

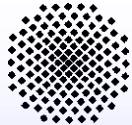
Nutzung der Festkörper-NMR-Spektroskopie für die Entwicklung und Charakterisierung von Feststoff-Katalysatoren

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Institut für Technische Chemie
Universität Stuttgart

Einweihung des Bruker-Avance-500WB-Spektrometers
am Fachbereich Chemie der TU Kaiserslautern,

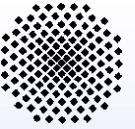
29. November 2011



Most abundant isotopes with nuclear spin

spin $I = 1/2$																	
H		integer spin															
Li	Be	quadrupolar nuclei with spin $I = 3/2, 5/2$ etc.															
Na	Mg	B	C	N	O	F	Ne	Al	Si	P	S	Cl	Ar				
K	Ca	Sc	Ti	V	Cr	Mn	Fe	Co	Ni	Cu	Zn	Ga	Ge	As	Se	Br	Kr
Rb	Sr	Y	Zr	Nb	Mo	Tc	Ru	Rh	Pd	Ag	Cd	In	Sn	Sb	Te	I	Xe
Cs	Ba	La	Hf	Ta	W	Re	Os	Ir	Pt	Au	Hg	Tl	Pb	Bi	Po	At	Rn
Fr	Ra	Ac	Ce	Pr	Nd	Pm	Sm	Eu	Gd	Tb	Dy	Ho	Er	Tm	Yb	Lu	
			Th	Pa	U	Np	Pu	Am	Cm	Bk	Cf	Es	Fm	Md	No	Lr	





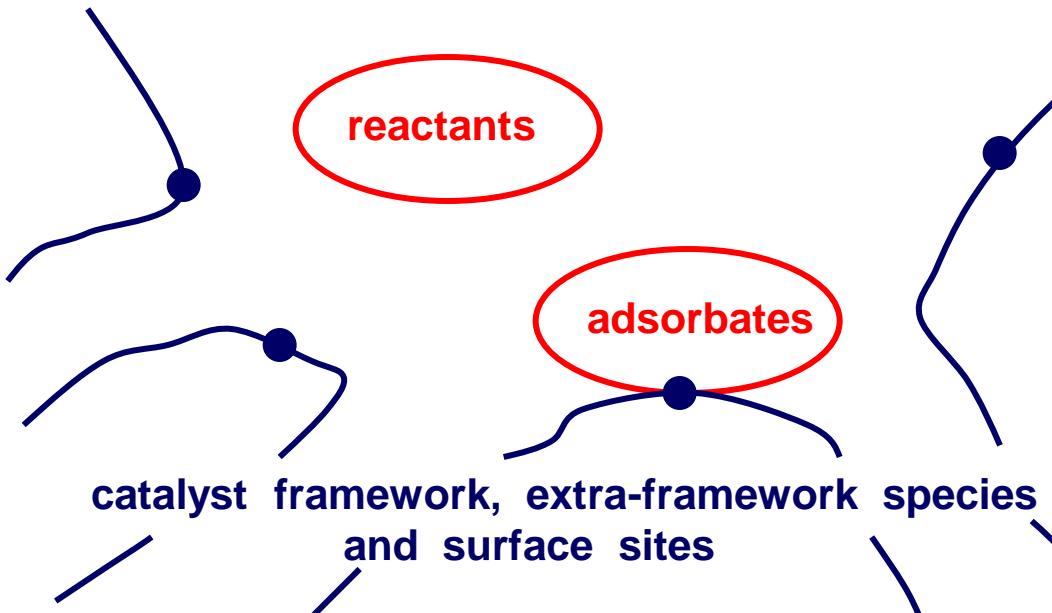
Isotopes interesting for solid-state NMR in heterogeneous catalysis

interesting isotopes (nuclear spin, relative sensitivity in comparison with ^1H)

^1H (1/2, 1.00), ^2H (1, 1.4×10^{-6})

^{13}C (1/2, 1.8×10^{-4}), ^{15}N (1/2, 3.8×10^{-6})

^{31}P (1/2, 6.6×10^{-2})



^7Li (3/2, 0.27)

^{11}B (3/2, 0.13)

^{17}O (5/2, 1.1×10^{-5})

^{23}Na (3/2, 9.2×10^{-2})

^{27}Al (5/2, 0.21)

^{29}Si (1/2, 3.7×10^{-4})

^{31}P (1/2, 6.6×10^{-2})

^{51}V (7/2, 0.38)

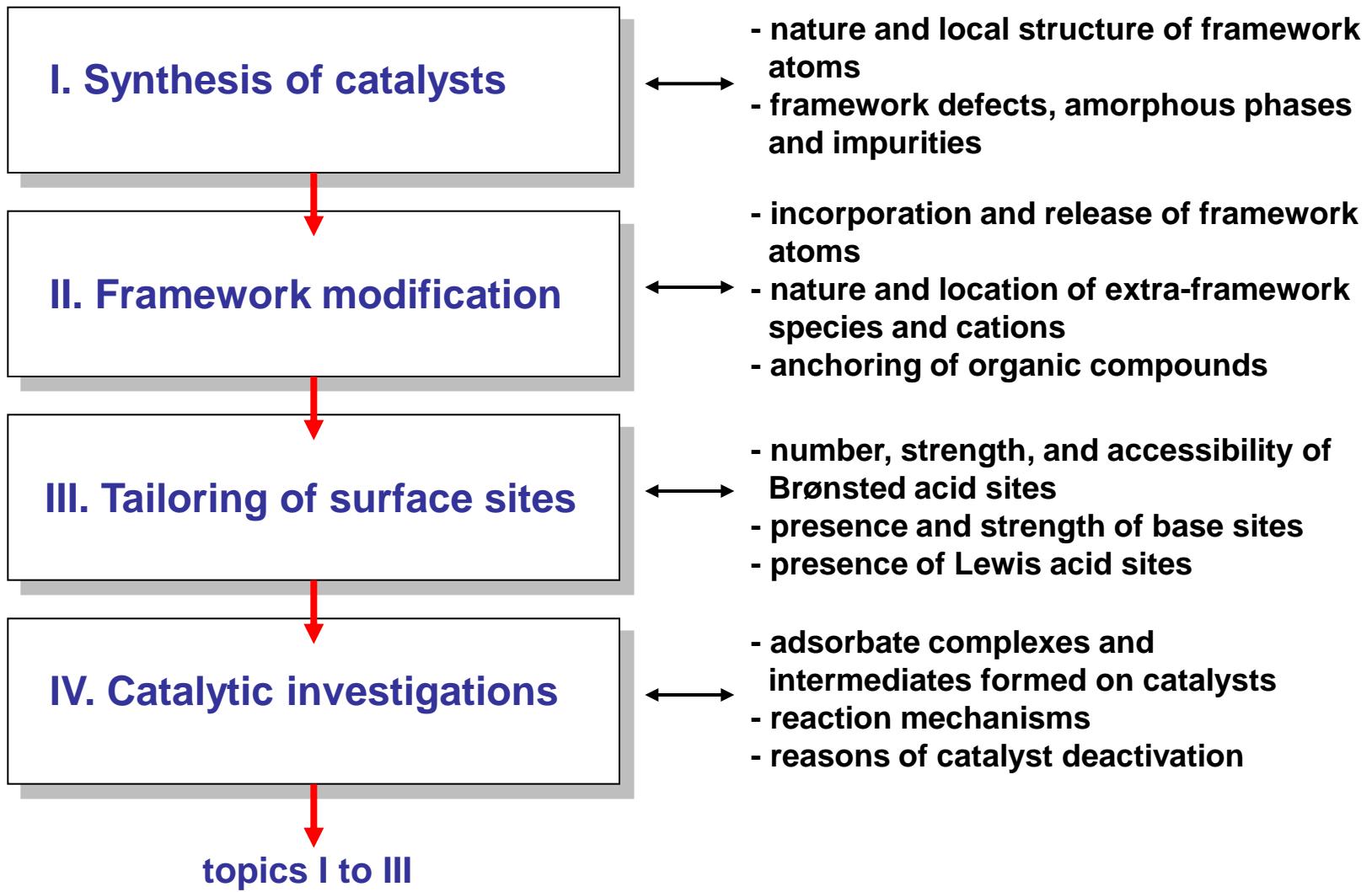
^{67}Zn (5/2, 1.2×10^{-2})

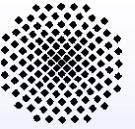
^{71}Ga (3/2, 5.6×10^{-2})

^{133}Cs (7/2, 4.7×10^{-2})



Solid-state NMR of solid catalysts





Specific problems of solid-state NMR spectroscopy

Magnetization M_0 , Curie's law:

$$M_0 = \frac{N \gamma^2 h^2 I(I+1) B_0}{(2\pi)^2 3 k_B T}$$

detection limit of solid-state NMR is
ca. $N = 10 \mu\text{mol}$ spins per gram for
 ^1H nuclei at room temperature

magnetization M_0 decreases with
increasing temperature T

broadening of NMR signals due to
internal solid-state interactions

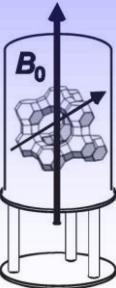
most important solid-state interactions:

H_{CSA} : anisotropic shielding of the magnetic field due to the anisotropic electron density in the local structure of the resonating nuclei;
 $\mathcal{F}\{\text{LP}^{(2)}\}$ $\Delta\nu_{\text{CSA}}$ up to 50 kHz

H_{DI} : dipolar interaction with magnetic dipole moments of neighboring spins in the local structure; $\mathcal{F}\{\text{LP}^{(2)}\}$

$\Delta\nu_{\text{DI}}$ up to 100 kHz

H_{Q} : quadrupolar interaction of the electric quadrupole moment of nuclei with spin $I = 3/2, 5/2$ etc. with electric field gradients; $\mathcal{F}\{\text{LP}^{(2)} + \text{LP}^{(4)}\}$
 $\Delta\nu_{\text{Q}}$ up to 20 MHz



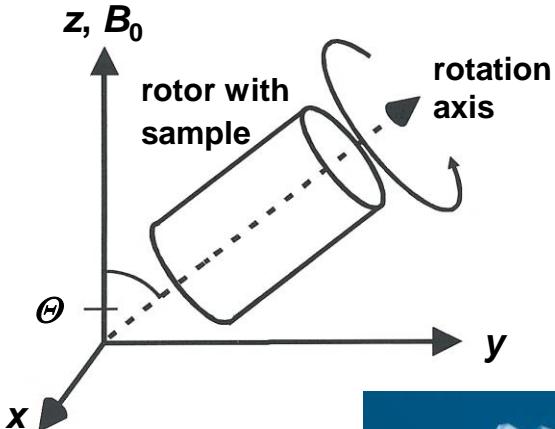
Techniques of solid-state NMR spectroscopy

spin $I = 1/2$:

magic angle spinning (MAS)

$$\nu_{\text{CSA, DI, } 1\text{QI}} = \mathcal{F} \{(3\cos^2\Theta - 1)/2\}$$

$$\rightarrow \Theta = 54.7^\circ$$



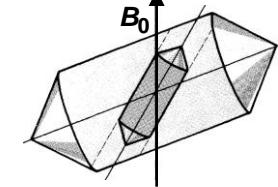
spin $I = 3/2, 5/2$ etc. :

double oriented rotation (DOR)

$$\nu_{2\text{QI}} = \mathcal{F} \{(35\cos^4\Theta - 30\cos^2\Theta + 3)/8\}$$

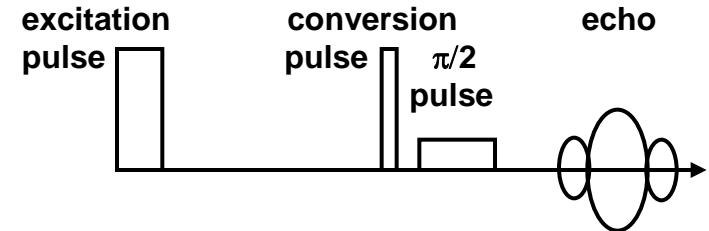
$$\rightarrow \Theta = 30.6^\circ$$

$$\Theta = 70.1^\circ$$

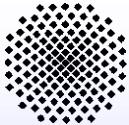


multiple-quantum MAS NMR (MQMAS)

- excitation of three- and five- quantum transitions
- recording of a spin-echo free of anisotropic contributions



J. Amoureaux et al., J. Magn. Reson A 123 (1996) 116

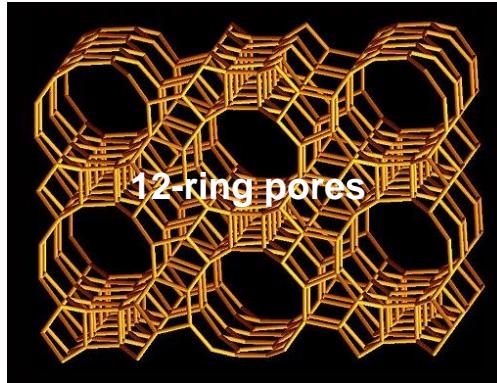


I. Synthesis of catalysts

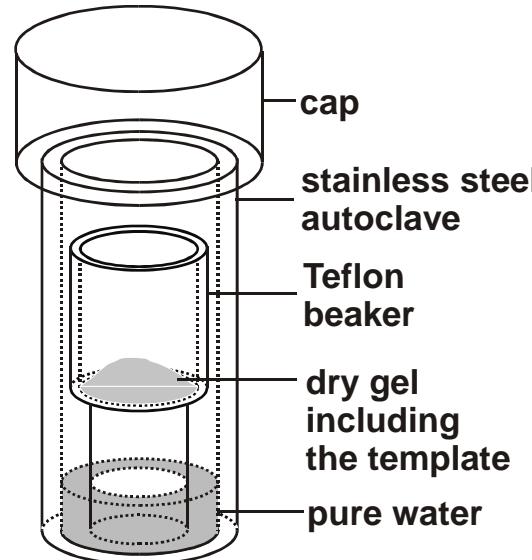
I. Synthesis of catalysts

synthesis of zeolite [Ga,Al]Beta by steam-assisted dry-gel conversion (SAC)

structure of zeolite Beta (BEA)



autoclave volume:
110 cm³
Teflon beaker:
14.5 cm³



Tetraethylammonium hydroxide (TEAOH)
 Ga_2O_3 , $\text{Ga}(\text{NO}_3)_3$, Pural SB or $\text{Al}_2(\text{SO}_4)_3$

Cab-osil M-5
(Fluka)

NaOH
water

Drying
at 353K

Dry gel

Crystallization
453 K, 3 days

Zeolite Beta (a.s.)

Calcination at
723 K in N_2 and air

Zeolite Beta (calc.)

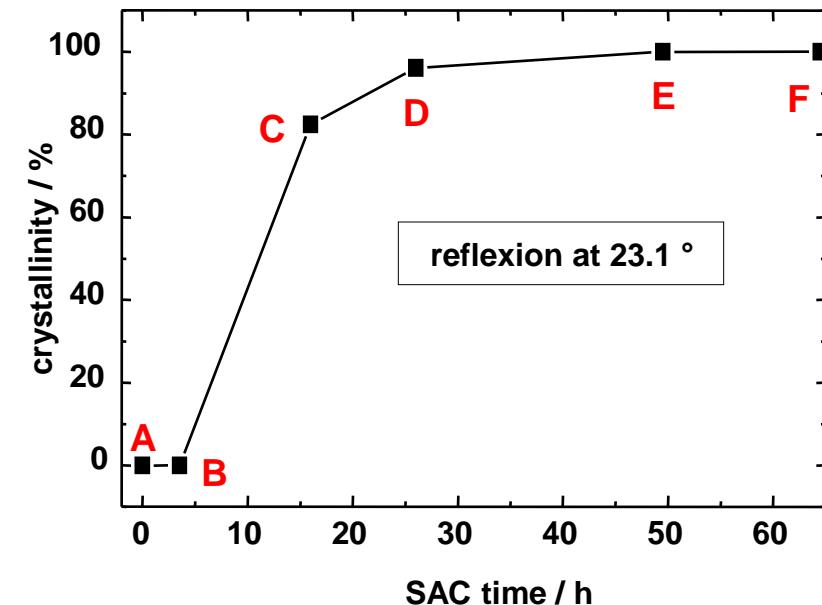
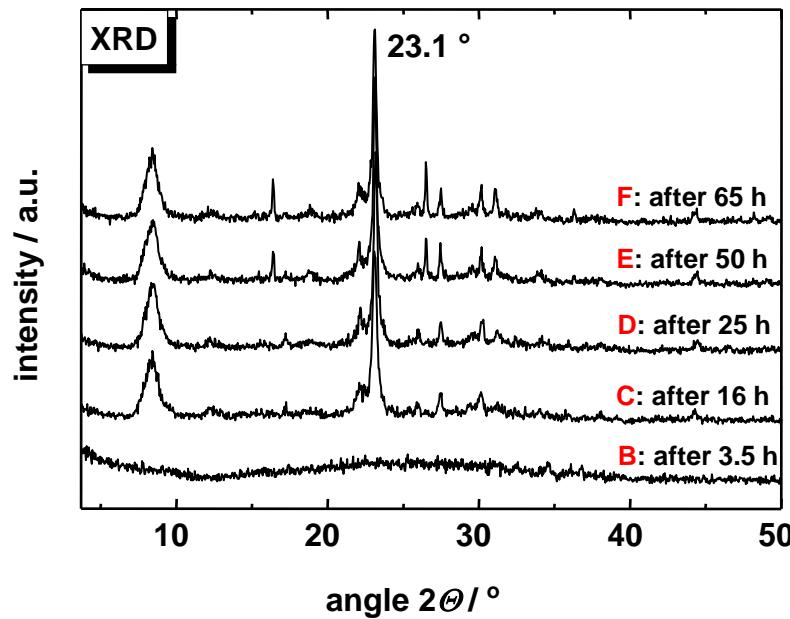
Ion exchange with
 NH_4NO_3 and thermal
treatment at 673 K

Zeolite H-Beta

I. Synthesis of catalysts

synthesis of zeolite [Ga,Al]Beta by steam-assisted dry-gel conversion (SAC)

powder X-ray diffractograms and crystallinity as a function of the dry-gel conversion time



sample A:

samples B to F:

dry gel taken before conversion

materials taken after conversion for 3.5 to 65 h



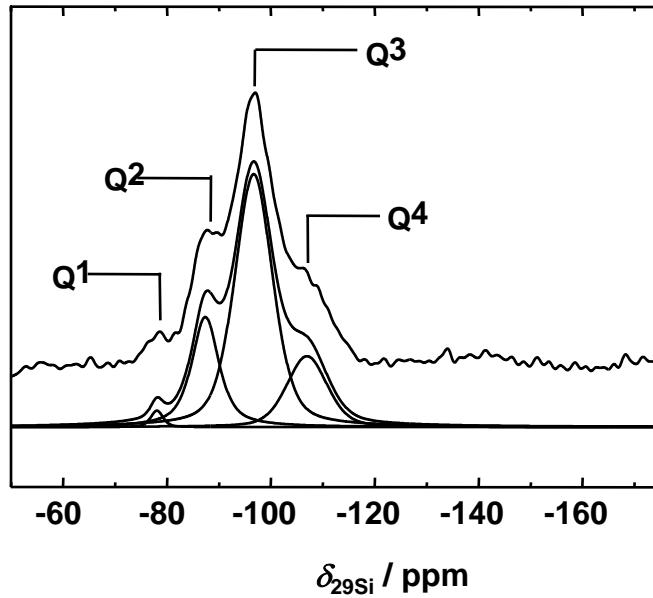
I. Synthesis of catalysts

synthesis of zeolite [Ga,Al]Beta by steam-assisted dry-gel conversion (SAC)

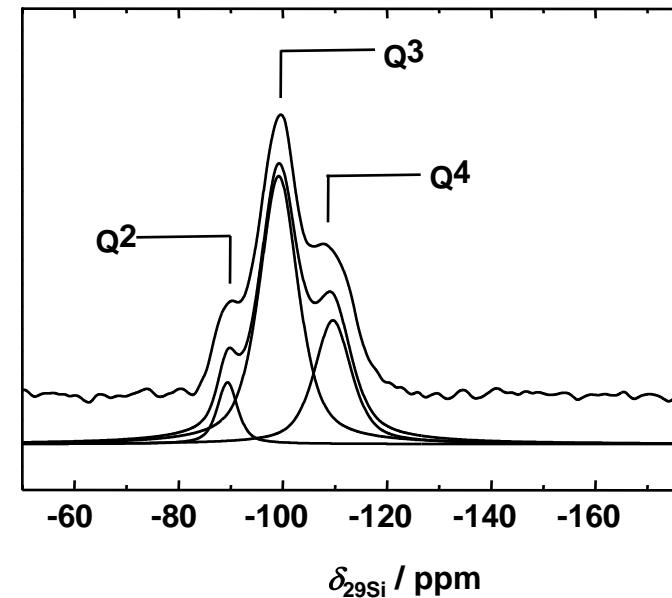
^{29}Si MAS NMR spectra recorded after different SAC times

$B_0 = 9.4 \text{ T}$, $\nu_0 = 79.5 \text{ MHz}$

A: fresh dry-gel particles (0 h)



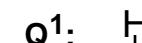
B: SAC time of 3.5 h



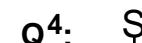
Q¹: silicon with one Si-O-Si bond, Si(1Si,3OH), at ca. -78 ppm

Q⁴: silicon with four Si-O-Si bonds, Si(4Si), at ca. -107 ppm

Q¹:



Q⁴:



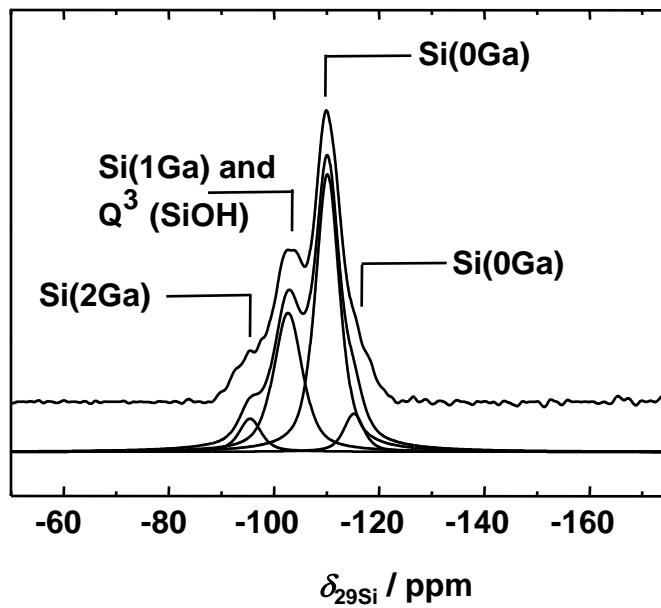
I. Synthesis of catalysts

synthesis of zeolite [Ga,Al]Beta by steam-assisted dry-gel conversion (SAC)

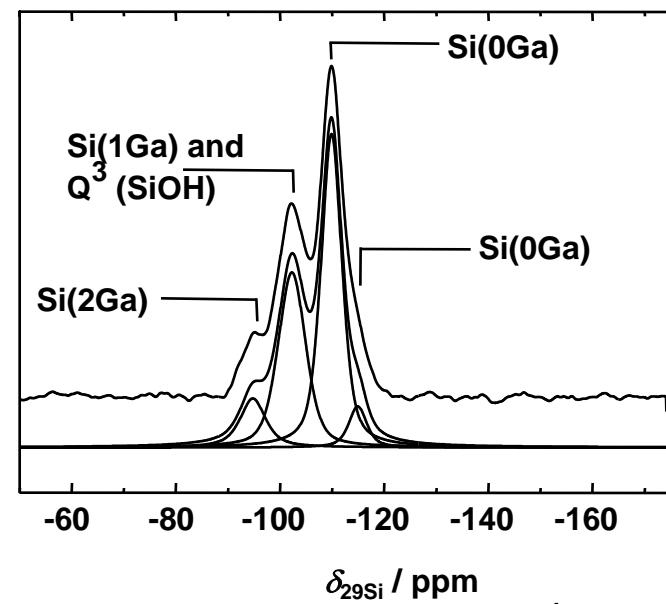
^{29}Si MAS NMR spectra recorded after different SAC times

$B_0 = 9.4 \text{ T}$, $\nu_0 = 79.5 \text{ MHz}$

C: SAC time of 16 h



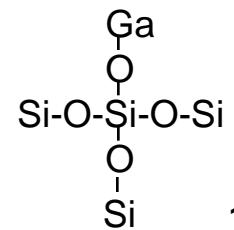
F: SAC time of 65 h



Si(1Ga): Q^4 framework silicon with one Si-O-Ga and three Si-O-Si bonds, Si(3Si,1Ga), at -101 ppm is overlapped by the Q³ signal, Si(3Si,1OH), at ca. -103 ppm

Si(2Ga): framework silicon with two Si-O-Ga and two Si-O-Si bonds, Si(2Si,2Ga), at -95 ppm

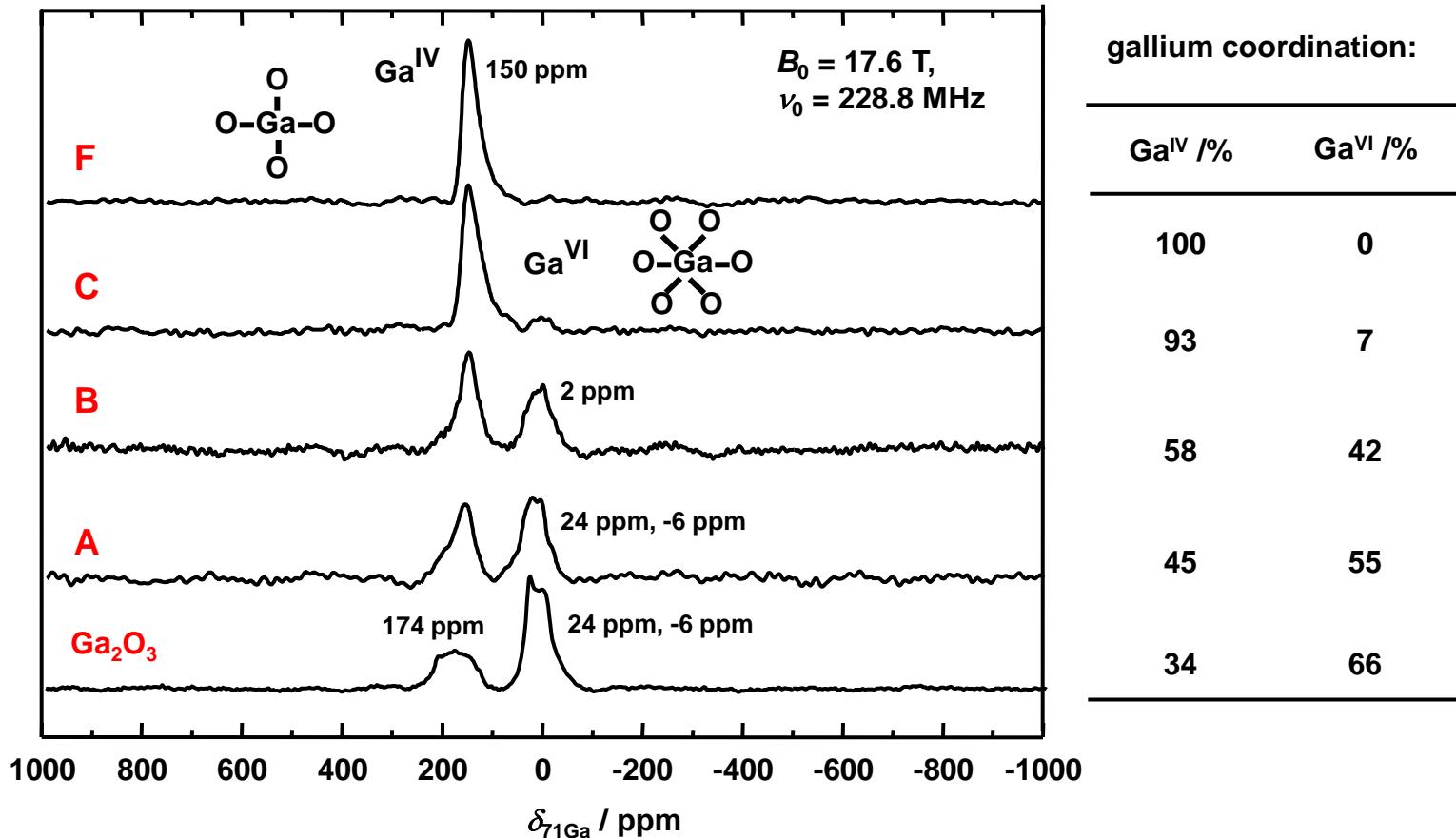
Q^4 : Si(3Si,1Ga)



I. Synthesis of catalysts

synthesis of zeolite [Ga,Al]Beta by steam-assisted dry-gel conversion (SAC)

^{71}Ga MAS NMR spectra (spin $I = 3/2$) recorded after different SAC times

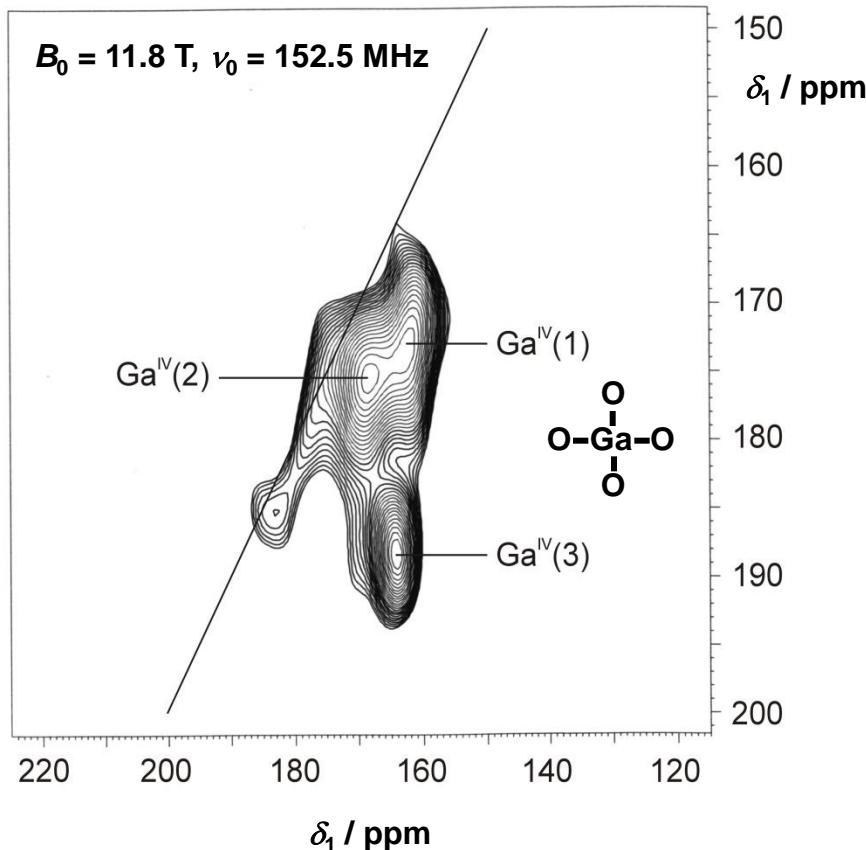


complete tetrahedral oxygen coordination of gallium atoms after a SAC time of 65 h

I. Synthesis of catalysts

synthesis of zeolite [Ga,Al]Beta by steam-assisted dry-gel conversion (SAC)

^{71}Ga MQMAS NMR spectroscopy (spin $I = 3/2$) of [Ga]Beta sample F (65 h)



$\text{Ga}^{\text{IV}}(1, 2)$:
framework gallium species,
 $\text{SOQE} = 2.2$ and 1.8 MHz ,
 $\delta_{\text{iso}} = 172$ and 168 ppm

$\text{Ga}^{\text{IV}}(3)$:
extra-framework gallium
species at defect sites or in
an amorphous phase,
 $\text{SOQE} = 4.7 \text{ MHz}$,
 $\delta_{\text{iso}} = 176 \text{ ppm}$

I. Synthesis of catalysts

synthesis of flame-derived silica-alumina with different aluminum contents

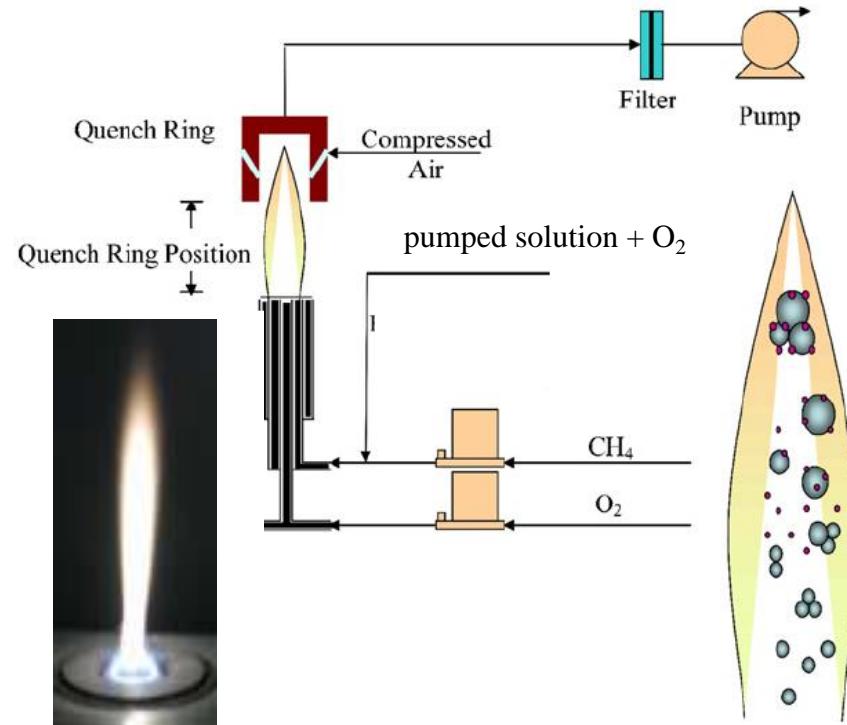
preparation of flame-made silica-alumina (SA) catalysts:

dissolving aluminum(III)
acetylacetone and tetraethoxysilane
in a 1:1 (vol%) mixture of acetic acid
and methanol

this solution was pumped through a
capillary with 5 ml/min and nebulized
with 5 l/min O₂

the spray was ignited by a methane/
oxygen flame (1.5/0.9 L/min) resulting
in an approximately 6 cm long flame

particles (ca. 20 nm) were collected on
a cooled Whatman GF6 filter

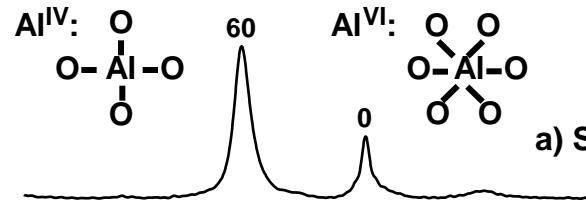


I. Synthesis of catalysts

synthesis of flame-derived silica-alumina with different aluminum contents

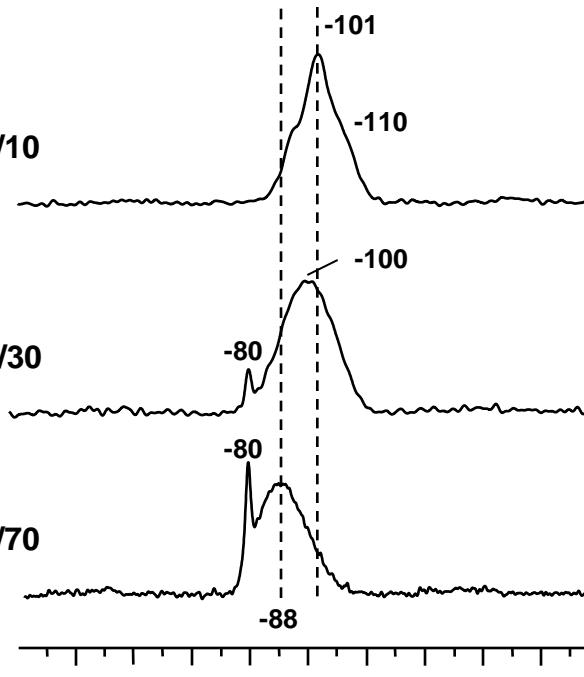
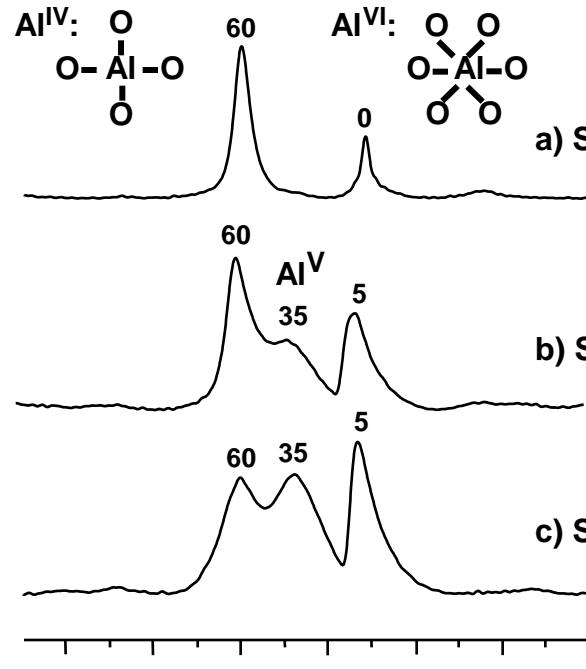
^{27}Al MAS NMR (spin $I = 5/2$)

$B_0 = 9.4 \text{ T}$, $\nu_0 = 104.4 \text{ MHz}$



^{29}Si MAS NMR

$B_0 = 9.4 \text{ T}$, $\nu_0 = 79.5 \text{ MHz}$



Q^3 silicon species:

$\text{Si}(3\text{Si},\text{OH})$
 $+\text{Si}(2\text{Si},1\text{Al},\text{OH})$

$+\text{Si}(1\text{Si},2\text{Al},\text{OH})$

$+\text{Si}(3\text{Al},\text{OH})$

formation of andalusite phases (Al_2SiO_5) with $\delta_{^{29}\text{Si}} = -79.8 \text{ ppm}$ (M. Mägi et al., J. Phys. Chem. 88 (1984) 1518) and octahedrally ($\delta_{^{27}\text{Al}} = 5 \text{ ppm}$) as well as pentacoordinated aluminum atoms ($\delta_{^{27}\text{Al}} = 35 \text{ ppm}$)



I. Synthesis of catalysts

synthesis of flame-derived silica-alumina with different aluminum contents

^1H MAS NMR

upon dehydration at 723 K

SA/0, pure silica



$B_0 = 9.4 \text{ T}$

$\nu_0 = 400.1 \text{ MHz}$

SA/0 + NH₃



SA/10



SA/10 + NH₃



SA/30

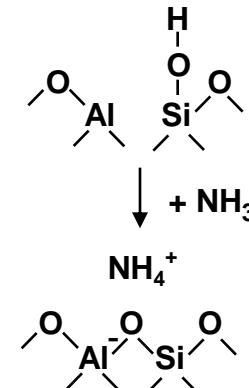
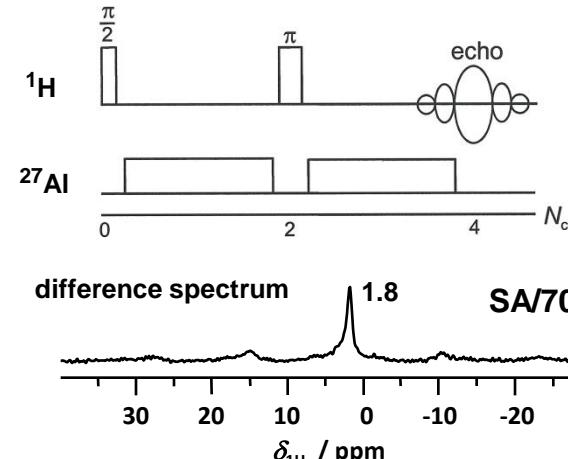


SA/30 + NH₃



increases with increasing
molar aluminum content

$^1\text{H}/^{27}\text{Al}$ TRAPDOR MAS NMR

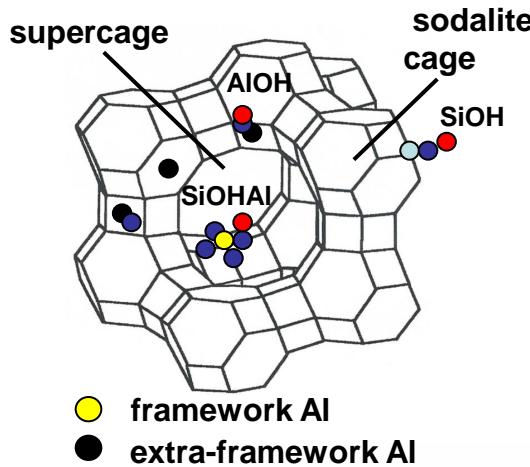


II. Modification of catalysts

II. Framework modification

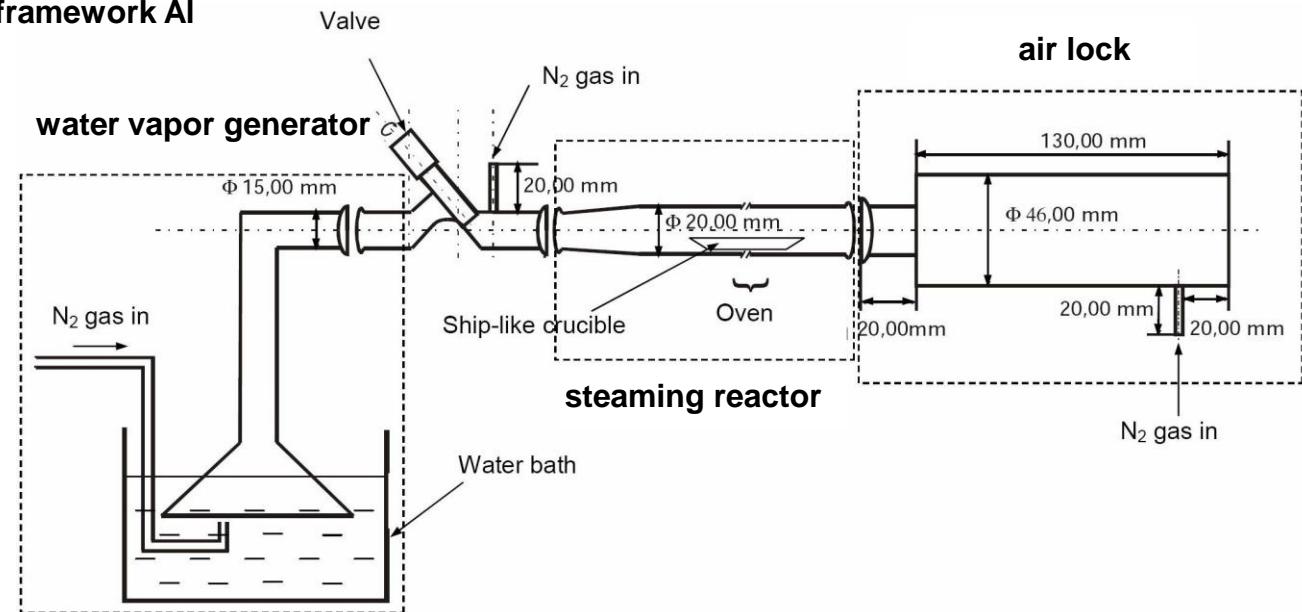
dealumination of zeolite H,Na-Y by steaming

structure of zeolite Y (FAU)



