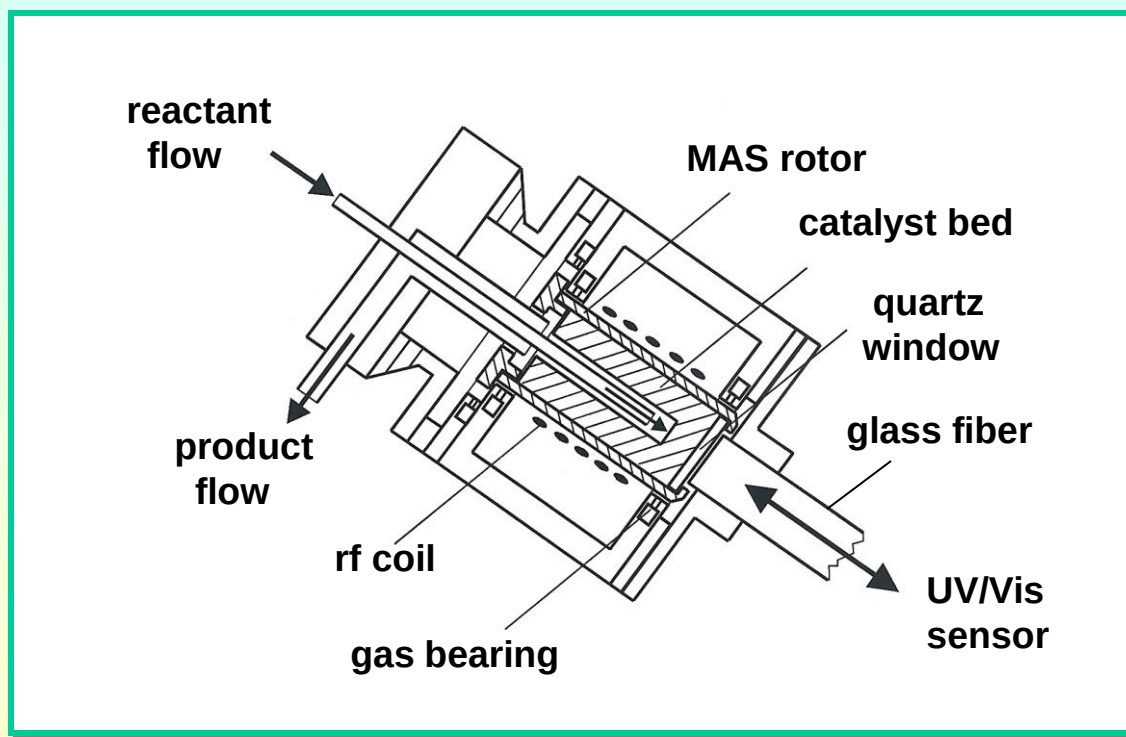
reaction of methoxy groups with cyclohexane on zeolite H-Y



- methylation of alkanes by surface methoxy groups starts at $T = 503 \text{ K}$
- intermediates of ylide or carbene nature

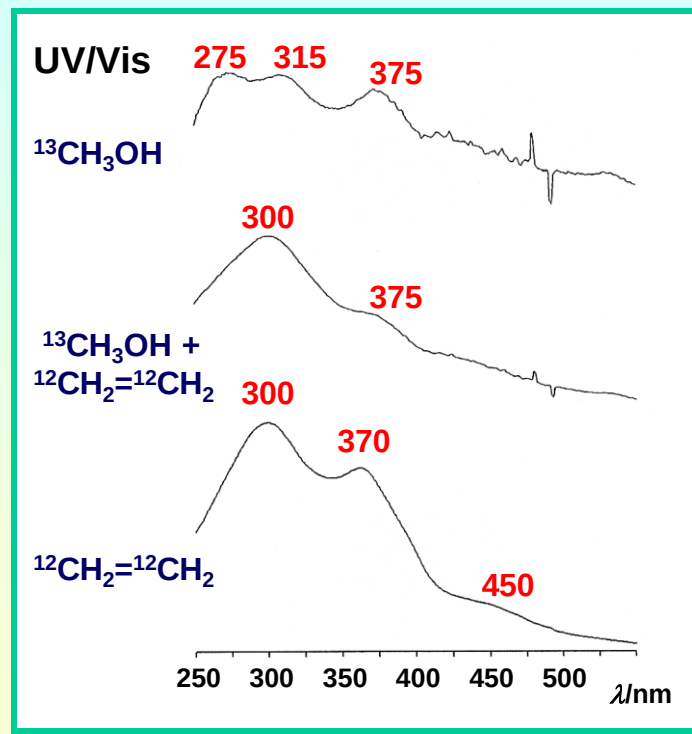
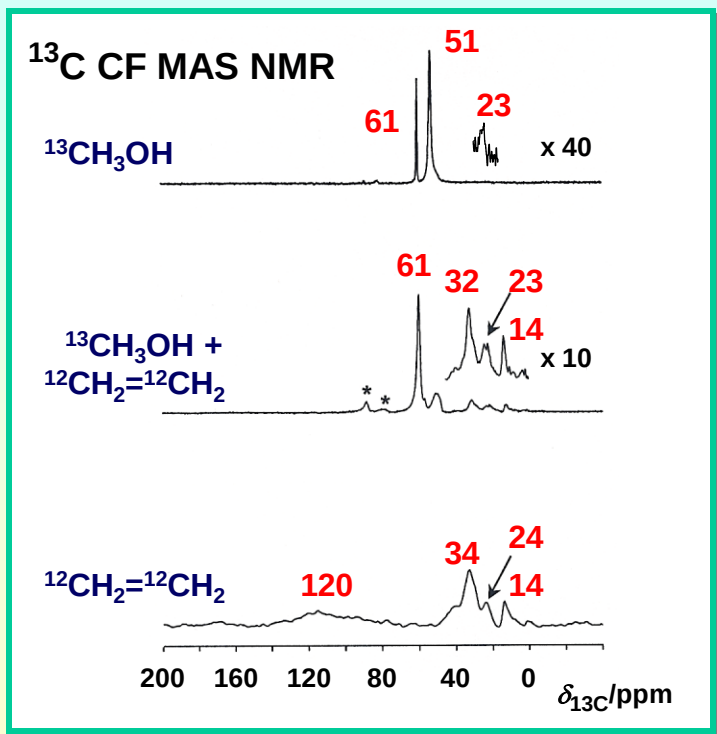
MAS NMR-UV/Vis Coupling