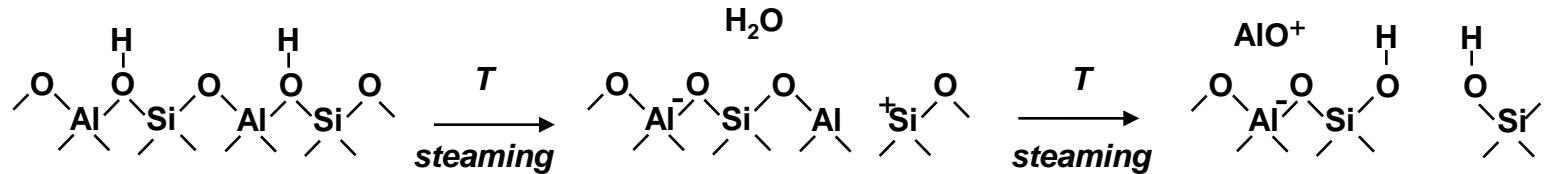
dealumination procedure

commercial zeolite Na-Y ($n_{\text{Si}}/n_{\text{Al}} = 2.7$) → ammonium exchange (93%) → dealuminated zeolite deH,Na-Y/31.1-81.5 ($n_{\text{Si}}/n_{\text{Al}} = 3.6-6.0$) → steaming at 748 K under flowing nitrogen (100 ml/min) with a water vapor pressure of 7.4-81.5 kPa → transfer into gas-tight MAS NMR rotor without rehydration

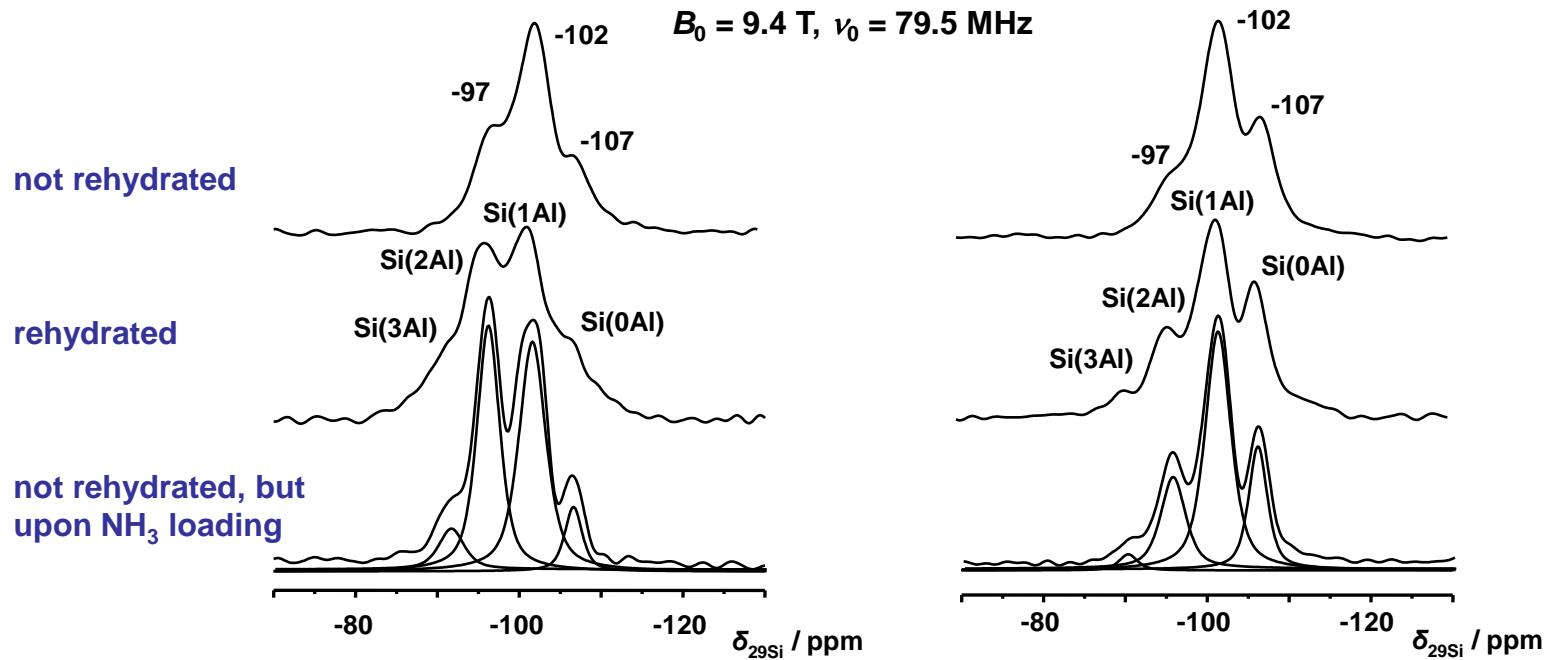


II. Framework modification

dealumination of acidic zeolites by steaming



^{29}Si MAS NMR spectroscopy of zeolites H,Na-Y (left) and deH,Na-Y/31.1 (right)



$$\frac{n_{\text{Si}}}{n_{\text{Al}}} = \frac{100}{\sum_n 0.25 \cdot n \cdot I_{\text{Si}(n\text{Al})}} : 2.7 \quad (\text{51.9 Al}^{\text{fr}} / \text{u.c.})$$

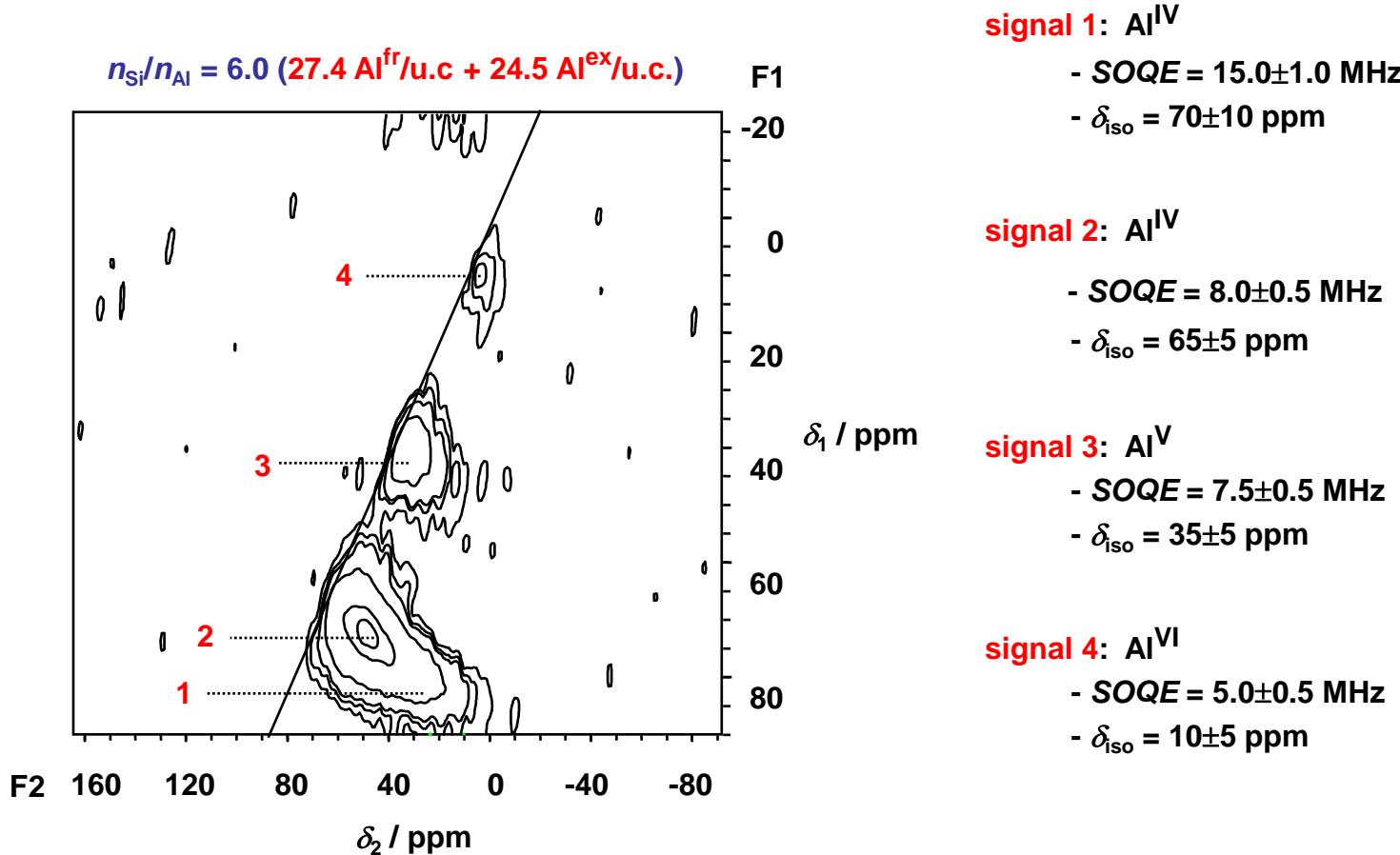
$$3.8 \quad (\text{40.0 Al}^{\text{fr}}/\text{u.c.} + \text{11.9 Al}^{\text{ex}}/\text{u.c.})$$

II. Framework modification

dealumination of zeolite H,Na-Y by steaming

^{27}Al MQMAS NMR spectroscopy (spin $I = 5/2$) of not rehydrated zeolite deH,Na-Y/81.5

$B_0 = 17.6 \text{ T}$, $\nu_0 = 195.5 \text{ MHz}$, $\nu_{\text{rot}} = 30 \text{ kHz}$



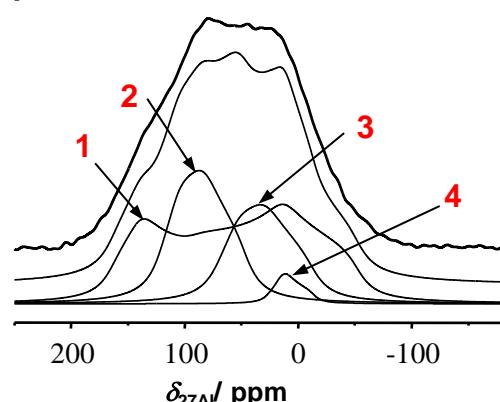
II. Framework modification

dealumination of zeolite H,Na-Y by steaming

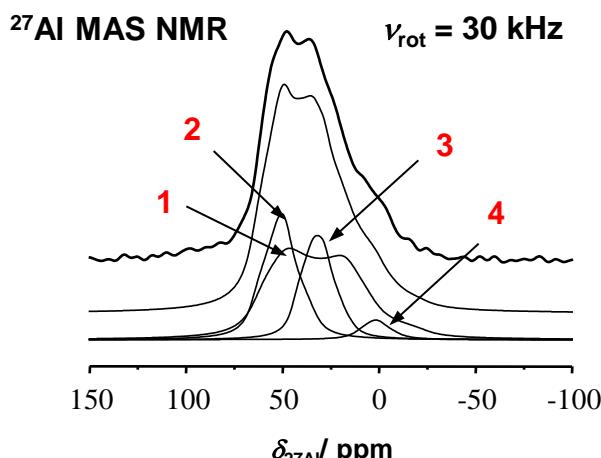
^{27}Al solid-state NMR spectroscopy (spin $I = 5/2$) of zeolite deH,Na-Y/81.5 (51.9 Al/u.c.)

$$B_0 = 17.6 \text{ T}, \nu_0 = 195.5 \text{ MHz}$$

^{27}Al spin-echo NMR



^{27}Al MAS NMR



Signals	1	2	3	4
assignments	$\text{Al}^{\text{IV}}/\text{H}^+$ $\text{Al}^{\text{IV}}/\text{Al}^{\text{cat,x+}}$	$\text{Al}^{\text{IV}}/\text{Na}^+$ cluster Al^{IV}	$\text{Al}^{\text{V,x+}}$ cat.	cluster Al^{VI}
δ_{iso} / ppm	70 ± 10	65 ± 5	35 ± 5	10 ± 5
C_{QCC} / MHz	15.0 ± 1.0	8.0 ± 0.5	7.5 ± 0.5	5.0 ± 0.5
η_Q	0.3	0.8	0.7	0.7
I in %	48 (27+21)	27 (7+20)	21	4

extra-framework
Al cations ($\text{Al}^{\text{V,x+}}$):

$$10.9 \text{ Al}^{\text{V,x+}}/\text{u.c.}$$

extra-framework
 Al_2O_3 clusters:

$$12.5 \text{ Al}^{\text{cluster}}/\text{u.c.}$$

in comparison with $24.5 \text{ Al}^{\text{ex}}/\text{u.c.}$ calculated using results of
 ^{29}Si MAS NMR spectroscopy

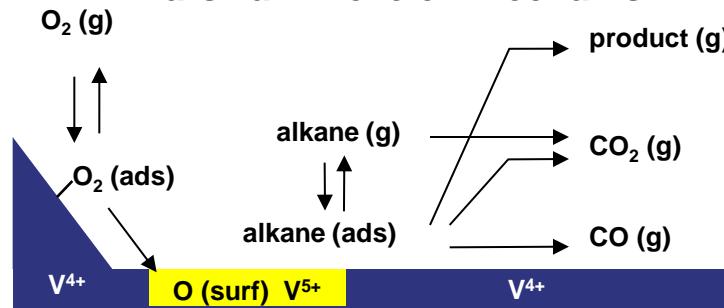
II. Modification of catalysts

VPO catalysts supported on mesoporous SBA-15 materials

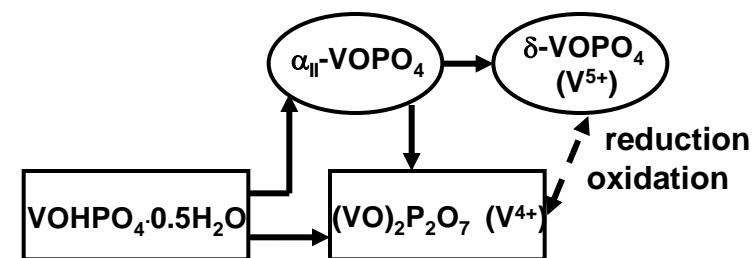
selective oxidation of *n*-butane



Mars van Krevelen mechanism



discussed phase transitions



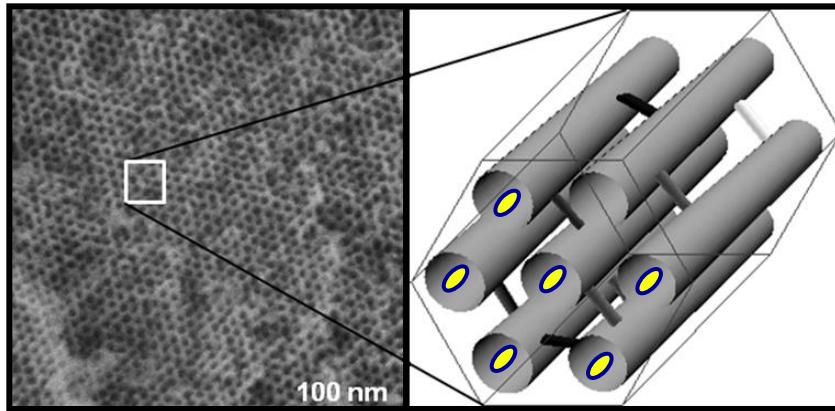
preparation procedure of X.-K. Li et al., J. Catal. 238 (2006) 232:

- siliceous SBA-15 is added to isobutyl/benzyl alcohols (1 : 1) with V_2O_5 and H_3PO_4
- activation in a flow of 1.5 % *n*-butane, 17.5 % O_2 and balance N_2 (100 ml/min) at 673 K

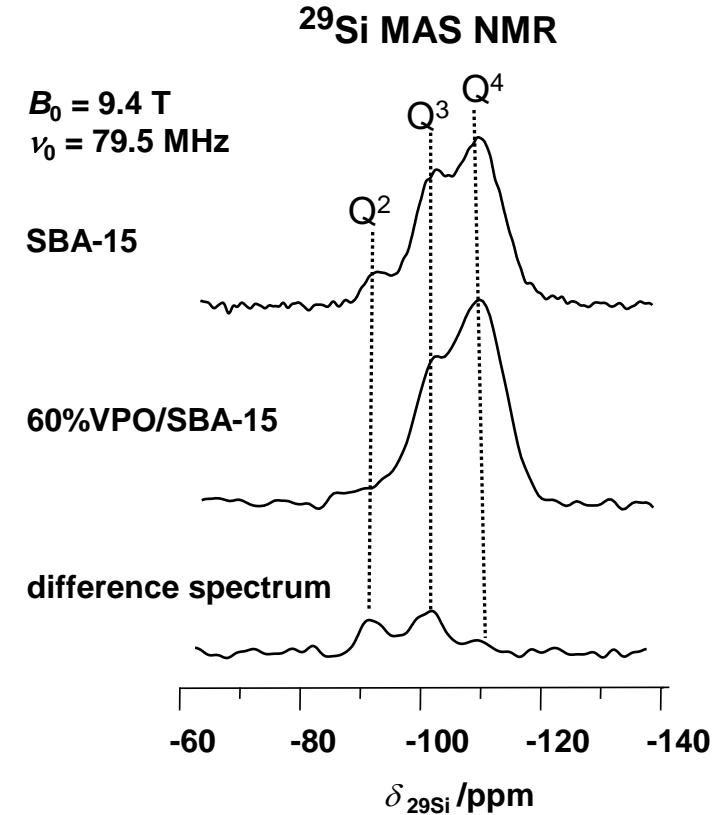


II. Framework modification

VPO catalysts supported on mesoporous SBA-15 materials



Materials	P / V	BET surface m ² / g	Pore volume cm ³ / g
SBA-15	-	1164	1.25
20%VPO/SBA-15	1.09	662	0.80
60%VPO/SBA-15	1.04	456	0.54

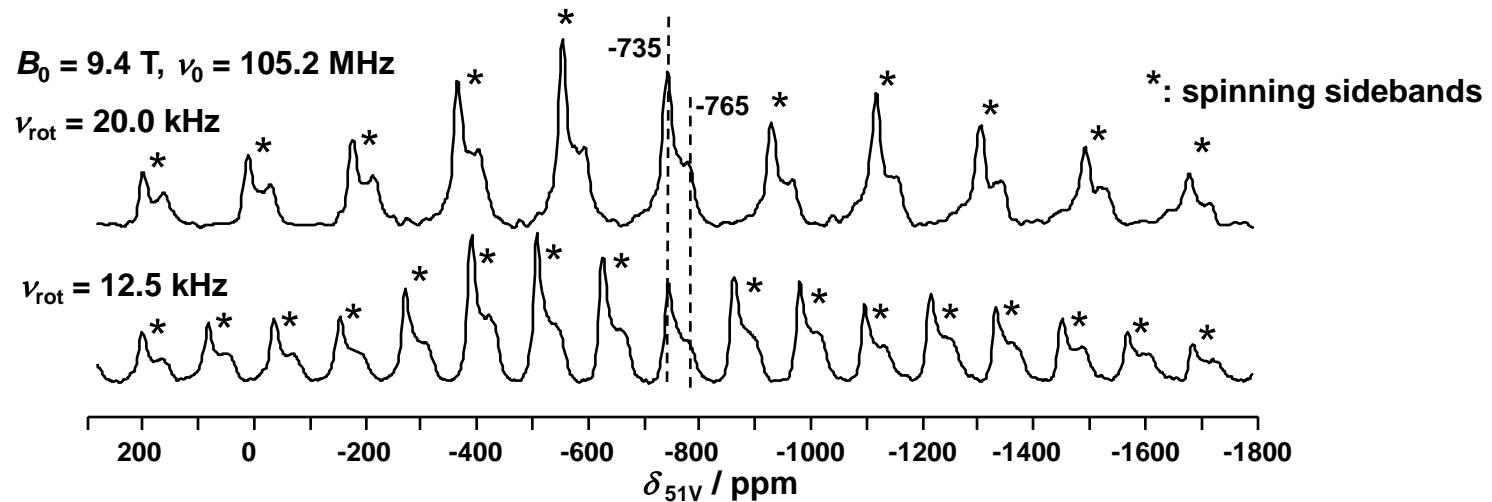


VPO is bound at former silanol groups on the mesoporous surface of SBA-15

II. Framework modification

VPO catalysts supported on mesoporous SBA-15 materials

^{51}V MAS NMR spectroscopy (spin $I = 7/2$) of 60%VPO/SBA-15 after activation



Materials	$\delta_{\text{iso}} / \text{ppm}$	$\Delta\sigma_{\text{CSA}} / \text{ppm}$	η_{CSA}	C_Q / MHz	η_Q
60%VPO/SBA-15	-735 -765	900 950	0.10 0.10	2.00 1.90	0.60 0.60
$\alpha_{\parallel}\text{-VOPO}_4$ ¹⁾	-755	992	0.08	0.63	0.09
$\beta\text{-VOPO}_4$ ¹⁾	-735	818	0.05	1.45	0.44

¹⁾ R. Siegel et al., Mag. Res. Chem. 42 (2004) 1022.
O.B. Lapina et al., Prog. Nucl. Magn. Reson. Spectrosc. 53 (2008) 128.

II. Framework modification

VPO catalysts supported on mesoporous SBA-15 materials

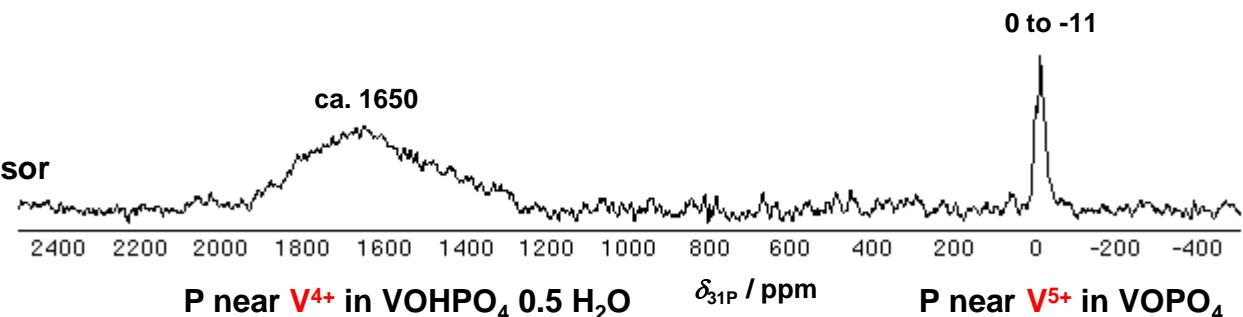
^{31}P MAS NMR spectroscopy of 60%VPO/SBA-15 before and after activation

$$B_0 = 9.4 \text{ T}$$

$$\nu_0 = 162.0 \text{ MHz}$$

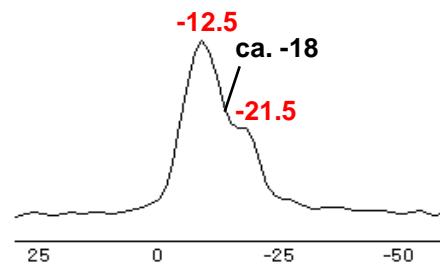
$$\nu_{\text{rot}} = 10 \text{ kHz}$$

non-activated precursor

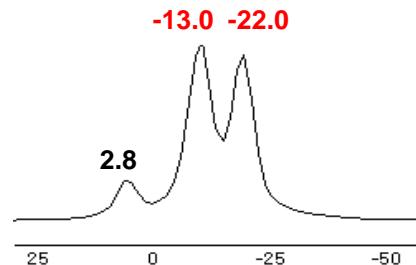


activated at 673 K
for 15 h

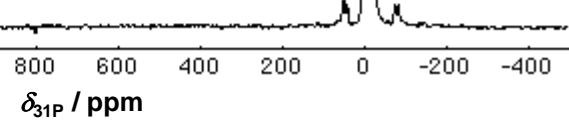
not rehydrated



rehydrated/dehydrated



2.8 to -22



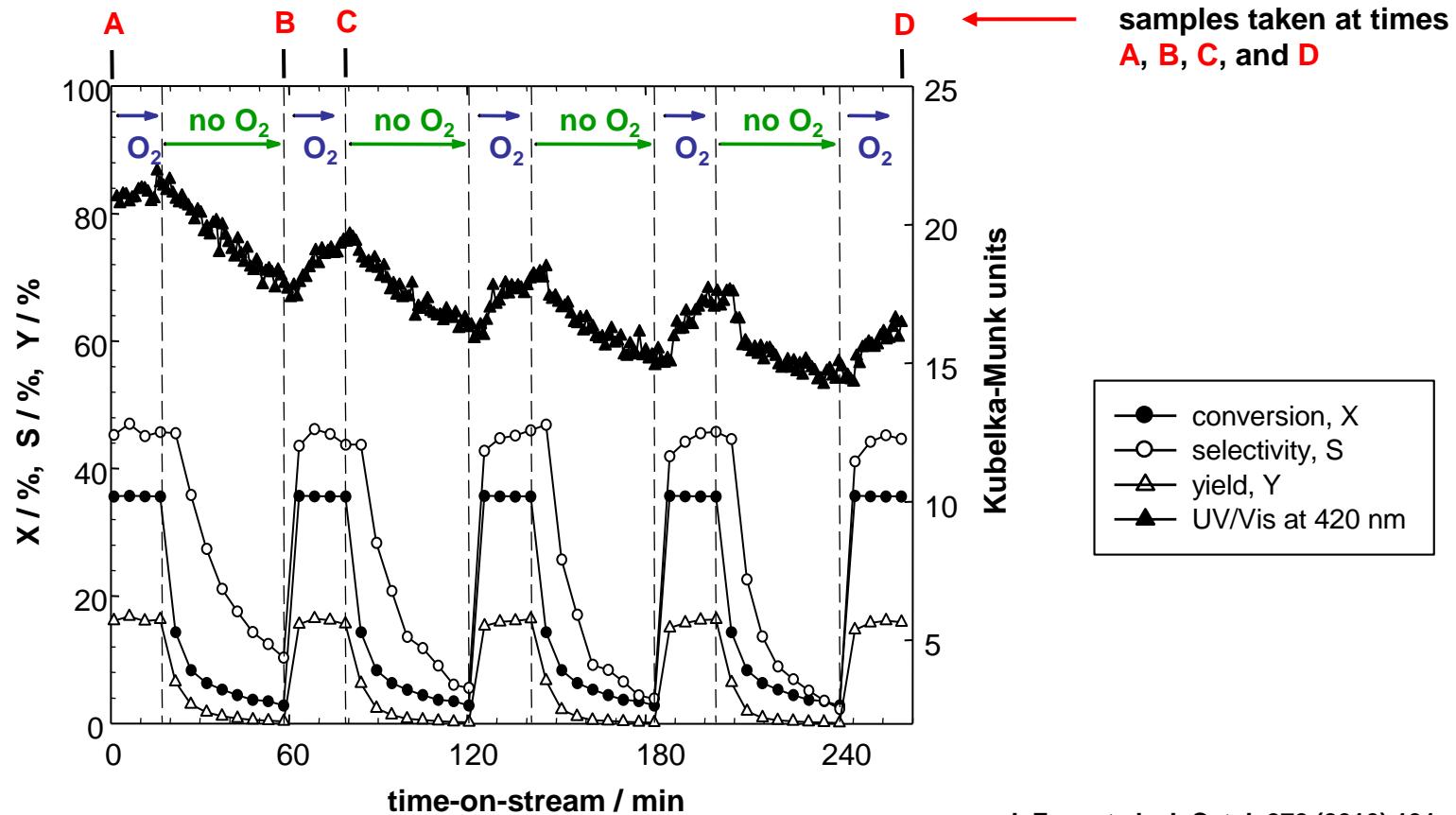
P near V^{5+} in VOPO_4 phases, such as $\beta\text{-VOPO}_4$ (-13 ppm) and $\alpha_{\parallel}\text{-VOPO}_4$ (-22 ppm)



II. Framework modification

VPO catalysts supported on mesoporous SBA-15 materials

selective oxidation of *n*-butane to maleic anhydride at 678 K with sequential switching on (15 min) and off (40 min) of the gaseous oxygen

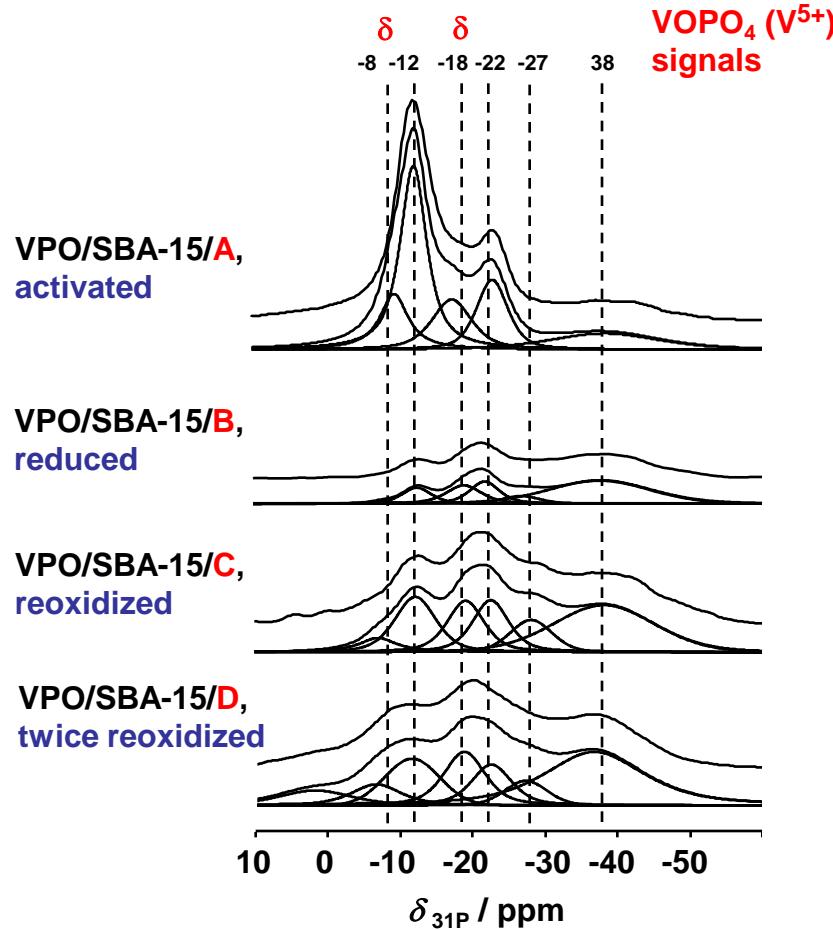


II. Framework modification

VPO catalysts supported on mesoporous SBA-15 materials

^{31}P MAS NMR spectra of VPO/SBA-15/A to VPO/SBA-15/D

$B_0 = 9.4 \text{ T}$, $\nu_0 = 162.0 \text{ MHz}$



Catalysts	Samples	Contents of P/V ⁵⁺
VPO/bulk	A	0.5 %
	B	0 %
	C	0.35 %
	D	0.4 %
VPO/SBA-15	A	2.6 %
	B	0.3 %
	C	0.9 %
	D	1.3 %

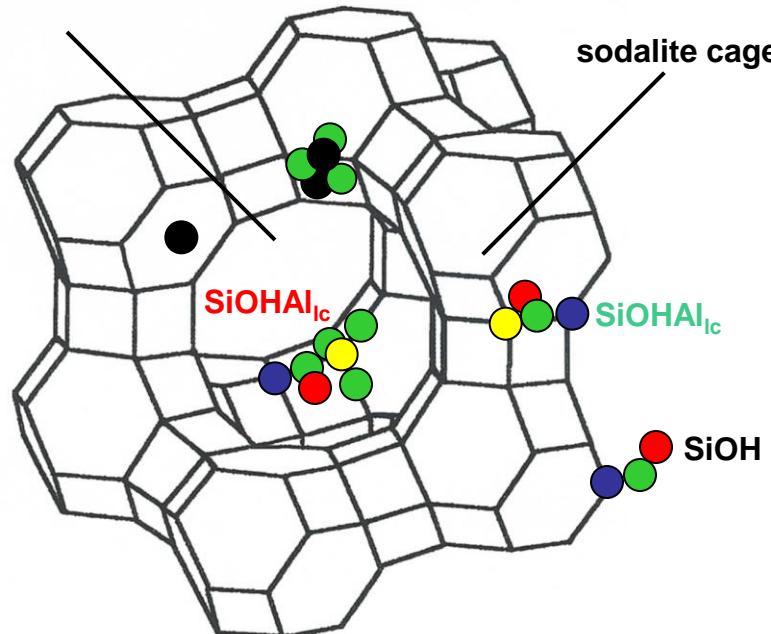
III. Tailoring of surface sites

III. Tailoring of surface sites

nature of acid sites on zeolites

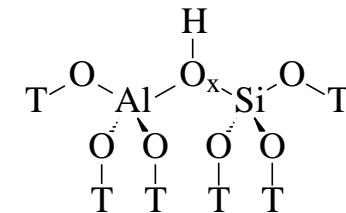
zeolite Y (FAU, faujasite): supercages connected via 12-ring windows (0.74 nm)

supercage (1.23 nm)



- Al atom
- O atom
- extra-framework cations (Na^+ ,
 Al_3^+ etc.)
- Si atom
- H atom

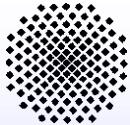
Brønsted acid sites:

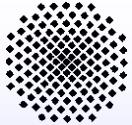


bridging OH group (SiOHAl)

Lewis acid sites:

- framework defects,
- extra-framework species
(Al oxide clusters)





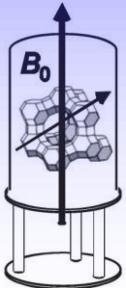
III. Tailoring of surface sites

preparation of dehydrated catalyst samples



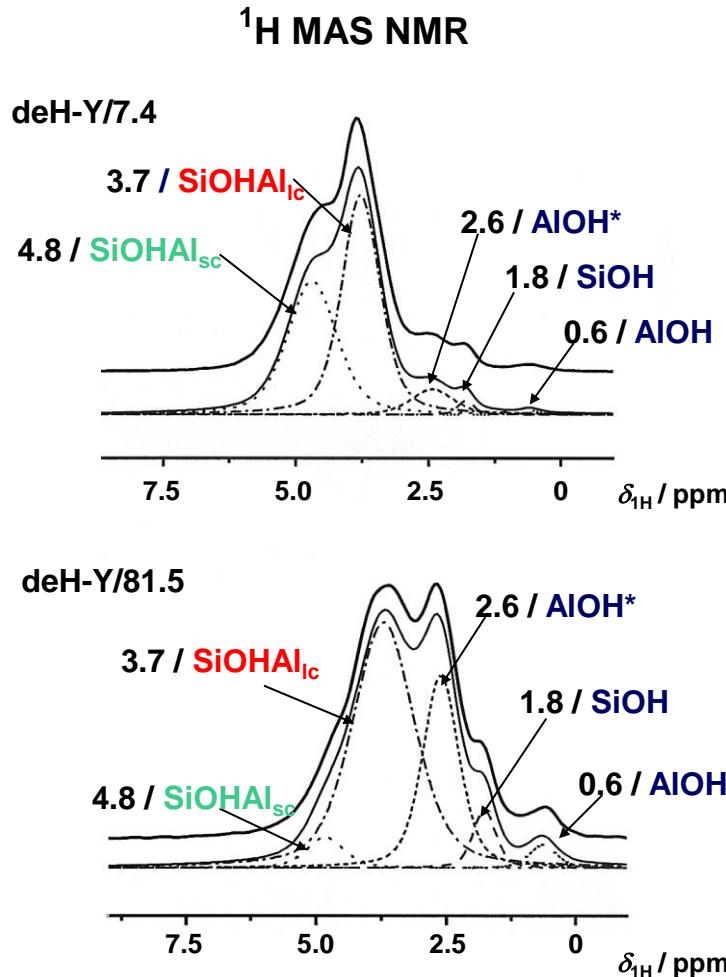
vacuum line for dehydration of catalyst samples in glass tubes at elevated temperatures (often 673 K)

transfer of the dehydrated catalyst samples from glass tubes into MAS rotors inside a glove box (dry nitrogen)



III. Tailoring of surface sites

modification of Brønsted acid sites in zeolites *via* steaming



undisturbed metal OH (AlOH) groups:
-0.5 to 0.5 ppm

defect SiOH groups:
1.2 to 2.2 ppm

AlOH* groups at extra-framework Al clusters:
2.8 to 3.6 ppm

bridging OH groups in large cages
and pores (SiOHAI_{lc}):
3.6 to 4.3 ppm

bridging OH groups in small cages
(SiOHAI_{sc}):
4.6 to 5.2 ppm

(hydrogen bonded SiOH and SiOHAI
groups: 5.2 to 13 ppm)

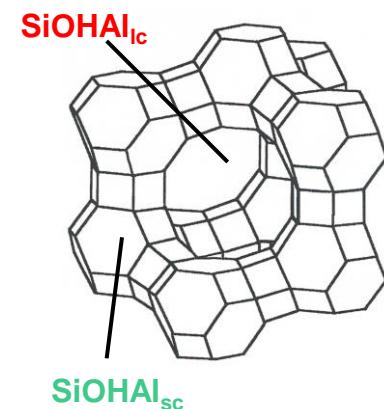
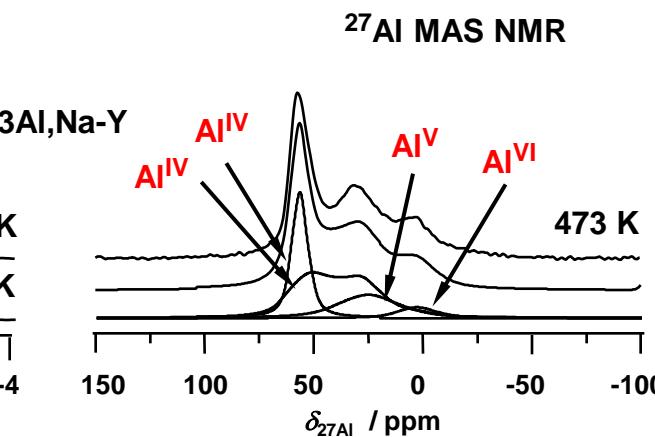
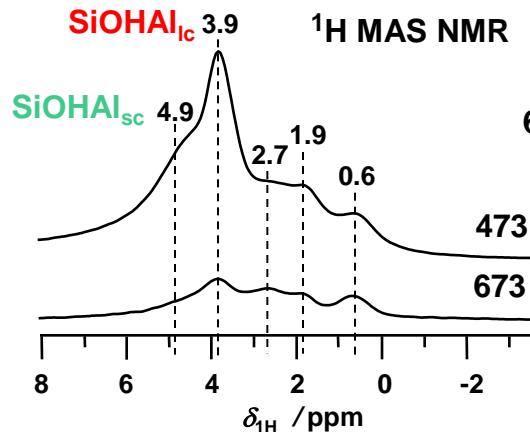
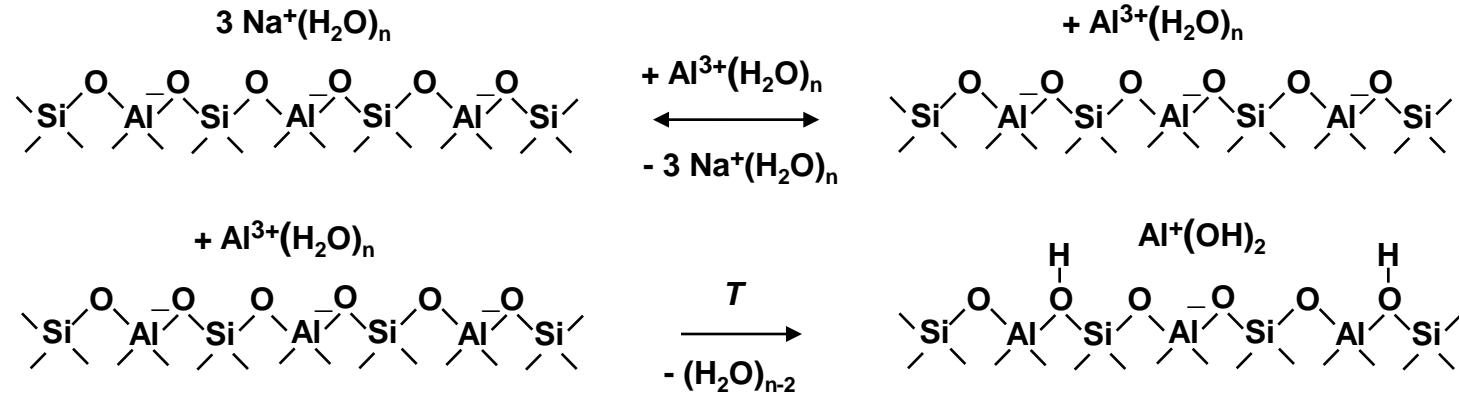


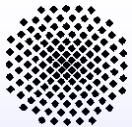
III. Tailoring of surface sites

preparation of Brønsted acid sites in zeolites *via* exchange with multivalent cations

exchange of zeolite Na-Y ($n_{\text{Si}}/n_{\text{Al}} = 2.7$) in 0.1 M $\text{Al}(\text{NO}_3)_3$ solution

Hirschler Plank mechanism



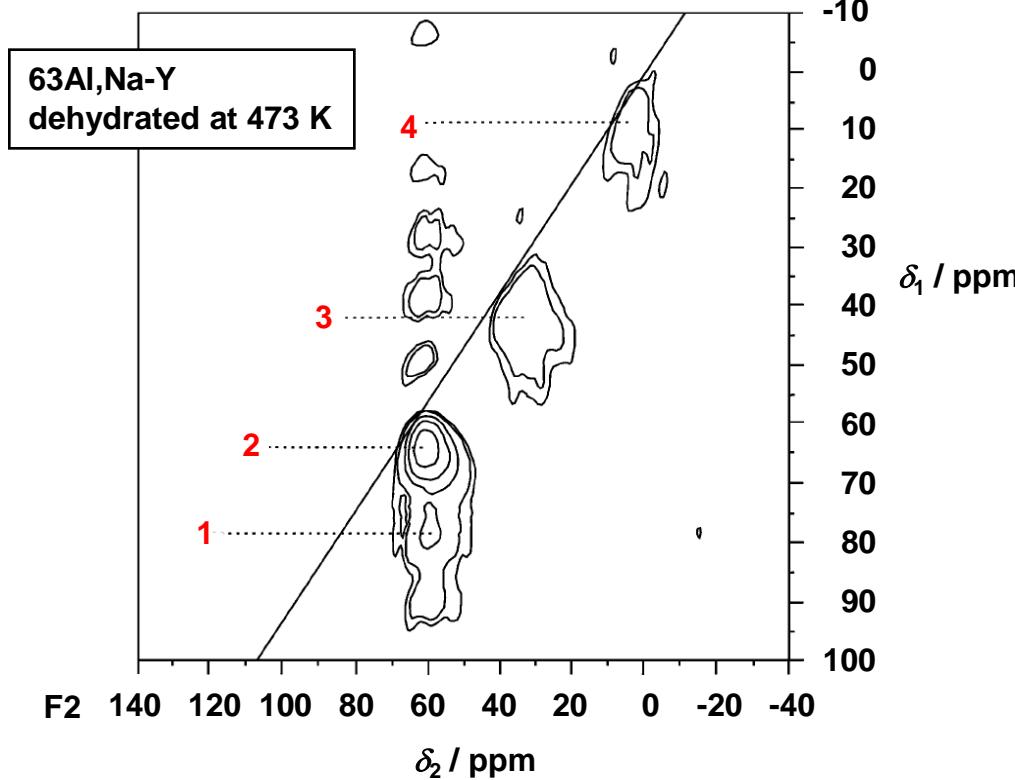


III. Tailoring of surface sites

preparation of Brønsted acid sites in zeolites *via* exchange with multivalent cations

^{27}Al MQMAS NMR (spin $I = 3/2$)

$B_0 = 17.6 \text{ T}$, $\nu_0 = 195.5 \text{ MHz}$, $\nu_{\text{rot}} = 30 \text{ kHz}$



signal 1: Al^{IV}

- SOQE = 10.1 MHz
- $\delta_{\text{iso}} = 71 \text{ ppm}$

signal 2: Al^{IV}

- SOQE = 3.6 MHz
- $\delta_{\text{iso}} = 62 \text{ ppm}$

signal 3: Al^{V}

- SOQE = 7.6 MHz
- $\delta_{\text{iso}} = 39 \text{ ppm}$

signal 4: Al^{VI}

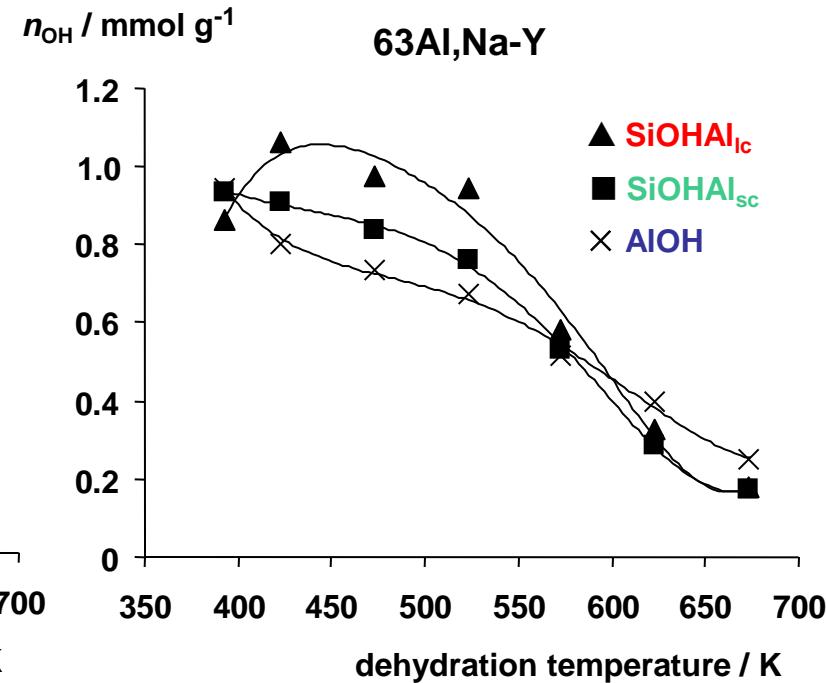
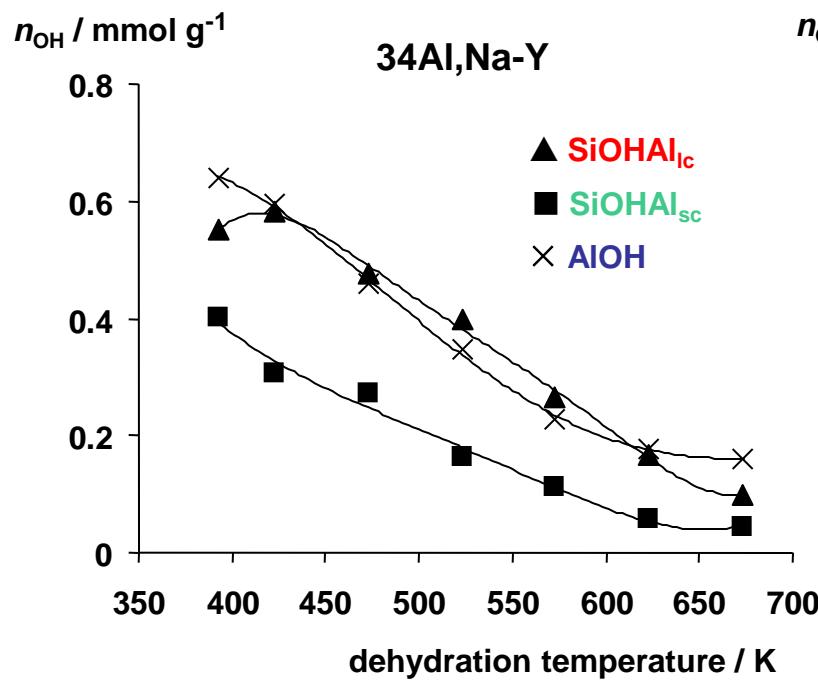
- SOQE = 6.2 MHz
- $\delta_{\text{iso}} = 6 \text{ ppm}$



III. Tailoring of surface sites

Brønsted acid sites in zeolites prepared via exchange with multivalent cations (Al^{3+})

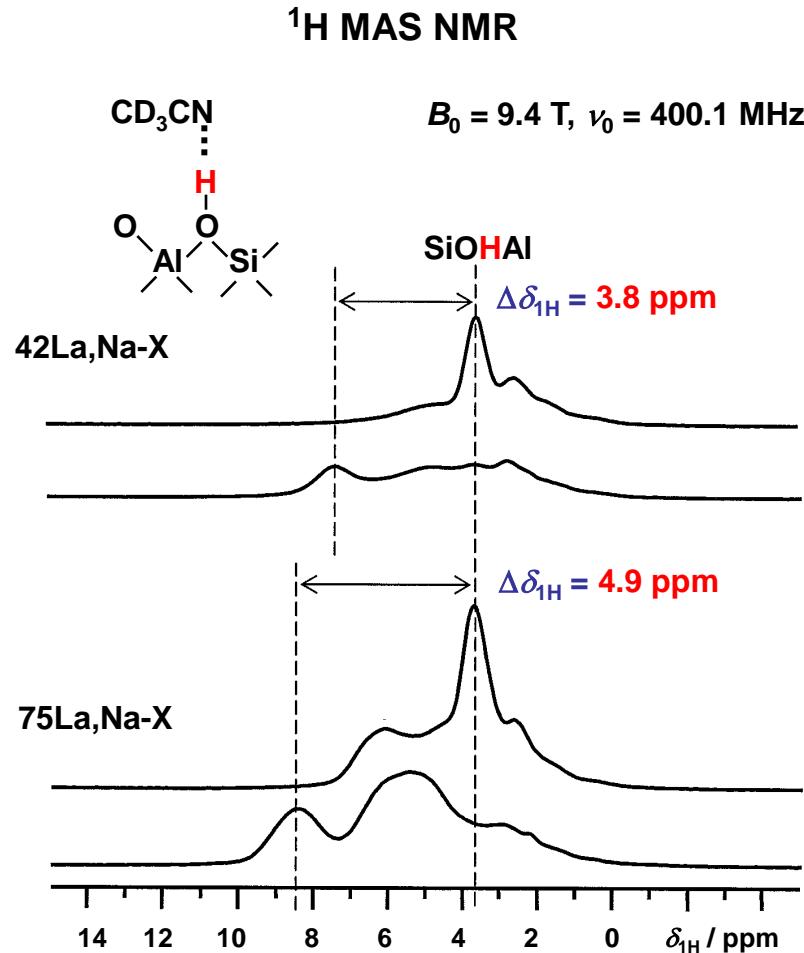
determination of the concentration of OH groups by evaluation of the ^1H MAS NMR intensities



cation-exchange degree and dehydration temperature affect the number of Brønsted sites

III. Tailoring of surface sites

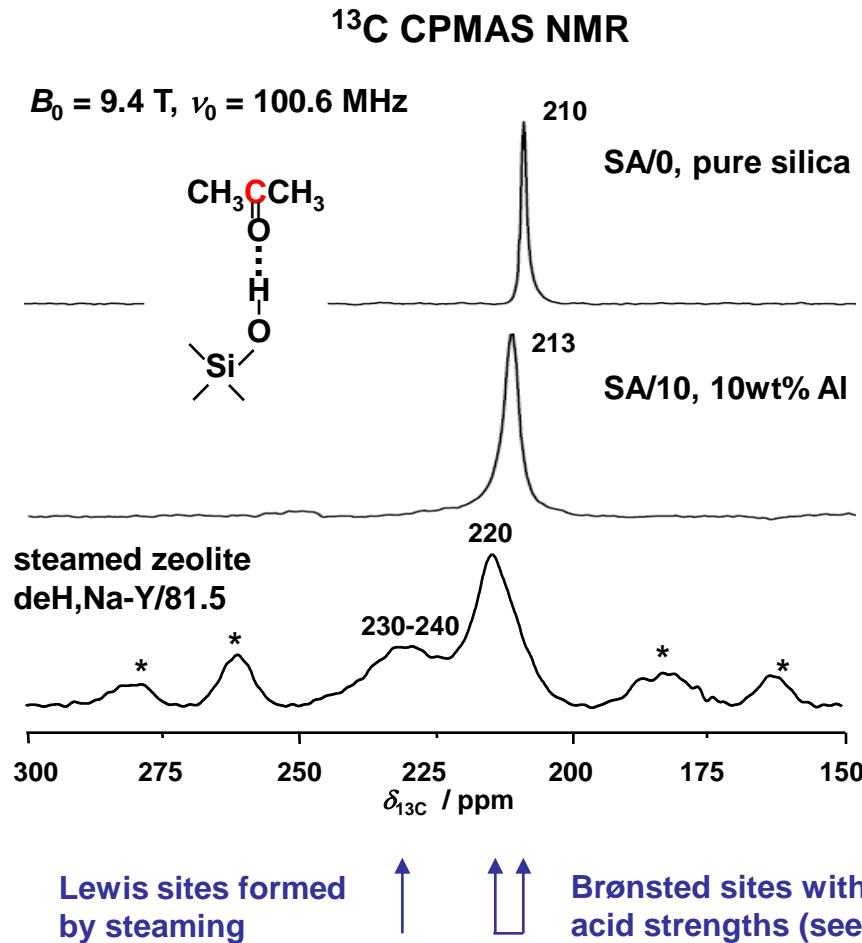
characterization of the Brønsted acid strength *via* acetonitrile-induced low-field shift $\Delta\delta_{1H}$



Low-field shift $\Delta\delta_{1H}$	Adsorbent and type of OH group
1.2 ppm	AlOH in MIL-53(Al)
3.6 ppm	H,Na-X ($\text{Si}/\text{Al} = 1.3$)
3.8 ppm	42La,Na-X and 32Al,Na-X ($\text{Si}/\text{Al} = 1.4$)
4.9 ppm	75La,Na-X ($\text{S}/\text{Al} = 1.4$)
5.1 ppm	H,Na-Y ($\text{Si}/\text{Al} = 2.7$)
5.3 ppm	34Al,Na-Y and 63Al,Na-Y ($\text{Si}/\text{Al} = 2.7$)
5.7 ppm	42La,Na-Y and 75La,Na-Y ($\text{Si}/\text{Al} = 2.7$)
6.5 ppm	steamed deH,Na-Y/81.5 ($\text{Si}/\text{Al} = 6$)
6.7 ppm	H-MOR ($\text{Si}/\text{Al} = 10$)
7.0 ppm	dealuminated H,Na-Y ($\text{Si}/\text{Al} = 18$)
7.9 ppm	H-ZSM-5 ($\text{Si}/\text{Al} = 26$)

III. Tailoring of surface sites

characterization of Brønsted and Lewis acid sites via ^{13}C -2-acetone as probe molecule

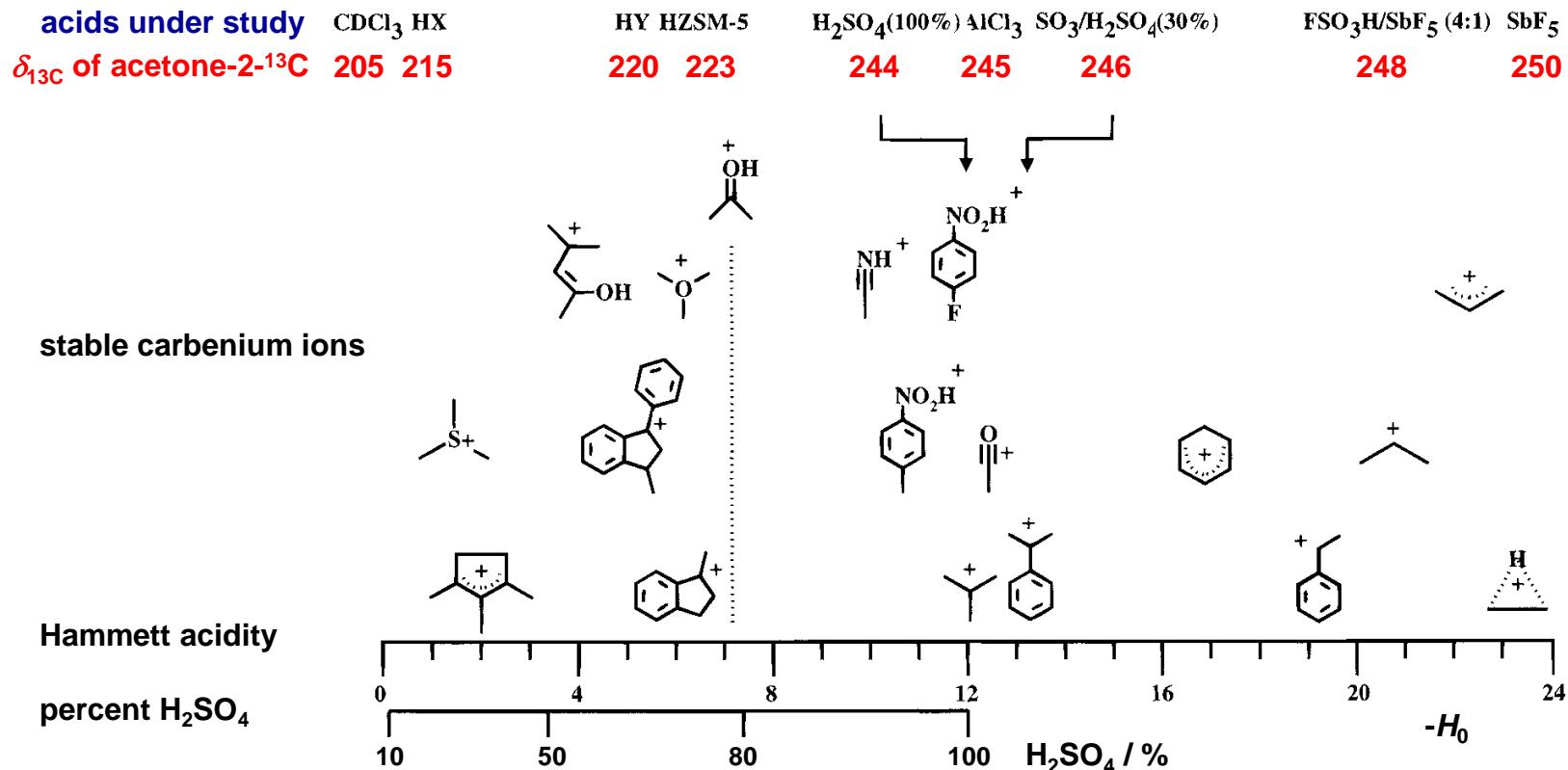


Materials	$\delta_{^{13}\text{C}}$	$\delta_{^{13}\text{C}}$
CDCl_3	205 ppm	0 ppm
SA/0	210 ppm	5 ppm
SA/10	213 ppm	8 ppm
H,Na-X	215 ppm	10 ppm
SA/70	216 ppm	11 ppm
H,Na-Y	220 ppm	15 ppm
ZSM-5	223 ppm	18 ppm
Lewis sites	230-240 ppm	25-35 ppm

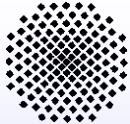
J.F. Haw et al., Accounts of Chemical Research 29 (1996) 259.

III. Tailoring of surface sites

comparison of different acidity scales



J.F. Haw et al., Acc. Chem. Res. 29 (1996) 259.



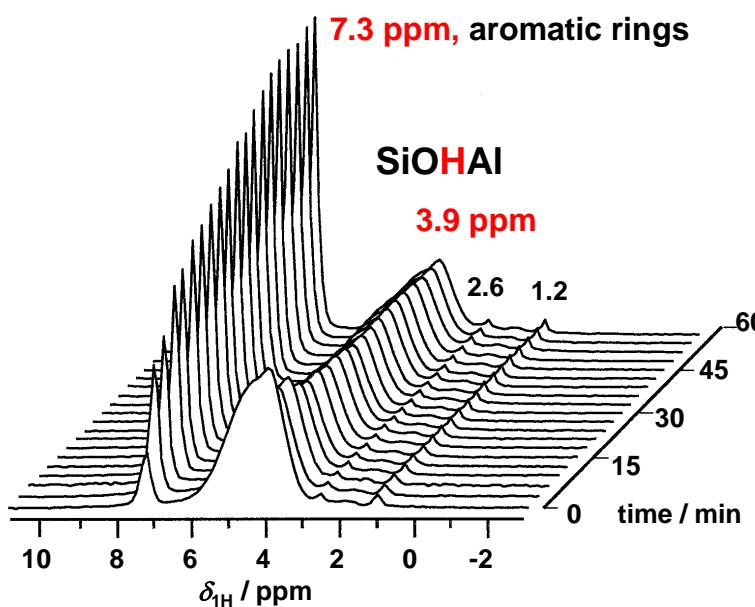
III. Tailoring of surface sites

H/D exchange kinetics as an acidity scale

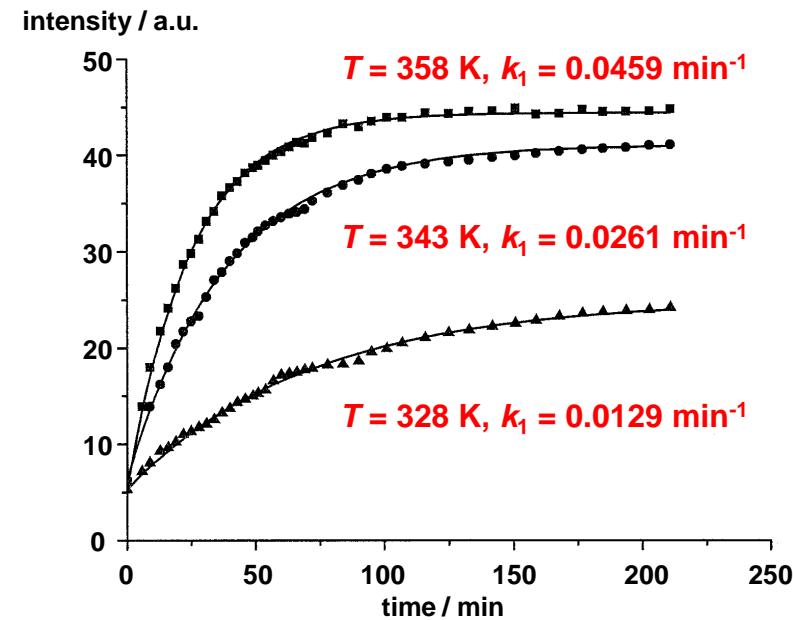
in situ ^1H MAS NMR studies of H/D exchange in zeolite $\text{H},\text{Na-Y}$ loaded with ethylbenzene ($\text{C}_6\text{D}_5\text{C}_2\text{H}_5$)

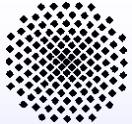
stack plot of ^1H MAS NMR spectra recorded at $T = 358\text{ K}$

$B_0 = 9.4\text{ T}$, $\nu_0 = 400.1\text{ MHz}$



H/D exchange rates at $T = 328 - 358\text{ K}$



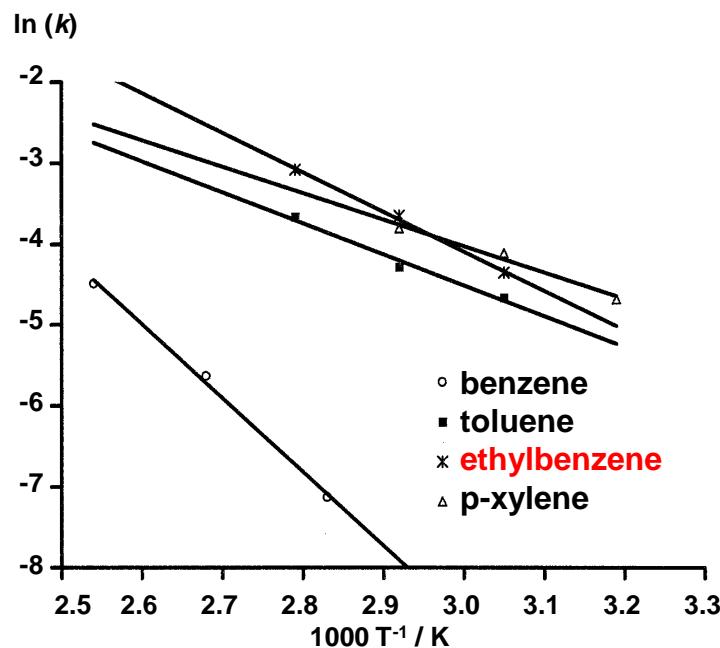


III. Tailoring of surface sites

H/D exchange kinetics as an acidity scale

in situ ^1H MAS NMR spectroscopy of H/D exchange in zeolites H,Na-Y ($n_{\text{Si}}/n_{\text{Al}} = 2.7$), 75La,Na-Y ($n_{\text{Si}}/n_{\text{Al}} = 2.7$), and H-ZSM-5 ($n_{\text{Si}}/n_{\text{Al}} = 26$)

deuterated aromatics on zeolite H,Na-Y



activation energies E_A of H/D exchange and low-field shifts $\Delta\delta_{1\text{H}}$ upon adsorption of CD₃CN:

catalyst	molecule	$E_A / \text{kJ mol}^{-1}$	$\Delta\delta_{1\text{H}} / \text{ppm}$
H,Na-Y	benzene	76	
	ethylbenzene	41	
	toluene	32	
	p-xylene	27	
H,Na-Y	benzene	76	5.1
La,Na-Y	benzene	67	5.7
H-ZSM-5	benzene	46	7.9

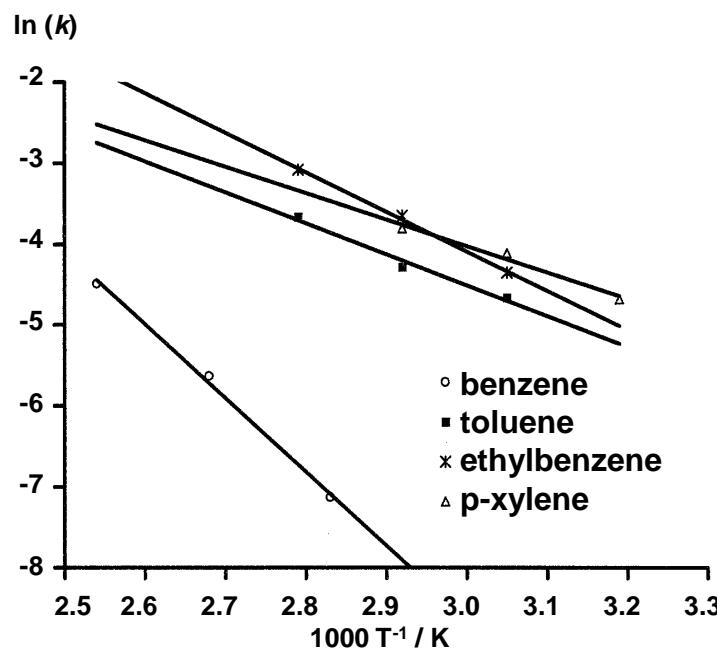


III. Tailoring of surface sites

H/D exchange kinetics as an acidity scale

in situ ^1H MAS NMR spectroscopy of H/D exchange in zeolites H,Na-Y ($n_{\text{Si}}/n_{\text{Al}} = 2.7$), 75La,Na-Y ($n_{\text{Si}}/n_{\text{Al}} = 2.7$), and H-ZSM-5 ($n_{\text{Si}}/n_{\text{Al}} = 26$)

deuterated aromatics on zeolite H,Na-Y



activation energies E_A of H/D exchange and low-field shifts $\Delta\delta_{1\text{H}}$ upon adsorption of CD_3CN :

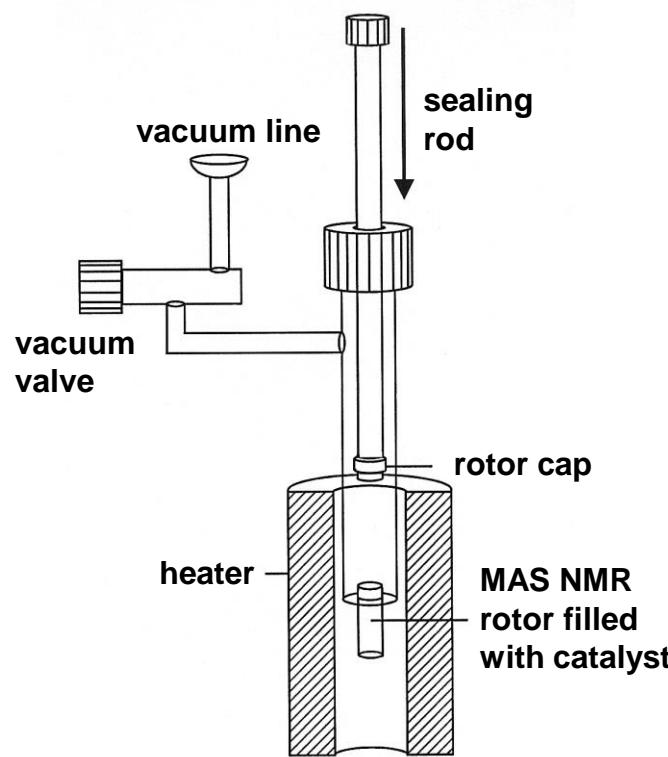
catalyst	molecule	$E_A / \text{kJ mol}^{-1}$	$\Delta\delta_{1\text{H}} / \text{ppm}$
H,Na-Y	benzene	76	
	ethylbenzene	41	
	toluene	32	
	p-xylene	27	
H,Na-Y	benzene	76	5.1
La,Na-Y	benzene	67	5.7
H-ZSM-5	benzene	46	7.9

IV. Catalytic investigations

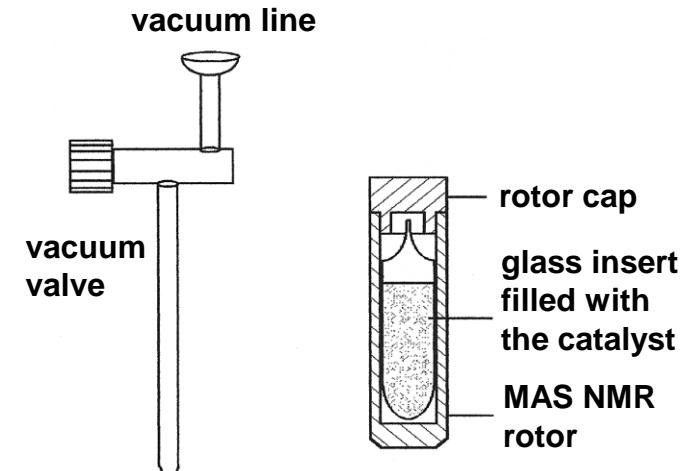
IV. Catalytic investigations

preparation of catalyst samples for *in situ* MAS NMR studies under **batch** conditions

dehydration, loading, and sealing of the catalyst filled in an MAS NMR rotor inside a vacuum equipment



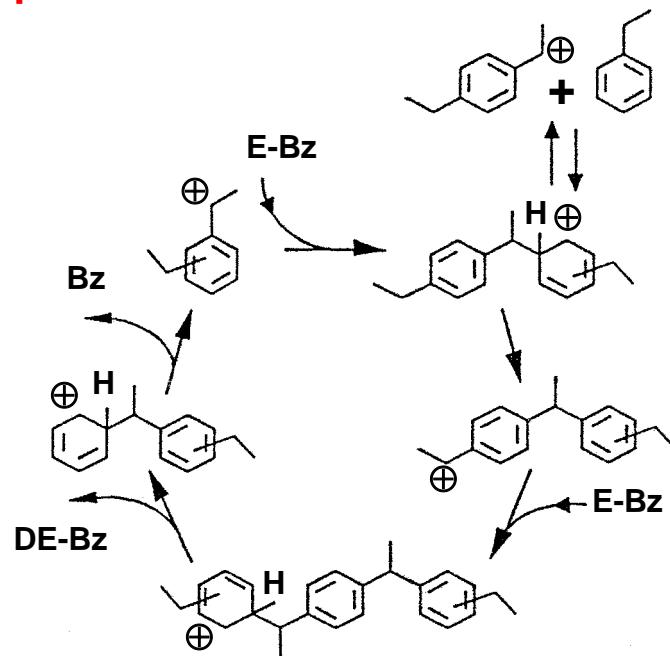
dehydration and loading of the catalyst inside the glass insert (e.g. commercial Wilmad MAS NMR inserts for 4 mm and 7 mm rotors)



IV. Catalytic investigations

mechanisms of the ethylbenzene disproportionation

Streitwieser-Reif mechanism for the homogeneously catalyzed ethylbenzene disproportionation



suggested reaction mechanisms for the heterogeneously catalyzed reaction on zeolites:

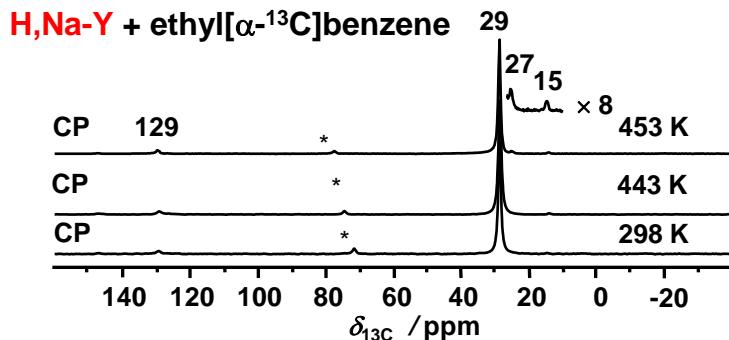
- via diphenylethane intermediates in large-pore zeolites
- dealkylation/realkylation with free ethene or alkoxy species in medium-pore zeolites

IV. Catalytic investigations

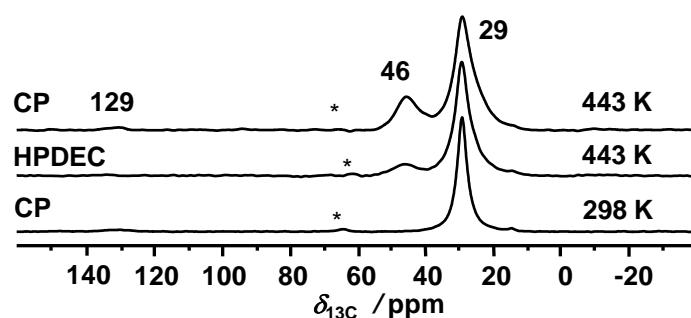
mechanisms of the ethylbenzene disproportionation

¹³C MAS NMR investigation of the ethylbenzene conversion on large-pore zeolites H,Na-Y and 63Al,Na-Y

¹³C MAS NMR



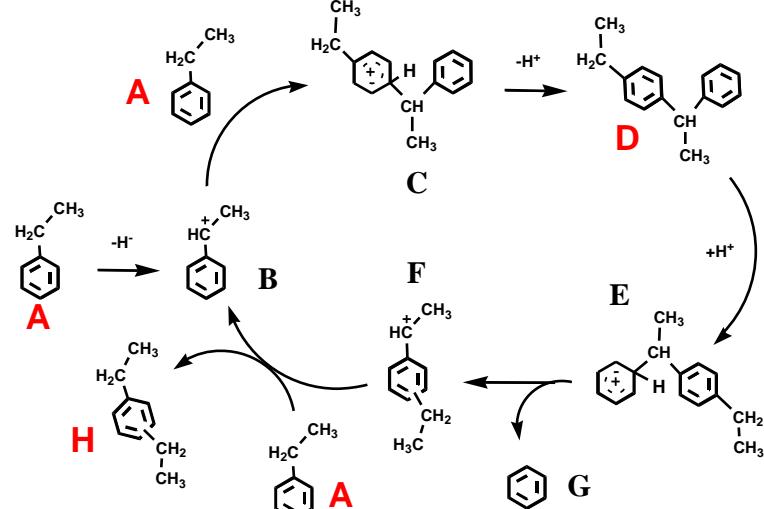
63Al,Na-Y + ethyl[α -¹³C]benzene



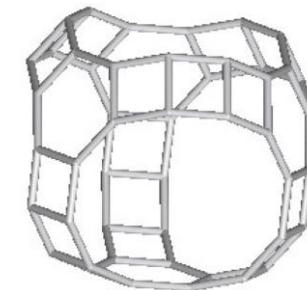
assignment: 27 ppm
29 ppm

diethylbenzene (H)
ethylbenzene (A)

reaction mechanism



in supercages with
diameter of 1.2 nm

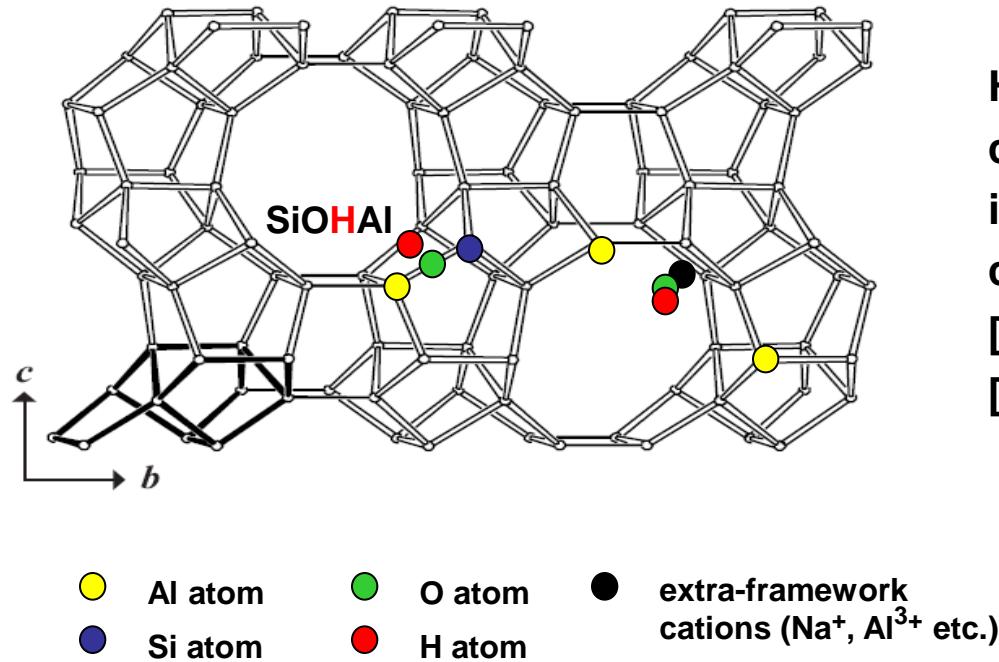


diphenylethane (D)
aromatic carbons

IV. Catalytic investigations

mechanisms of the ethylbenzene disproportionation

structure of medium-pore zeolite ZSM-5:



$\text{H}^+ \text{n}[\text{Al}_n\text{Si}_{96-n}\text{O}_{192}]$
crossing intersections with
interconnecting 10-ring
channels
[100] 0.51 nm x 0.55 nm
[010] 0.53 nm x 0.56 nm



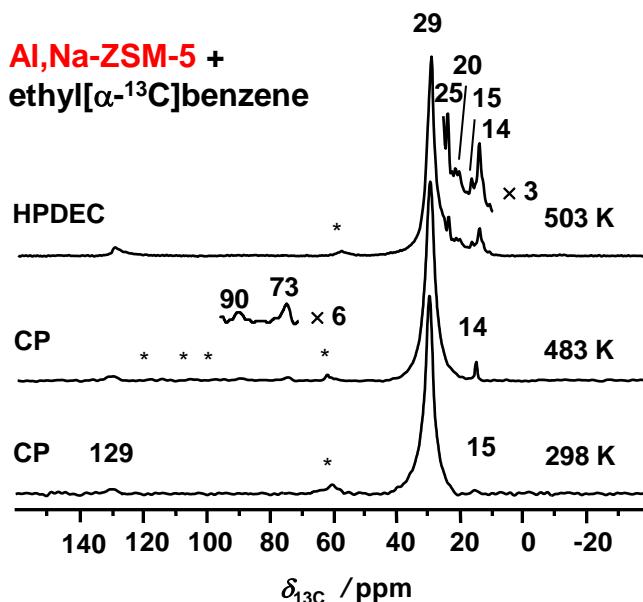
IV. Catalytic investigations

mechanism of the ethylbenzene disproportionation

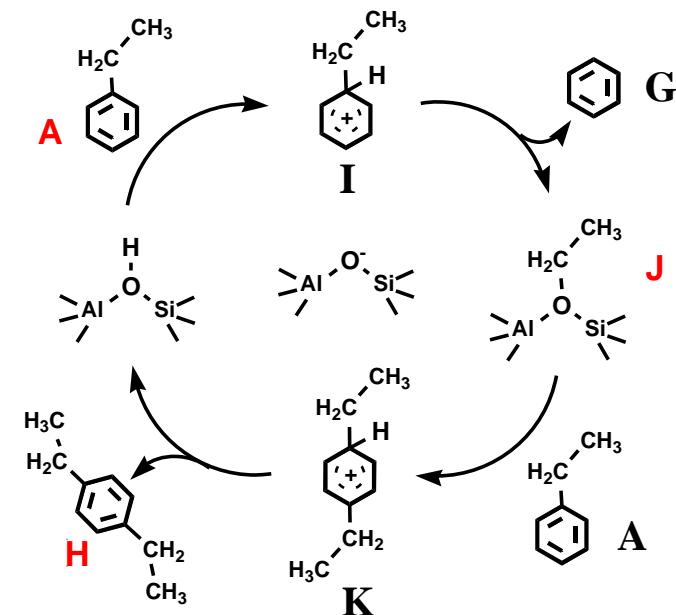
¹³C MAS NMR investigation of the ethylbenzene conversion on medium-pore zeolite ZSM-5

¹³C MAS NMR
mechanism

Al₂Na-ZSM-5 +
ethyl[α -¹³C]benzene



reaction



assignment: 25 ppm diethylbenzene (H)
29 ppm ethylbenzene (A)

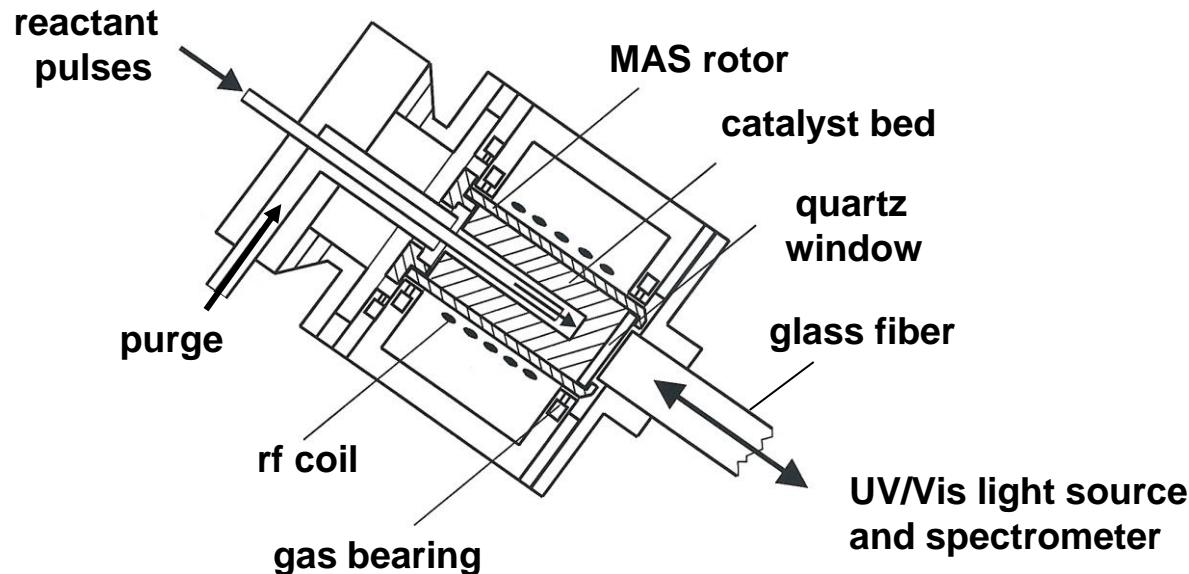
73 ppm
90 ppm
129 ppm surface ¹³C-1-ethoxy groups (J)
oligomeric alkoxy groups
aromatic carbons

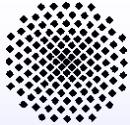


IV. Catalytic investigations

continuous-flow (CF) and pulsed-flow (PF) MAS NMR spectroscopy

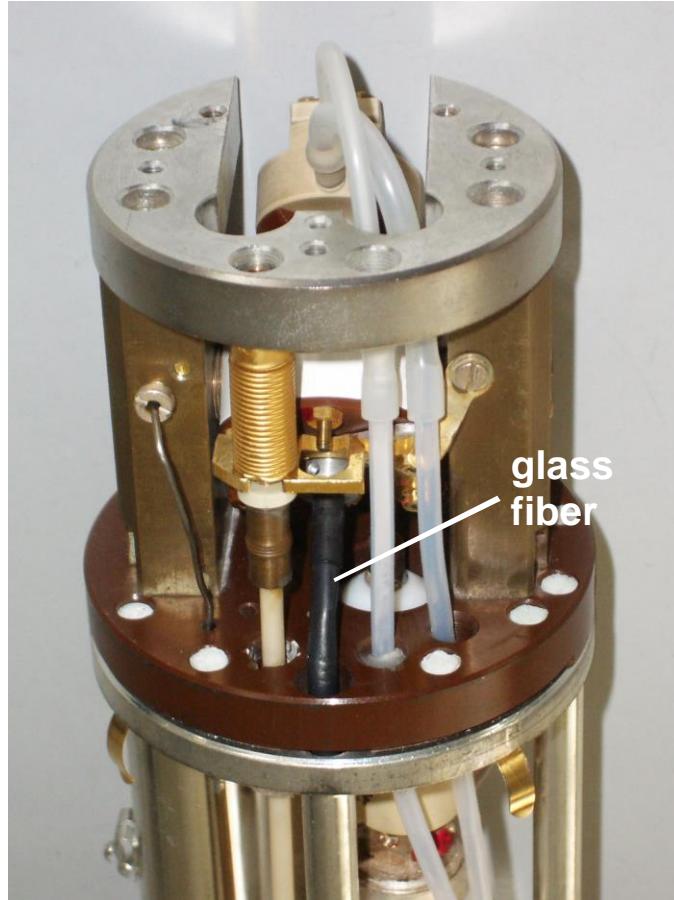
coupling of MAS NMR and UV/Vis spectroscopy by installation of a quartz fiber at the bottom of the MAS NMR stator





IV. Catalytic investigations

continuous-flow (CF) and pulsed-flow (PF) MAS NMR spectroscopy

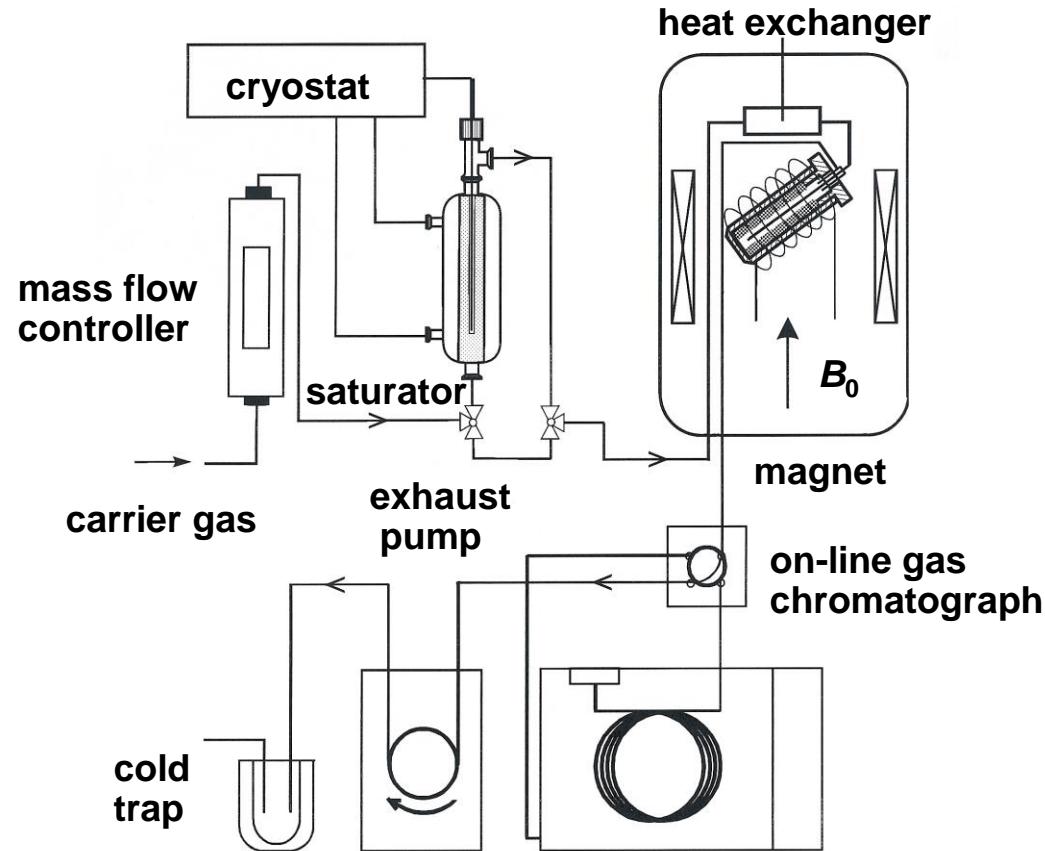


7 mm Bruker MAS NMR probe
equipped with a glass fiber (left) and
UV/Vis light source and spectrometer
of Avantes (bottom)



IV. Catalytic investigations

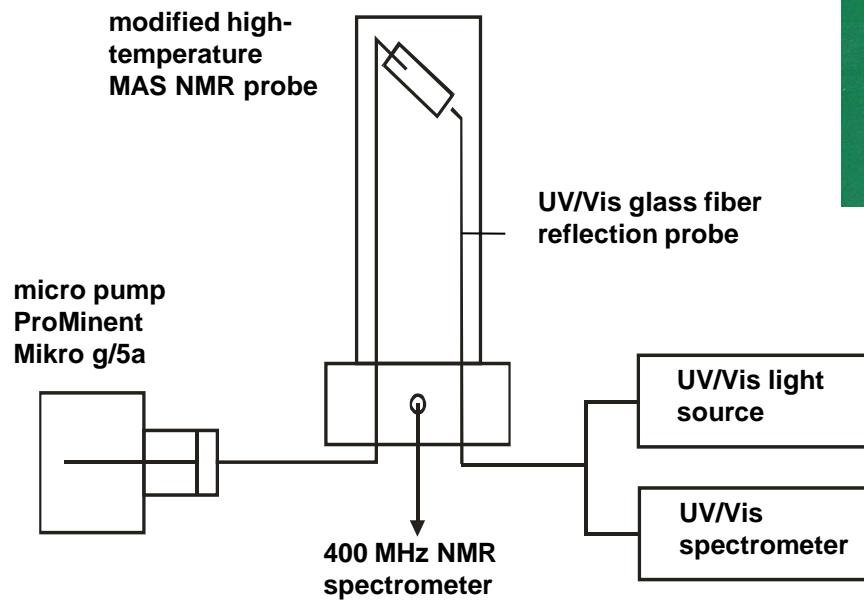
continuous-flow (CF) MAS NMR spectroscopy

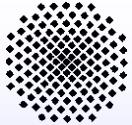


IV. Catalytic investigations

pulsed-flow (PF) MAS NMR spectroscopy

connection of a micro pump with the *in situ* MAS NMR probe



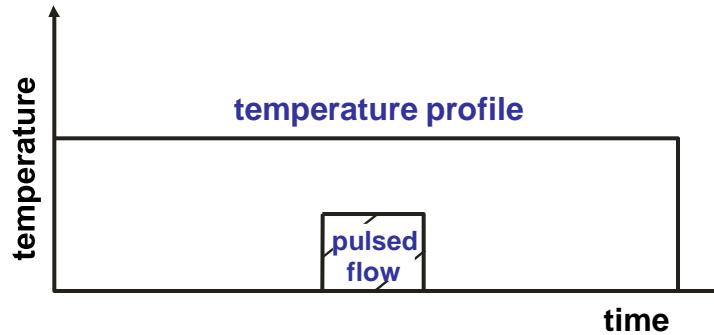


IV. Catalytic investigations

pulsed-flow (PF) MAS NMR-UV/Vis spectroscopy

injection of liquid reactants into the spinning MAS NMR rotor *via* a micro-pulse pump

pulsed-flow experiment



pulsed-flow experiments:

- study of the time dependence of the conversion of reactants
- study of the isotopic exchange of reactants at high temperatures with well-defined starting time



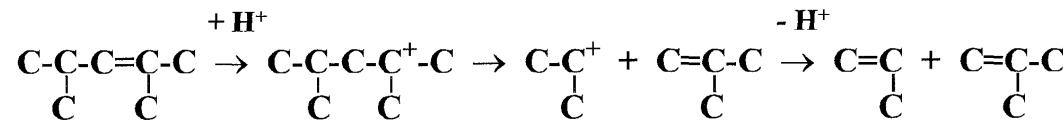
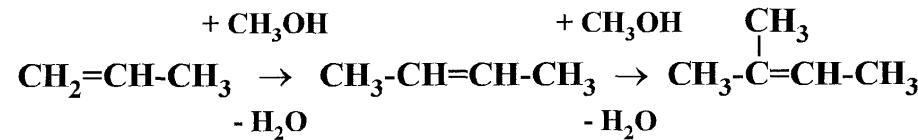
pump Mikro g/5 of Fa. ProMinent, Germany, for single pulses with volumes of 2 to 50 μl



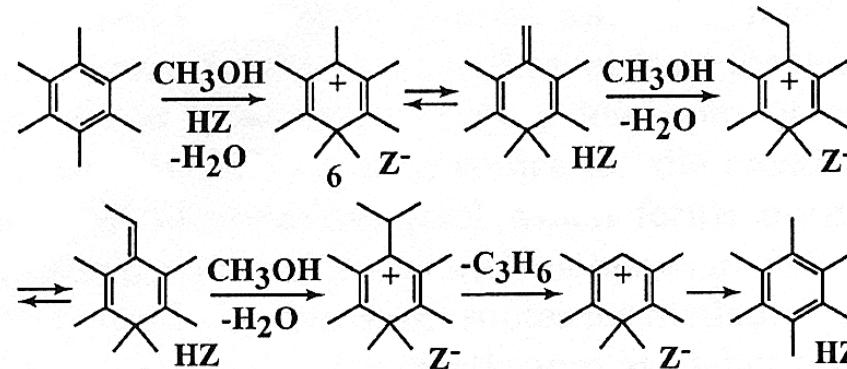
IV. Catalytic investigations

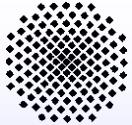
mechanism of the methanol-to-olefin (MTO) conversion on acidic zeolites

via olefinic compounds (H. Schulz, M. Wei, Microporous Mesoporous Mater. 29 (1999) 205)



via polyalkylaromatics (J.F. Haw et al., Acc. Chem. Res. 36 (2003) 317)





IV. Catalytic investigations

mechanism of the methanol-to-olefin (MTO) conversion on acidic zeolites

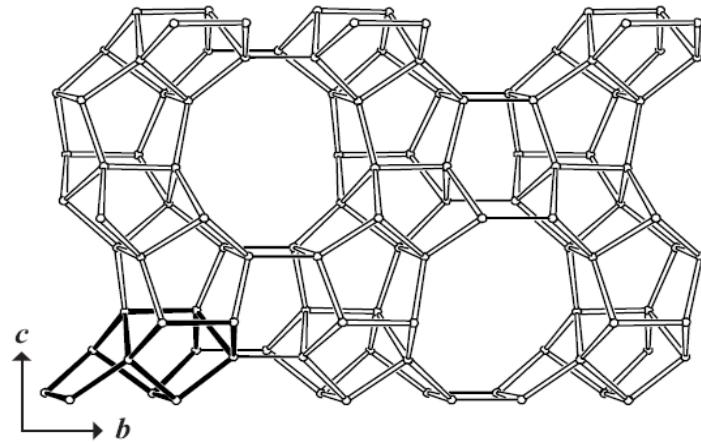
H-ZSM-5: Structure type MFI

$\text{H}^+ \text{n}[\text{Al}_n \text{Si}_{96-n} \text{O}_{192}]$

crossing intersections at
interconnecting 10-ring channels

[100] 0.51 nm x 0.55 nm

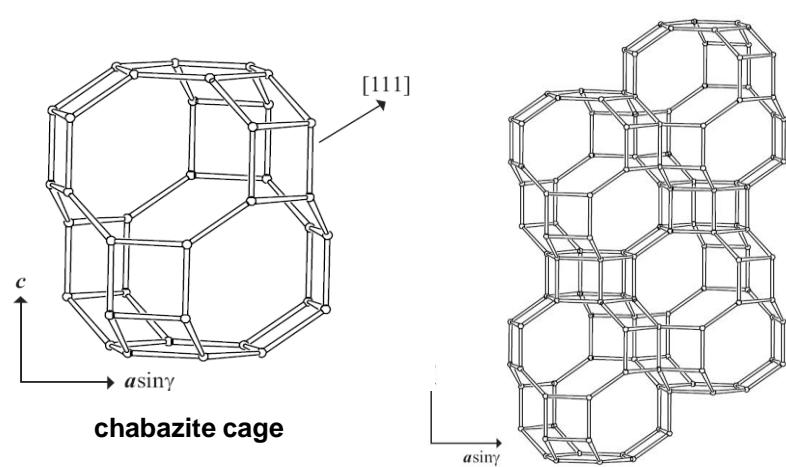
[010] 0.53 nm x 0.56 nm



H-SAPO-34: Structure type CHA

$\text{H}^+ \text{n}[\text{Al}_{18} \text{P}_{18-n} \text{Si}_n \text{O}_{72}]$

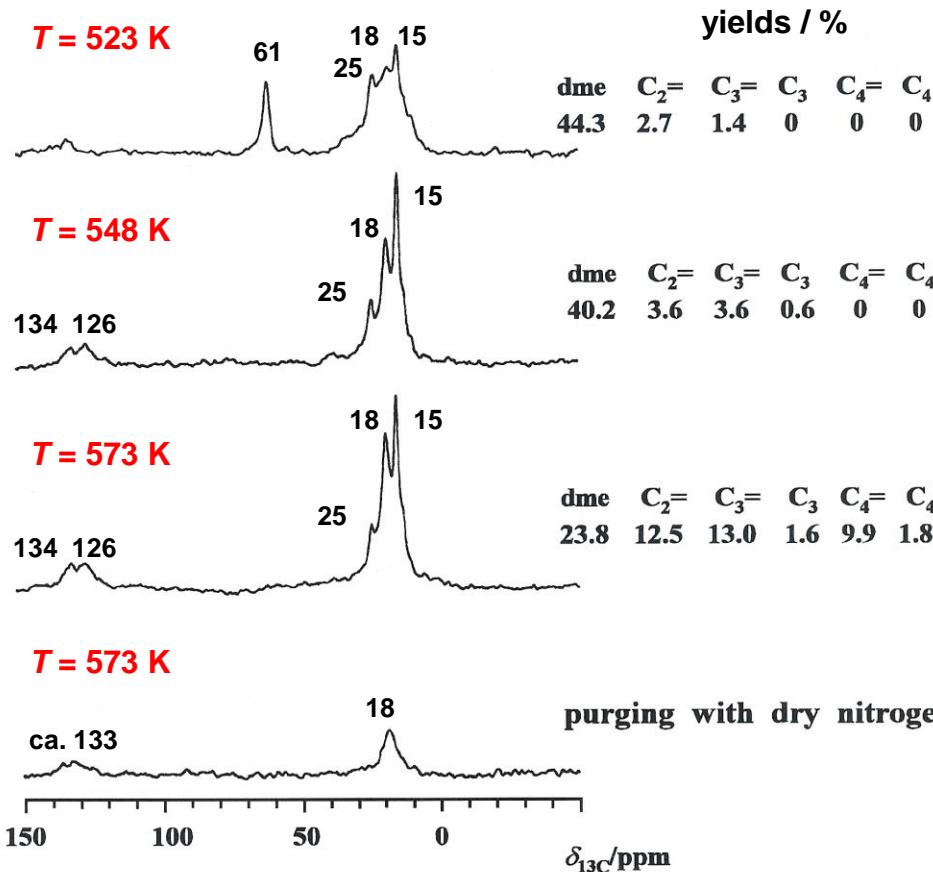
chabazite cages accessible by
8-ring windows perpendicular to
[001] 0.38 nm x 0.38 nm



IV. Catalytic investigations

mechanism of the methanol-to-olefin (MTO) conversion on acidic zeolites

in situ CF ^{13}C MAS NMR study of ZSM-5 ($W_{\text{cat}}/F_{\text{me}} = 25 \text{ gh/mol}$)



T < 548 K:

mixture of olefinic and aromatic compounds, such as:

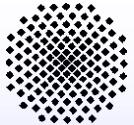
3-hexene (14.4, 25.9, 131.2 ppm)
2,4-hexadiene (17.2, 126.2, 132.5 ppm)

....
hexamethylbenzene (17.6, 132.1 ppm)

T = 573 K:

polymethylaromatics remain after purging, such as:

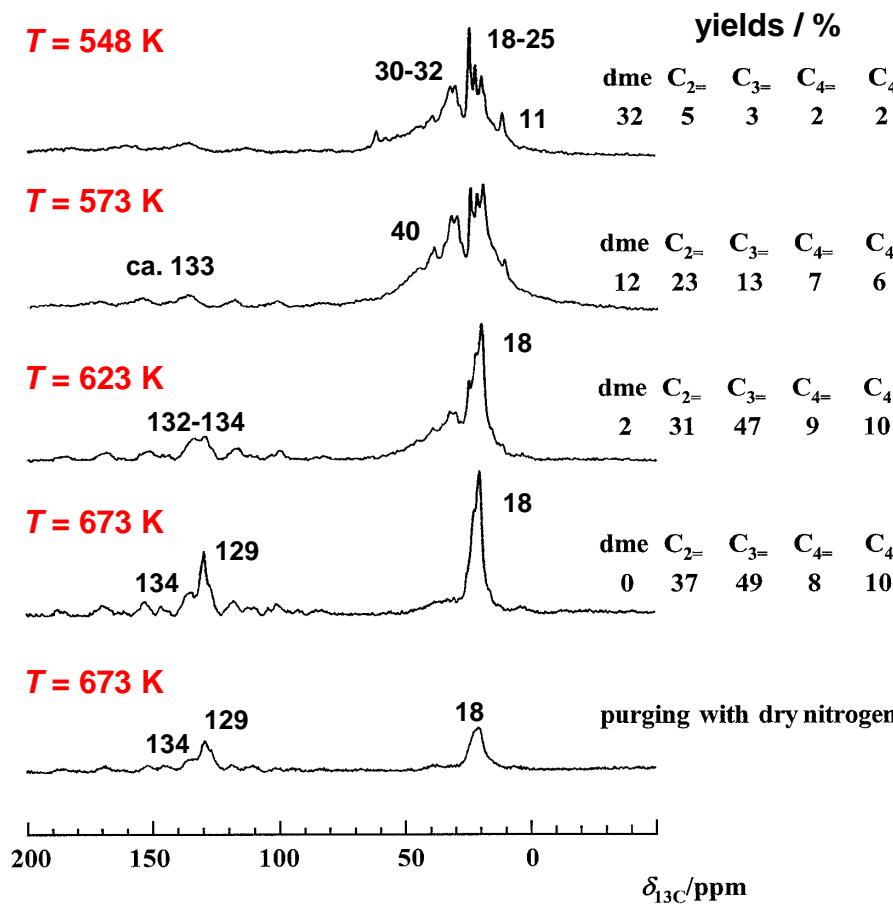
toluene (20.3, 128.5, 129.0 ppm)
....
hexamethylbenzene (17.6, 132.1 ppm)



IV. Catalytic investigations

mechanism of the methanol-to-olefin (MTO) conversion on acidic zeolites

in situ CF ^{13}C MAS NMR study of SAPO34 ($W_{\text{cat}}/F_{\text{me}} = 25 \text{ gh/mol}$)



$T < 573 \text{ K}$:

mixture of olefinic and aromatic compounds, such as:

2-methyl-2-butene (9.3-22.5, 118.8, 131.8 ppm)

2,4-hexadiene (19.5, 132.5 ppm)

....

tetramethylbenzene (18.9, 131.1, 134.0 ppm)

$T > 573 \text{ K}$:

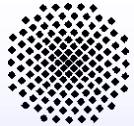
domination of polymethyl-aromatics, such as:

toluene (20.3, 128.5, 129.0 ppm)

....

trimethylbenzene (21.2, 127.4, 137.6 ppm)

hexamethylbenzene (17.6, 132.1 ppm)

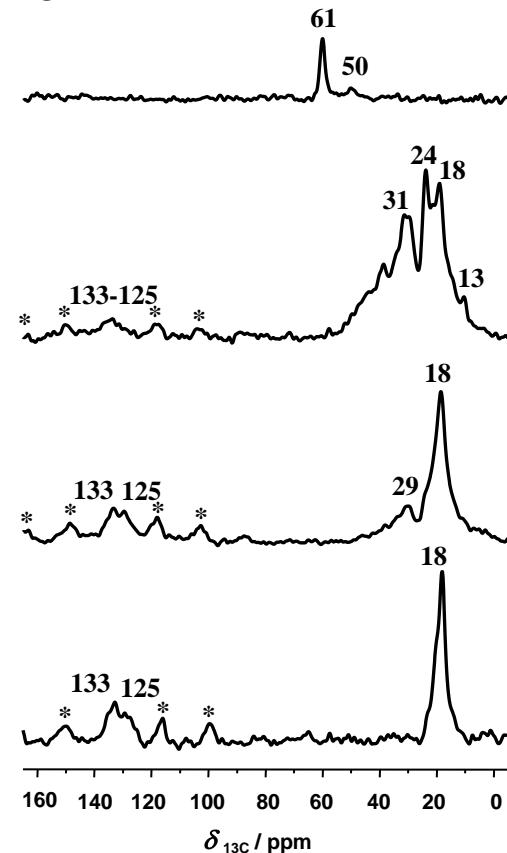


IV. Catalytic investigations

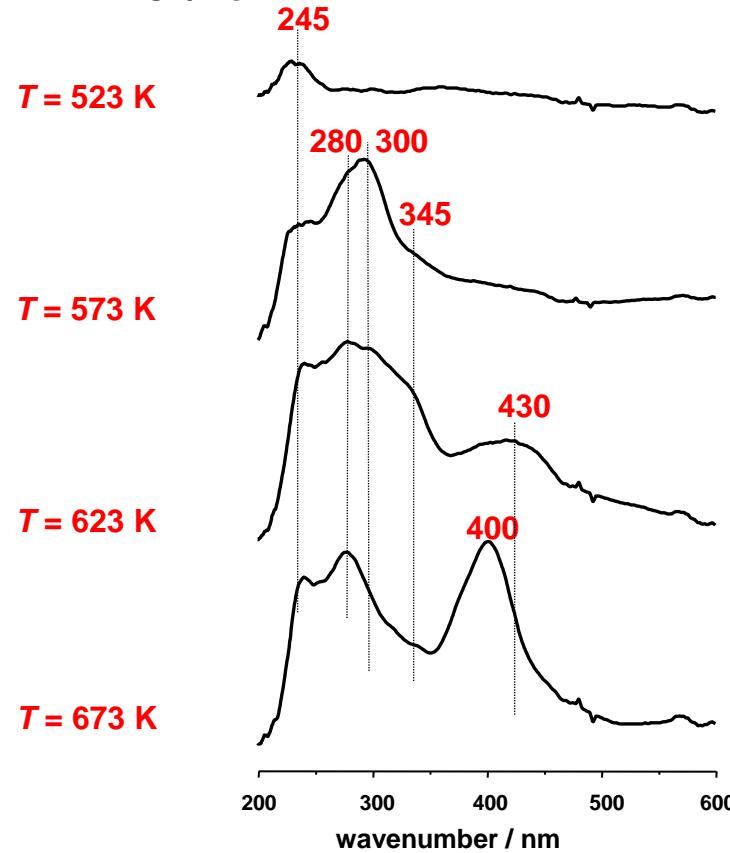
mechanism of the methanol-to-olefin (MTO) conversion on acidic zeolites

comparing study of organic deposits formed on H-SAPO-34 ($W_{\text{cat}}/F_{\text{me}} = 25 \text{ gh/mol}$)

^{13}C MAS NMR



UV/Vis



245 nm: dienes

280 nm: polyalkylaromatics

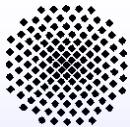
300 nm: monoenylic carbénium

345 nm: dienylic carbénium

400 nm: polycyclic coke

430 nm: trienylic carbénium





IV. Catalytic investigations

side-chain H/D exchange of ethylbenzene on steamed zeolite deH_nNa-Y/81.5

in situ PF ^1H MAS NMR
experiments:

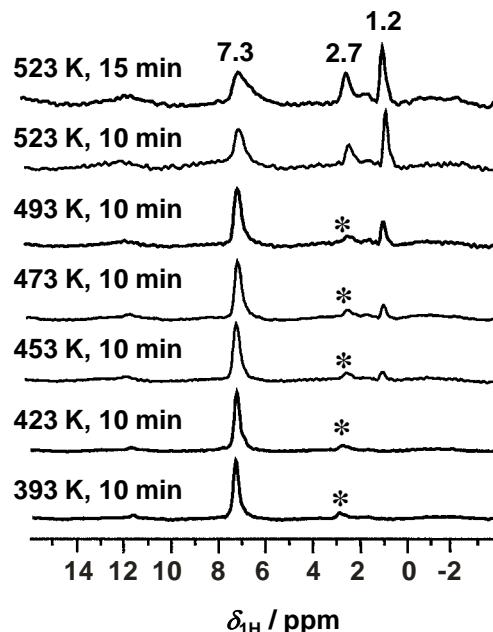
- pulses of 7.8 mg ethyl- d_5 -benzene
- 32 scans per spectrum with repetition time of 10 s at 9.4 T
- sample spinning rate of ca. 2 kHz

message:

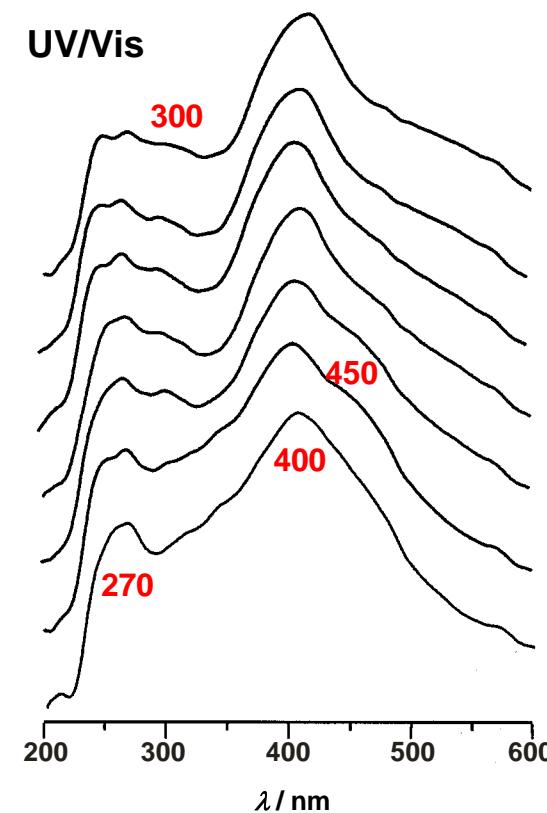
- regioselective H/D exchange at 443 to 463 K (^1H MAS NMR)
- different types of carbenium ions (UV/Vis)



^1H MAS NMR



UV/Vis

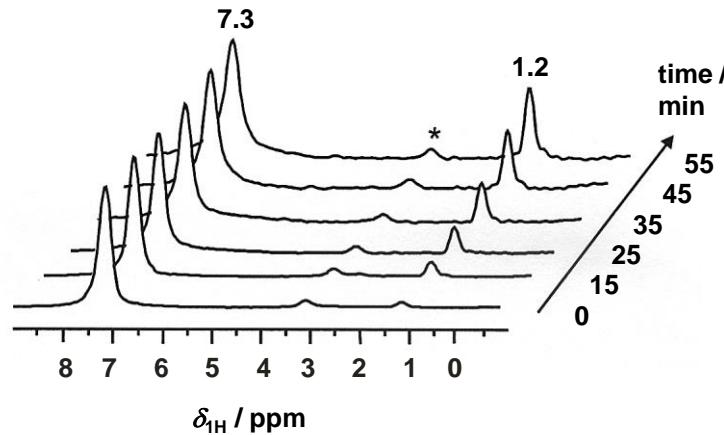


IV. Catalytic investigations

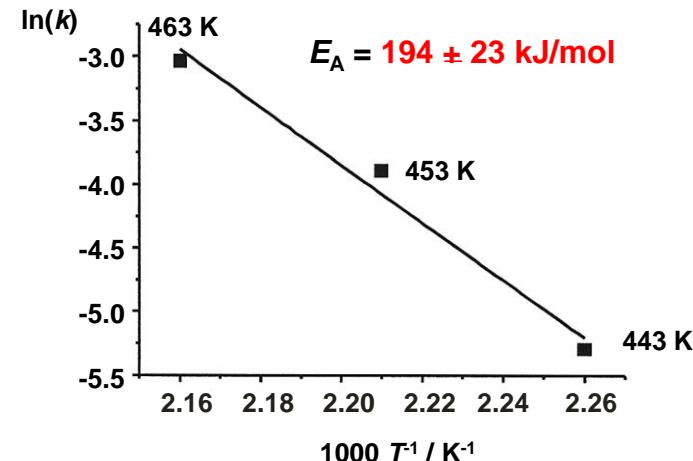
side-chain H/D exchange of ethylbenzene on steamed zeolite deH_xNa-Y/81.5

$\text{C}_6\text{H}_5\text{CD}_2\text{CD}_3$ on dealuminated zeolite deH_xNa-Y/81.5 (24.5 Al^{ex}/u.c., 10.9 SiOHAl /u.c.)

in situ PF ^1H MAS NMR



Arrhenius plot



activation energy of the regioselective H/D exchange (194 kJ/mol) indicates that a hydride transfer reaction is the rate determining step



IV. Catalytic investigations

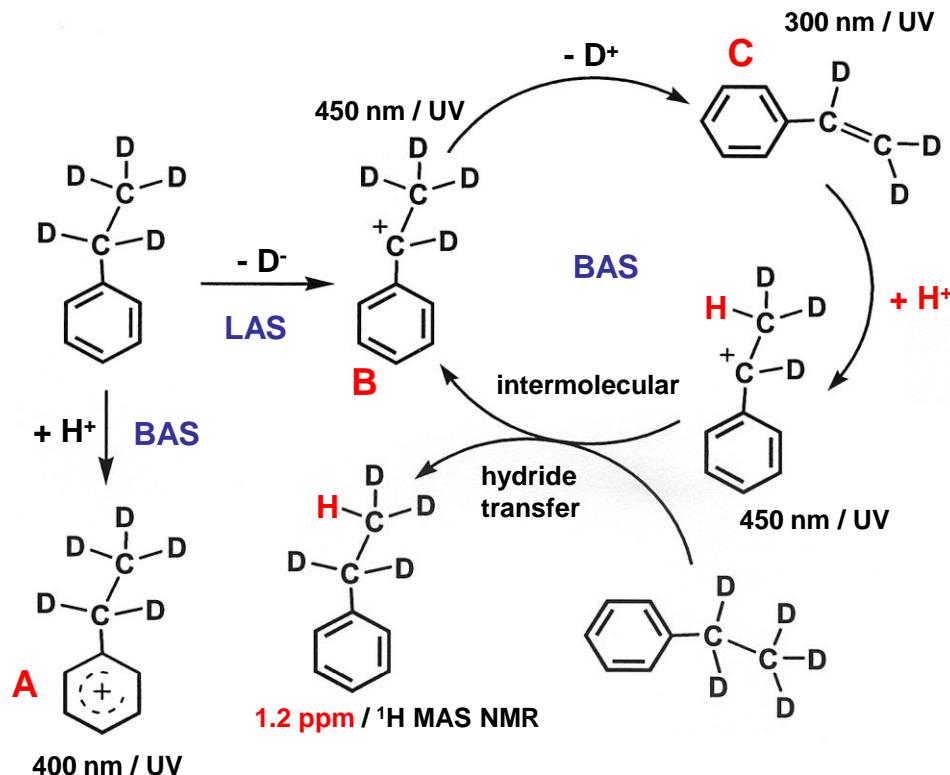
side-chain H/D exchange of ethylbenzene on steamed zeolite deH_xNa-Y/81.5

¹H MAS NMR:

- selective H/D exchange of methyl groups (**1.2 ppm**)
- activation energy of **194 kJ/mol** indicates hydride transfer

UV/Vis:

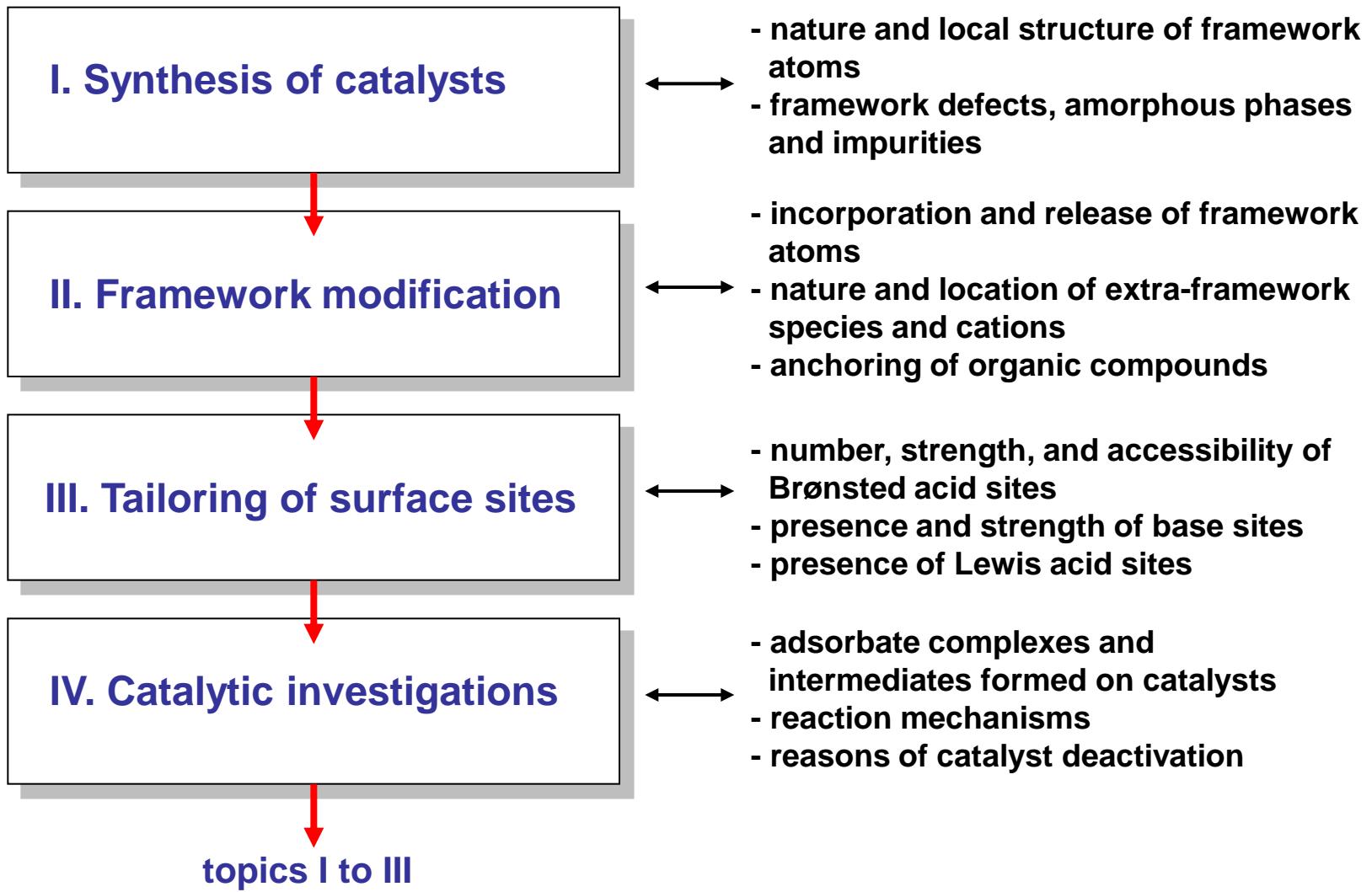
- ethylcyclohexadienyl carbenium ions at **BAS** (400 nm), **A**
- sec-ethylphenyl carbenium ions at **LAS** (450 nm), **B**
- styrene at **BAS** (300 nm), **C**

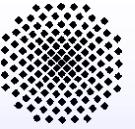


BAS: Broensted acid site

LAS: Lewis acid site

Solid-state NMR of solid catalysts





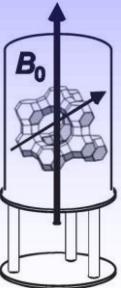
Thanks to

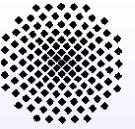
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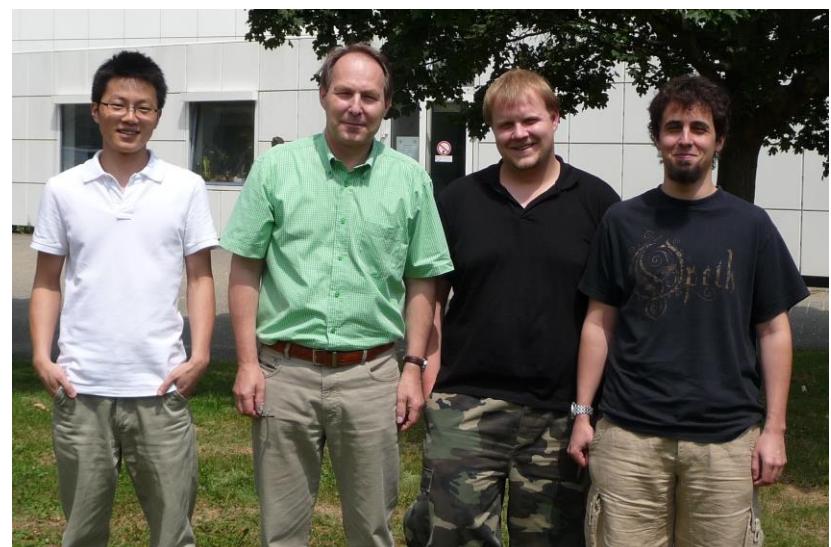
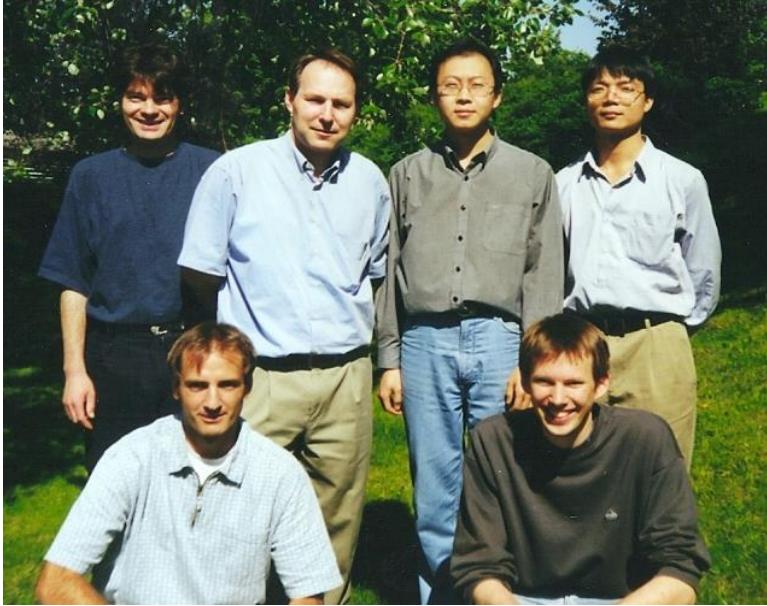
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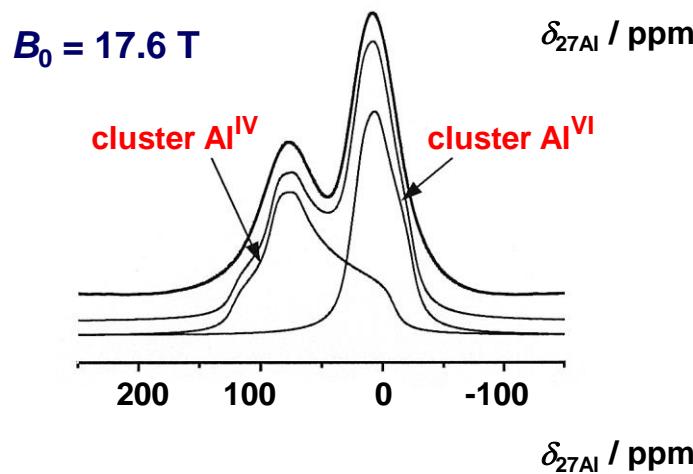
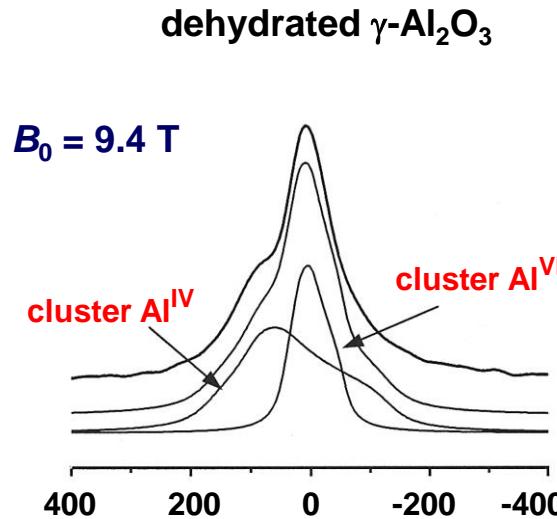




Thanks to



^{27}Al spin-echo NMR studies of reference materials



- spectroscopic parameters of cluster Al^{IV}:
 - QCC = 8.5 MHz, $\eta = 0.8$
 - $\delta_{\text{iso}} = 68 \pm 5 \text{ ppm}$
 - $I_{\text{rel}} = 60 \%$
- spectroscopic parameters of cluster Al^{VI}:
 - QCC = 5.5 MHz, $\eta = 0.7$
 - $\delta_{\text{iso}} = 12 \pm 5 \text{ ppm}$
 - $I_{\text{rel}} = 40 \%$