installation of a quartz fiber optic at the bottom of the CF MAS NMR stator



MAS NMR-UV/Vis Coupling

conversion of $^{13}\text{CH}_3\text{OH}$ on dealuminated H-ZSM-5 at 423 K

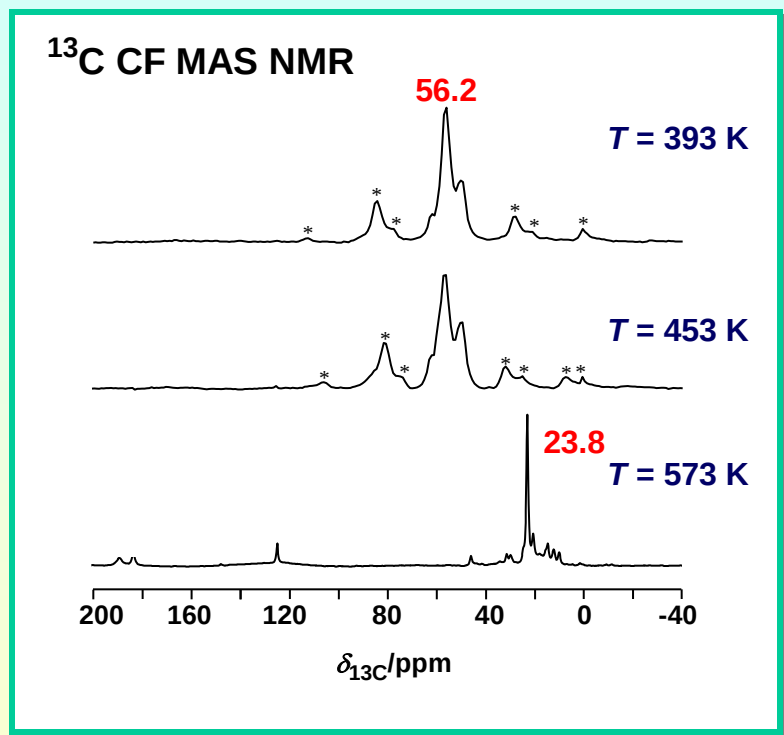


→ **275 nm:** neutral aromatics
315 nm: monoenyl carbenium ions

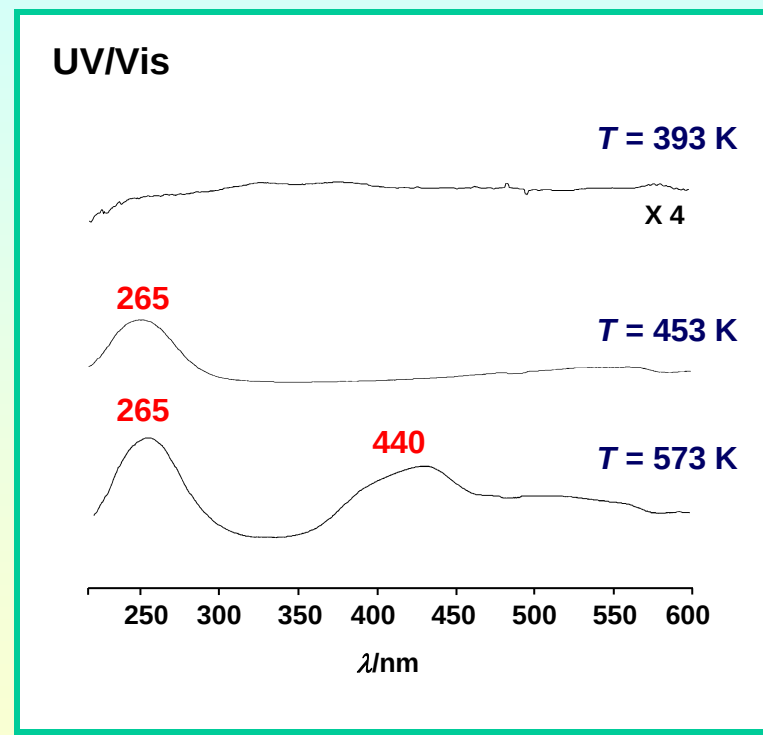
375 nm: dienyl carbenium ions
450 nm: polyaromatics

MAS NMR-UV/Vis Coupling

conversion of surface methoxy groups on zeolite H-Y



→ 23.8 ppm: isobutane
ca. 130 ppm: aromatics



265 nm: neutral aromatics
440 nm: polyaromatics,
trienylcarbenium ions

Summary II

Study of the methanol-to-olefin conversion on acidic zeolites:

- **under steady-state conditions, mixtures of polyalkylated olefins and aromatics are formed in the zeolite pores**
- **composition of this carbon pool depends on the reaction conditions and on the catalyst**
- **alkyl groups of the carbon pool contribute to the conversion of methanol**
- **surface methoxy groups may be responsible for the formation of first hydrocarbons during the induction period of the MTO process**
- **aromatics are formed immediately after starting the conversion of methanol or methoxy groups on acidic zeolite catalysts**

Acknowledgements

**Thomas Horvath
Udo Schenk
Michael Seiler
Wei Wang
Andreas Buchholz
Mingcan Xu
Jian Jiao
Yijiao Jiang**

**Mikhail Luzgin
Alexander Stepanov
Irina Ivanova
Dieter Freude**

**Deutsche Forschungs-
gemeinschaft**

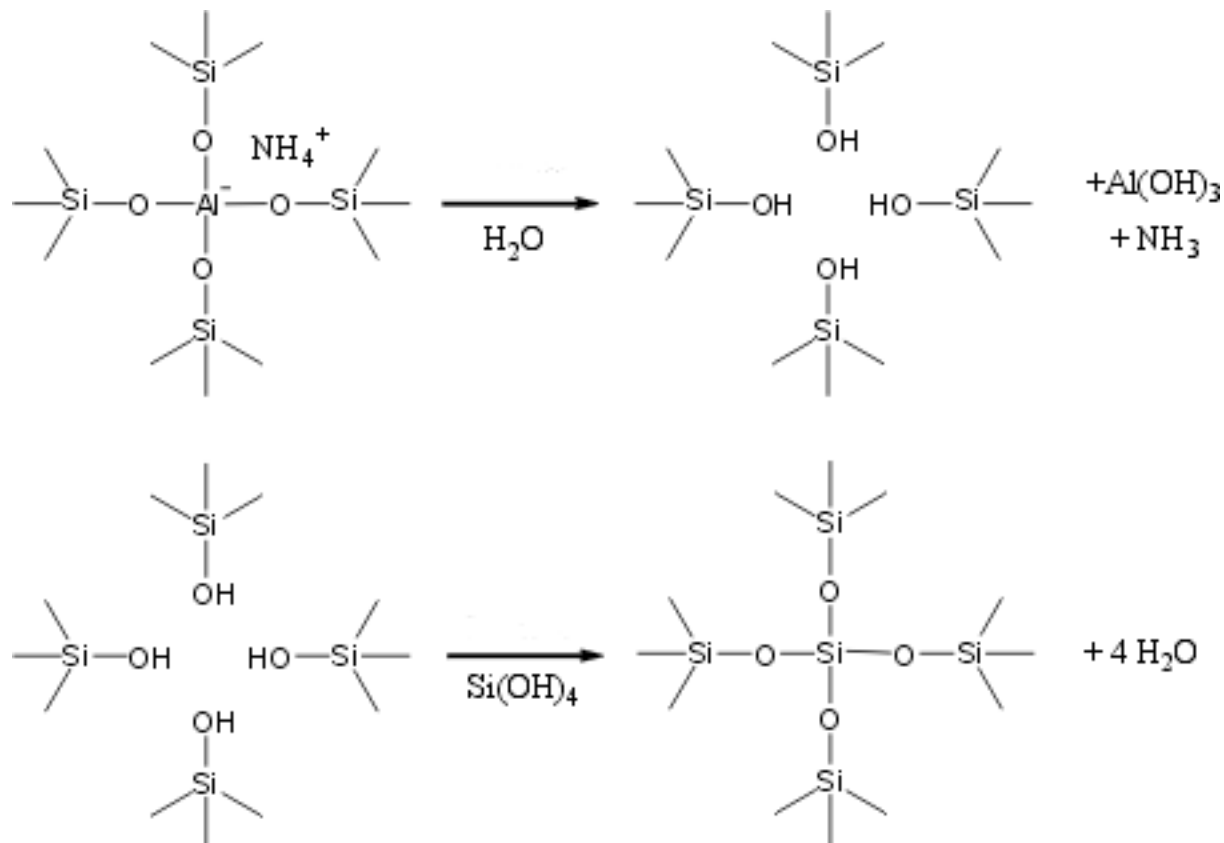
**Volkswagen-Stiftung
Hannover**

**Max-Buchner-Forschungs-
stiftung**

**Fonds der Chemischen
Industrie**

Proposed Dealumination Mechanisms I

Kerr, 1974:



G.T. Kerr, in: W.M. Meier, J.B. Uytterhoeven (Eds.), *Molecular Sieves, Advances in Chemistry Series*, Vol. 121, American Chemical Society, Washington, 1974, p. 219-229.

Proposed Dealumination Mechanisms II

Kuehl, 1977:

