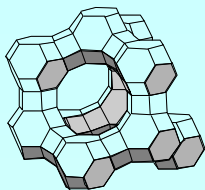


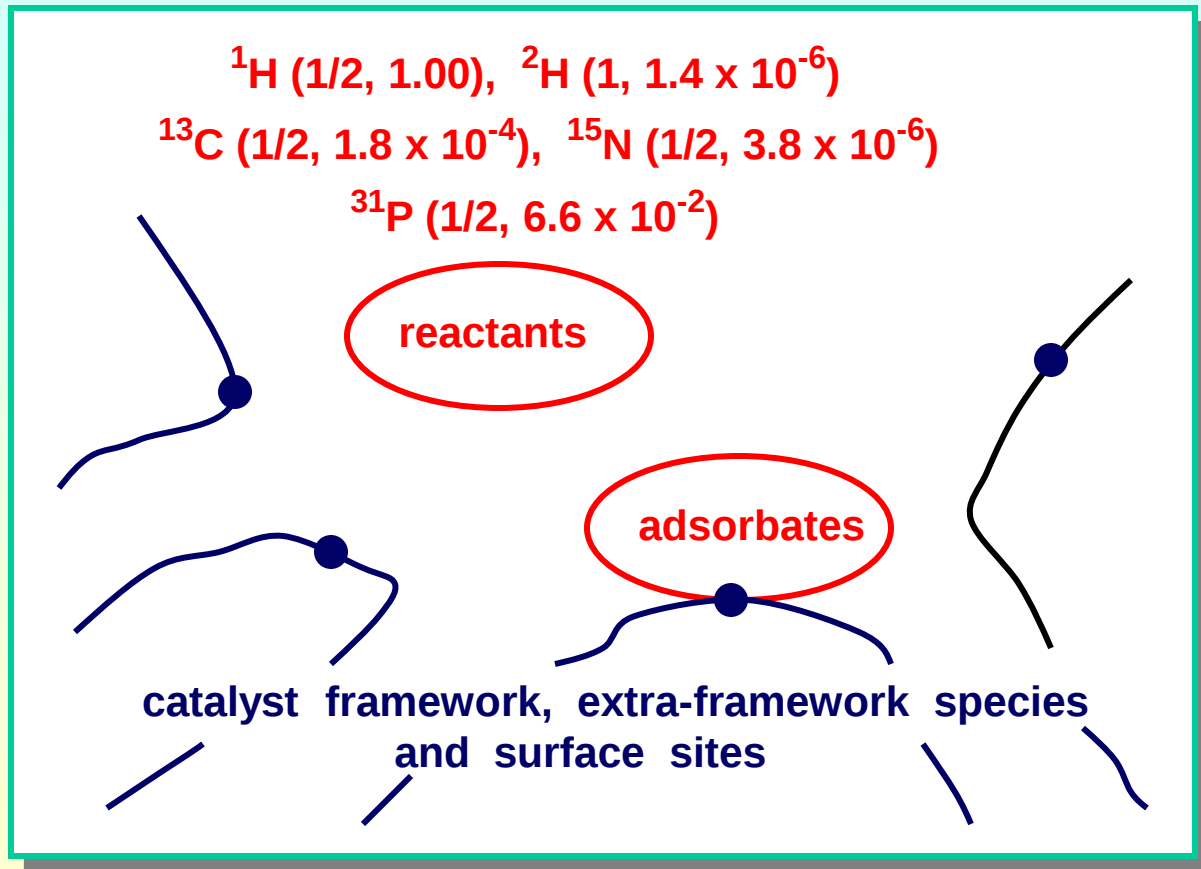
In situ NMR spectroscopy in heterogeneous catalysis

Michael Hunger

***Institute of Chemical Technology
University of Stuttgart, Germany***

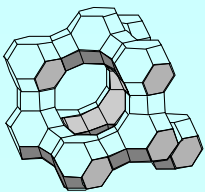


Examples of nuclei accessible for in situ NMR in heterogeneous catalysis



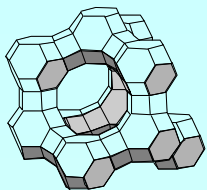
^7Li	(3/2, 0.27)
^{11}B	(3/2, 0.13)
^{17}O	(5/2, 1.1×10^{-5})
^{23}Na	(3/2, 9.2×10^{-2})
^{27}Al	(5/2, 0.21)
^{29}Si	(1/2, 3.7×10^{-4})
^{31}P	(1/2, 6.6×10^{-2})
^{51}V	(7/2, 0.38)
^{67}Zn	(5/2, 1.2×10^{-2})
^{71}Ga	(3/2, 5.6×10^{-2})
^{133}Cs	(7/2, 4.7×10^{-2})

isotope (nuclear spin, relative sensitivity in comparison with ^1H)



Contents

- specific problems of NMR spectroscopy on working catalysts
- experimental techniques applied for studies under batch and continuous-flow (CF) conditions
- solid-state NMR investigations of heterogeneous reaction systems under *in situ* conditions:
 - zeolite framework and surface sites
 - reactions catalyzed by basic zeolites
 - reactions catalyzed by acidic zeolites

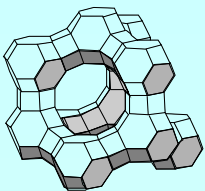


Specific problems of NMR on working catalysts

magnetization:

$$M_0 = \frac{N \gamma^2 h^2 I (I + 1) B_0}{(2\pi)^2 3 k_B T}$$

- absolute number of spins of $N > 10^{19}$ per gram (^1H NMR)
- decrease of magnetization M_0 with increasing temperature T
- rapid chemical exchange of adsorbate complexes at elevated temperatures
- observation times of 10 ms (flow conditions) to hours (batch conditions)
- quenching of signals in the neighborhood of paramagnetic and ferromagnetic sites
- broadening of signals due to solid-state interactions

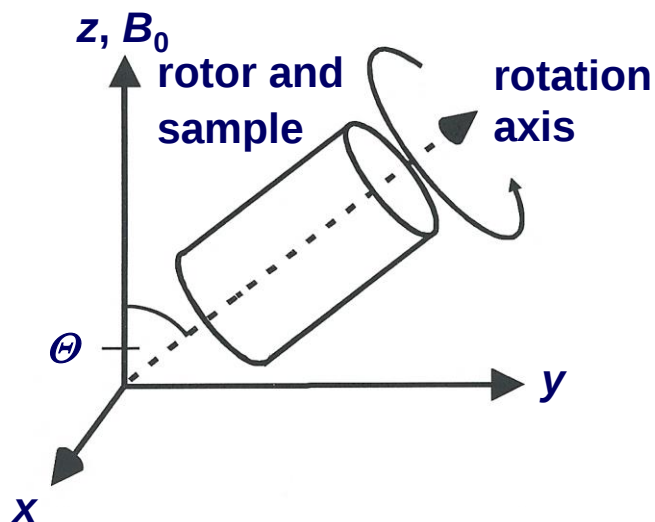


Solid-state NMR techniques

spin $I = \frac{1}{2}$:

- magic angle spinning (**MAS**)

$$\nu_{\text{CSA,DI,1QI}} = f \{3\cos^2\Theta - 1\} \rightarrow \Theta = 54.7^\circ$$



spin $I > \frac{1}{2}$:

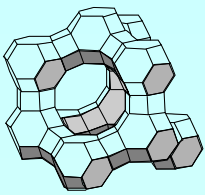
- double oriented rotation (**DOR**)

$$\nu_{2\text{QI}} = f \{35\cos^4\Theta - 30\cos^2\Theta + 3\}$$

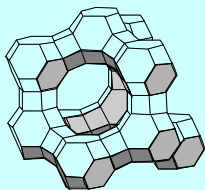
$$\rightarrow \Theta = 30.6^\circ$$

$$\Theta = 70.1^\circ$$

- multiple-quantum MAS NMR (**MQMAS**)
 - sampling of three- and five-quantum transitions
 - recording of spin-echoes free of anisotropic contributions



***Experimental techniques applied for studies
under batch and continuous-flow conditions***



Experimental approaches

- batch experiments, external reaction
 - sealed samples
 - heating in an external stove
- batch experiments, *in situ* reaction
 - sealed samples
 - high-temperature solid-state NMR probes
 - go-and-stop studies using a Laser heating system

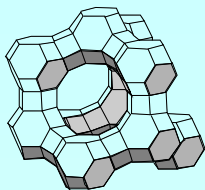
characteristics:

- accessible with commercial equipments
- infinite contact times

- flow experiments, external reaction
 - reaction in an external reactor
 - transfer of the loaded catalysts after quenching the reaction
- flow experiments, *in situ* reaction
 - continuous injection of reactants into the MAS NMR rotor reactor
 - high-temperature solid-state NMR probes

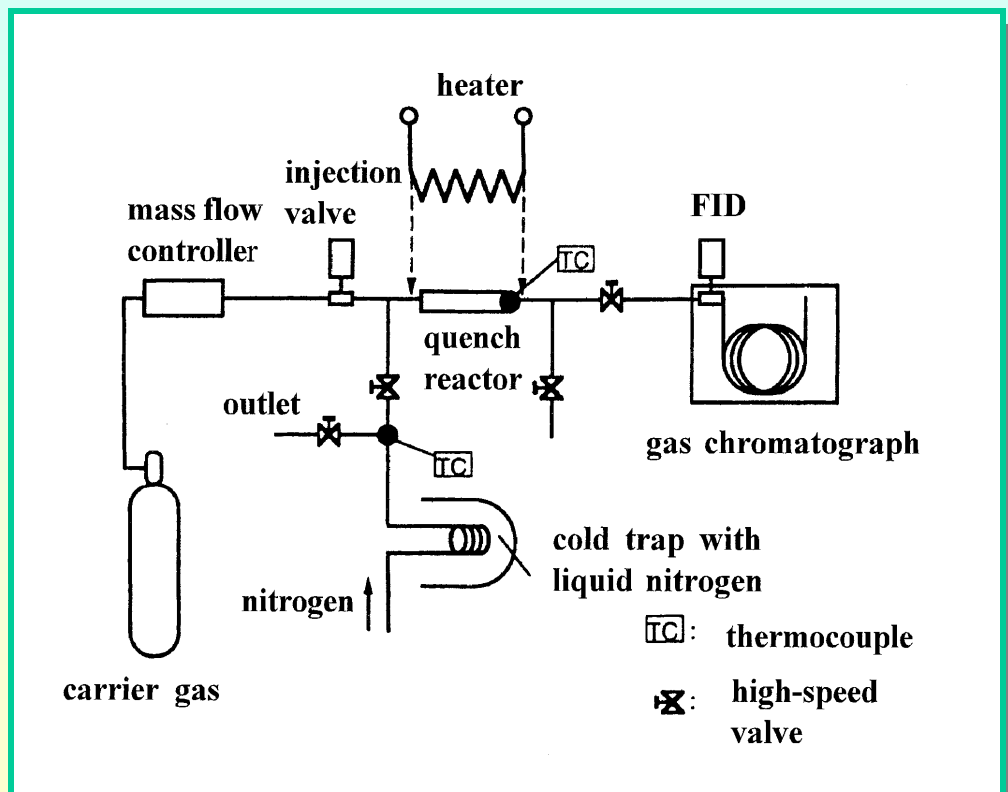
characteristics:

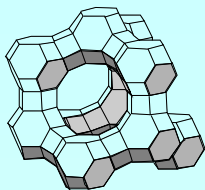
- self-made equipments
- study of reactions under steady state conditions



Go-and-stop experiments using an external reactor

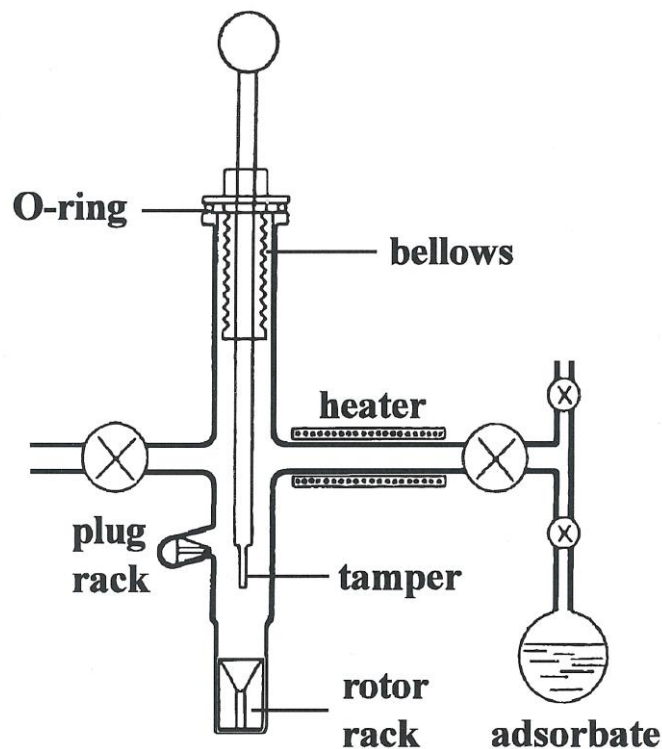
- pulse-quench technique:
 - conversion of reactants in an external fixed-bed reactor
 - rapid stopping of the reaction by pre-cooled nitrogen gas
- NMR investigations:
 - transfer of the catalyst loaded with reaction products into an MAS NMR rotor
 - measurements performed at room temperature

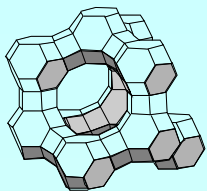




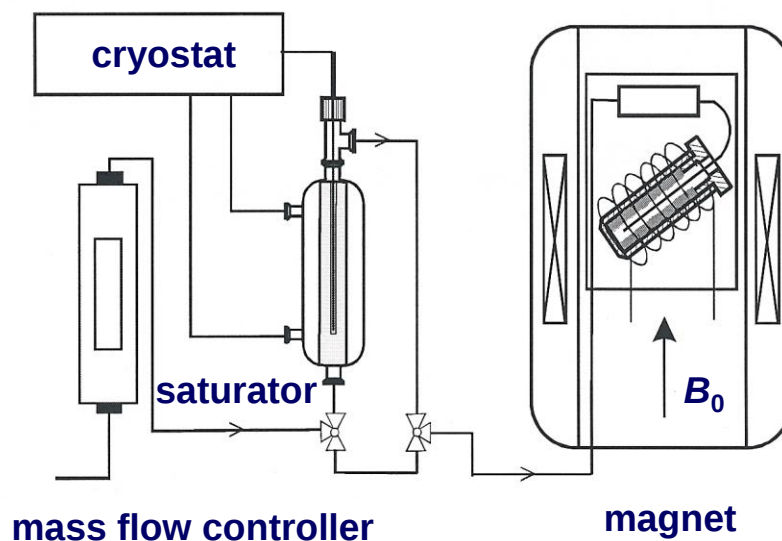
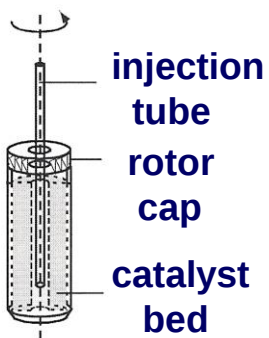
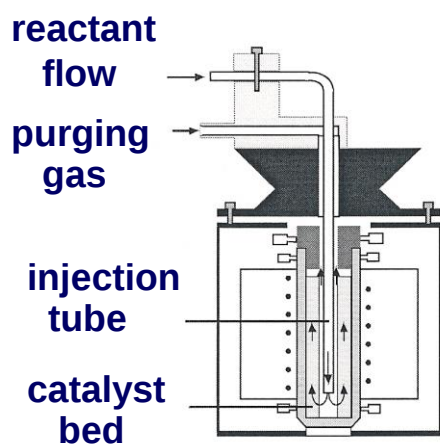
Approach for batch and continuous-flow experiments in an external reactor

- apparatus for evacuation, loading and catalysis on solid materials in an external reactor
- no contact to air during the transfer of the catalyst material into an MAS NMR rotor
- sealing of the MAS NMR rotor inside the apparatus

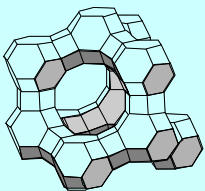




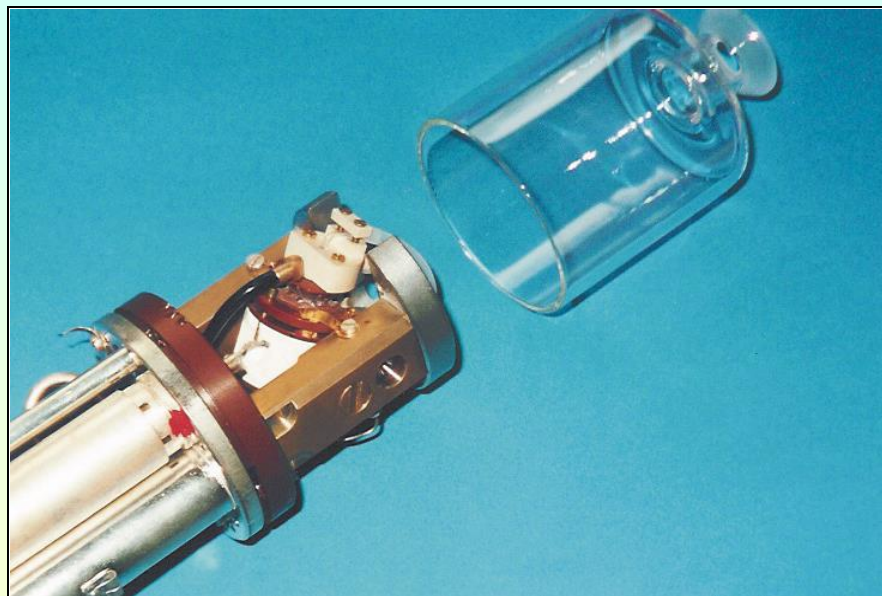
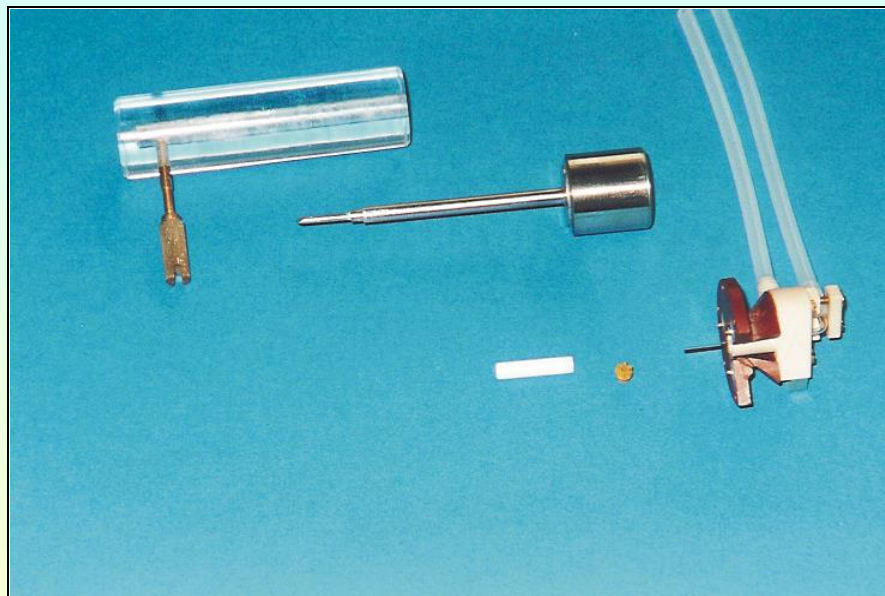
Continuous-flow (CF) MAS NMR technique



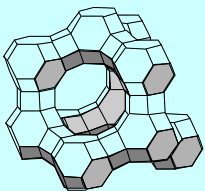
- continuous injection of reactants into a spinning MAS NMR rotor reactor ($T < 923$ K)



Continuous-flow (CF) MAS NMR technique



- **modified 4 mm Bruker MAS NMR probe equipped with an injection system**



Behavior of the high-temperature CF MAS NMR probe

- ^{207}Pb MAS NMR of $\text{Pb}(\text{NO}_3)_2$:

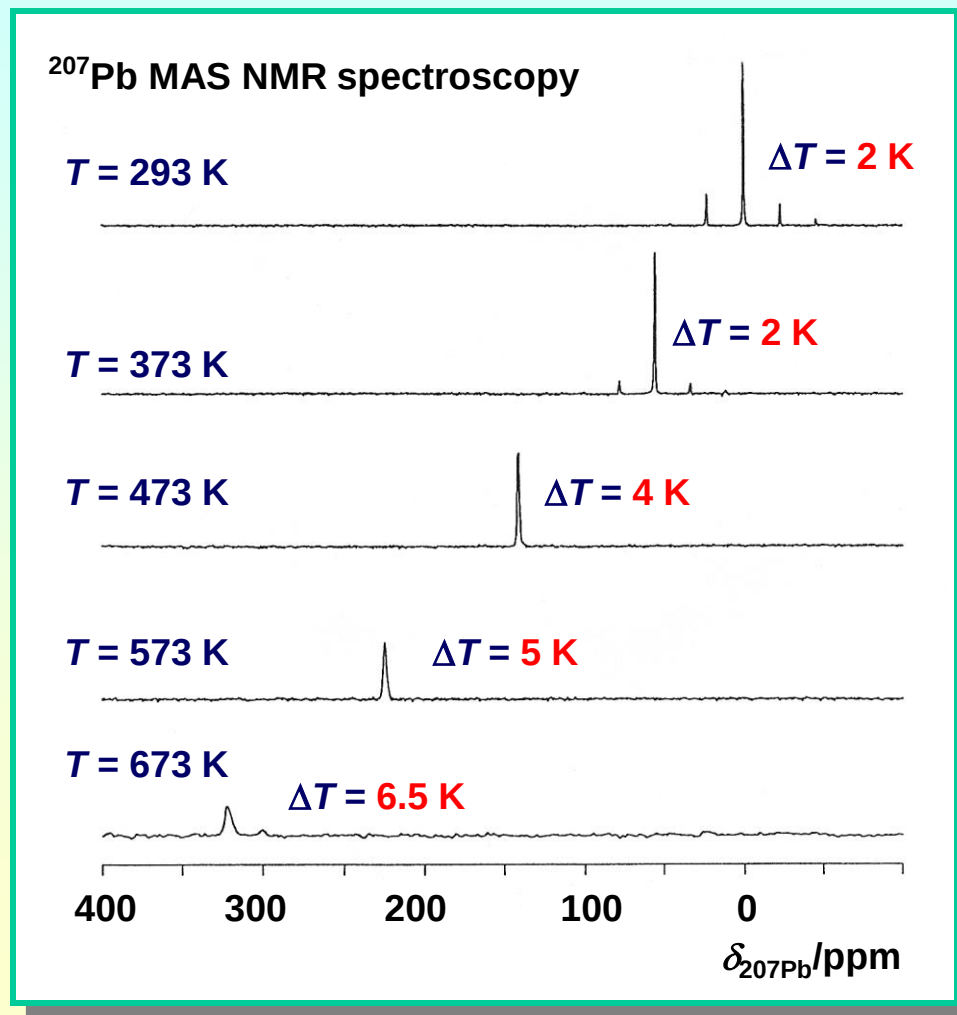
$$\Delta T / \Delta \delta = 1.29 \text{ K / ppm}^*$$

- modified 7 mm Doty MAS NMR probe DSI-740:

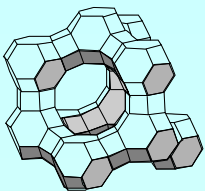
$$\nu_0 = 83.2 \text{ MHz}$$

$$\nu_{\text{rot}} = 2.5 \text{ kHz}$$

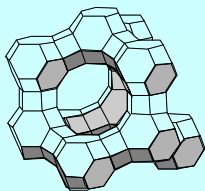
$$F_{\text{N}_2} = 15 \text{ ml/min}$$



* D.B. Ferguson et al., Anal. Chem. 67 (1995) 3342.

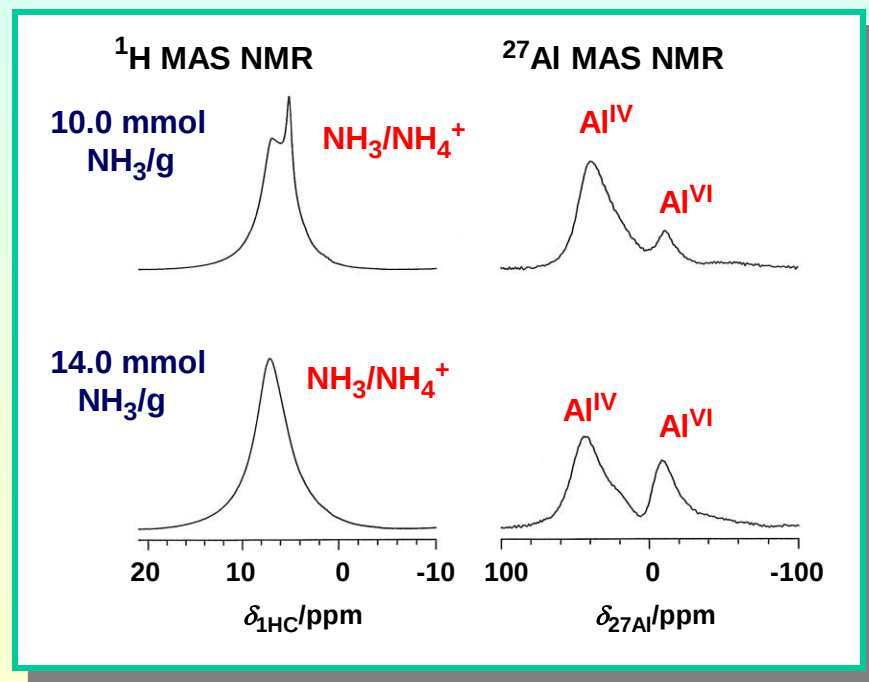
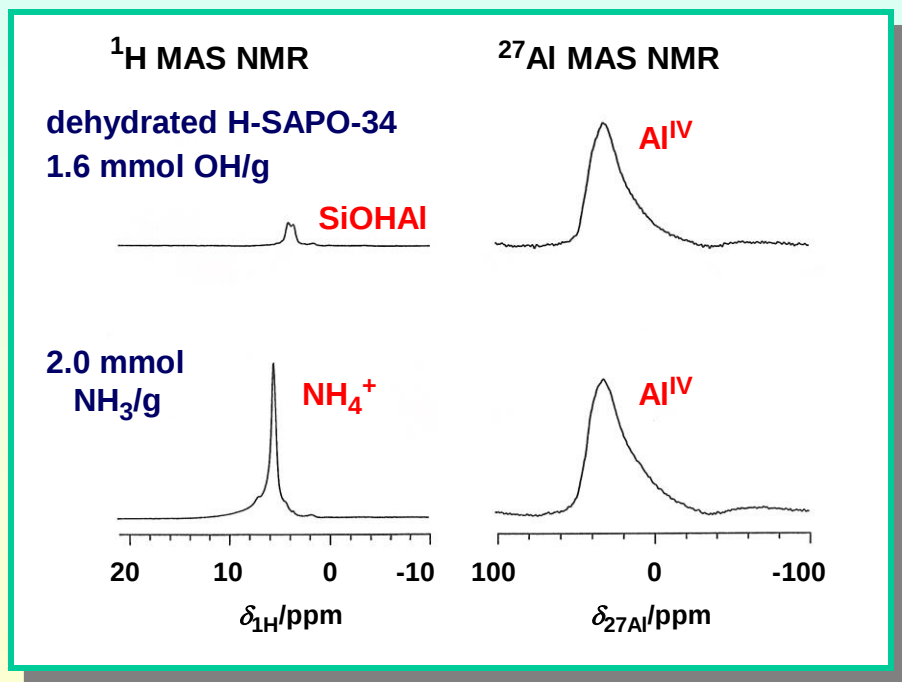


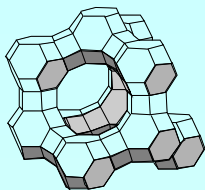
***Investigation of the catalyst framework and
of surface sites under in situ conditions***



Ammoniation of H-SAPO-34

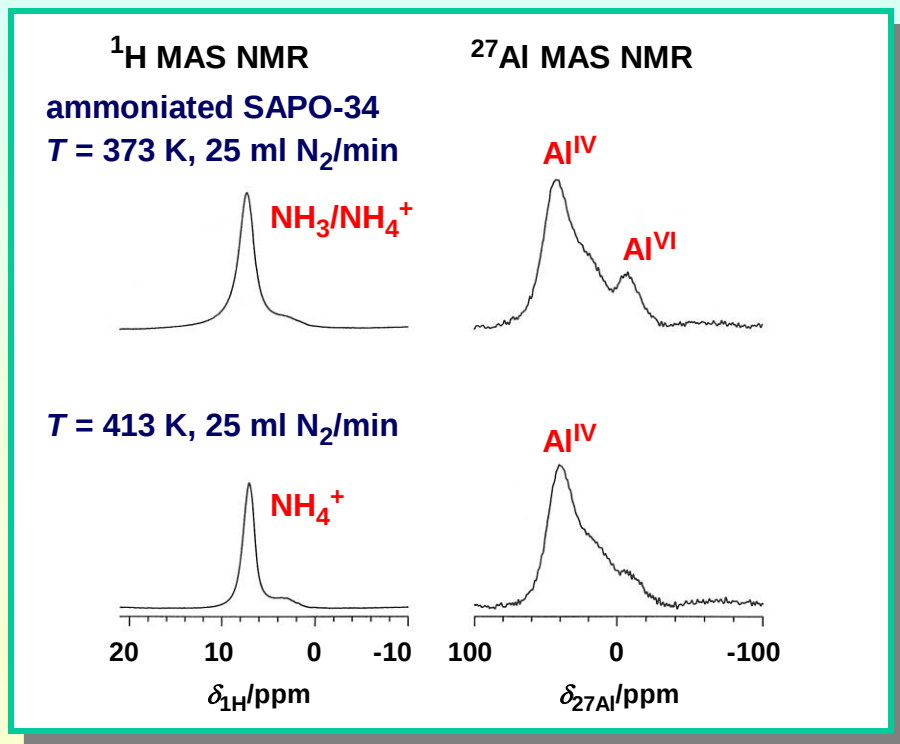
- stabilizing effect of ammonia on H-SAPO-34 (Mees et al., Chem. Commun. (2003) 44)



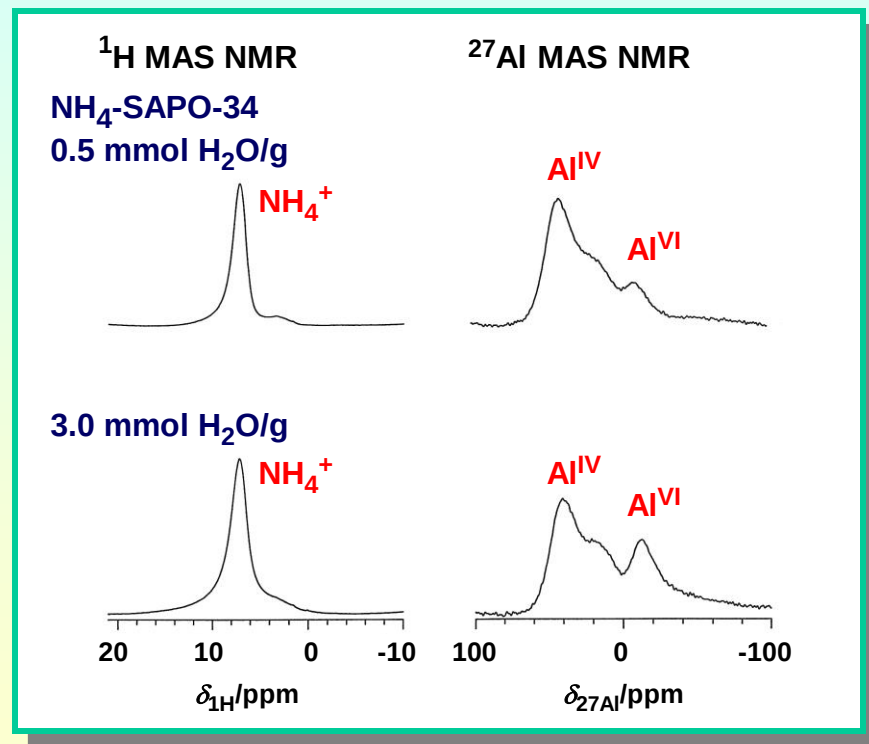


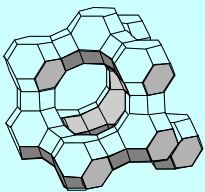
Ammoniation of H-SAPO-34

- reversibility of framework ammoniation

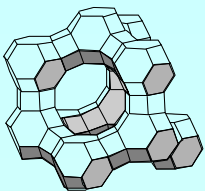


- influence on the hydration behavior



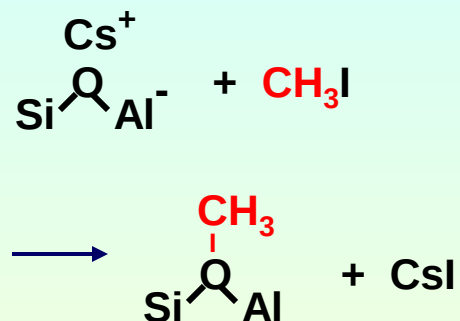


***Investigation of base sites and of reactions
catalyzed by basic zeolites***



Characterization of basic zeolites under reaction conditions

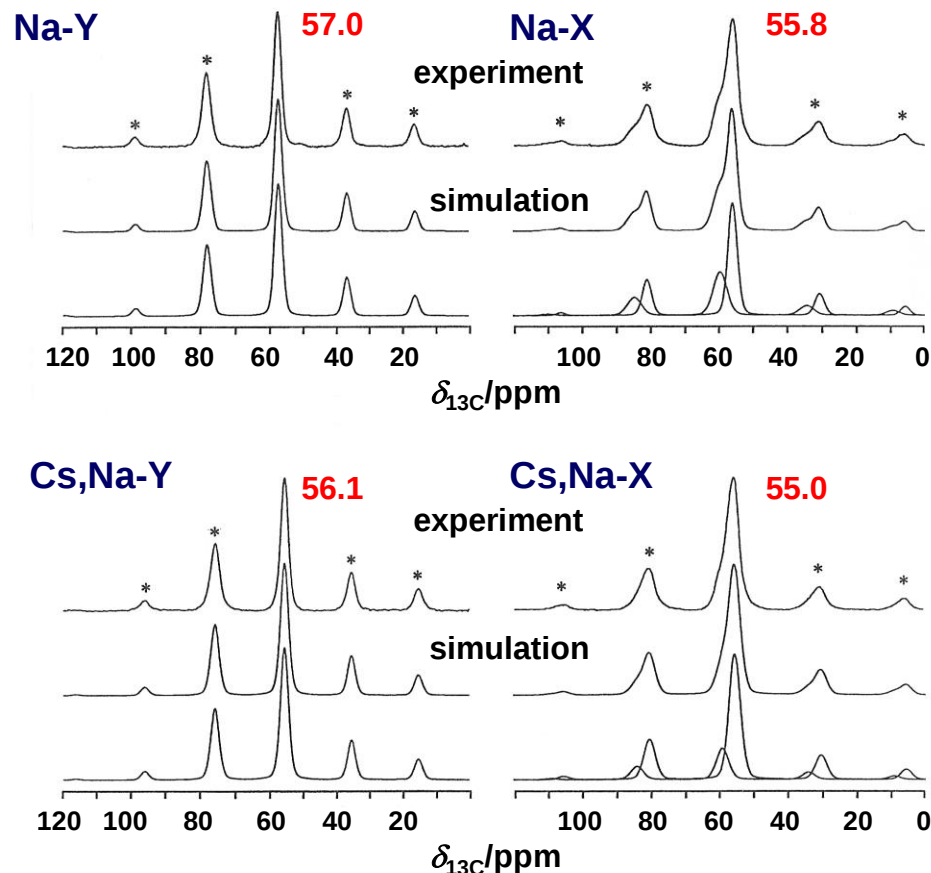
- conversion of CH_3I on basic zeolites:

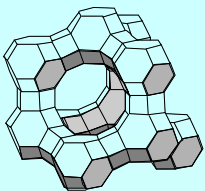


- ^{13}C MAS NMR spectroscopy of the surface methoxy groups formed under batch conditions:

→ signals at 54.3 to 59.2 ppm with a chemical shift anisotropy of ca. $\Delta\sigma = -40$ ppm

^{13}C MAS NMR spectroscopy



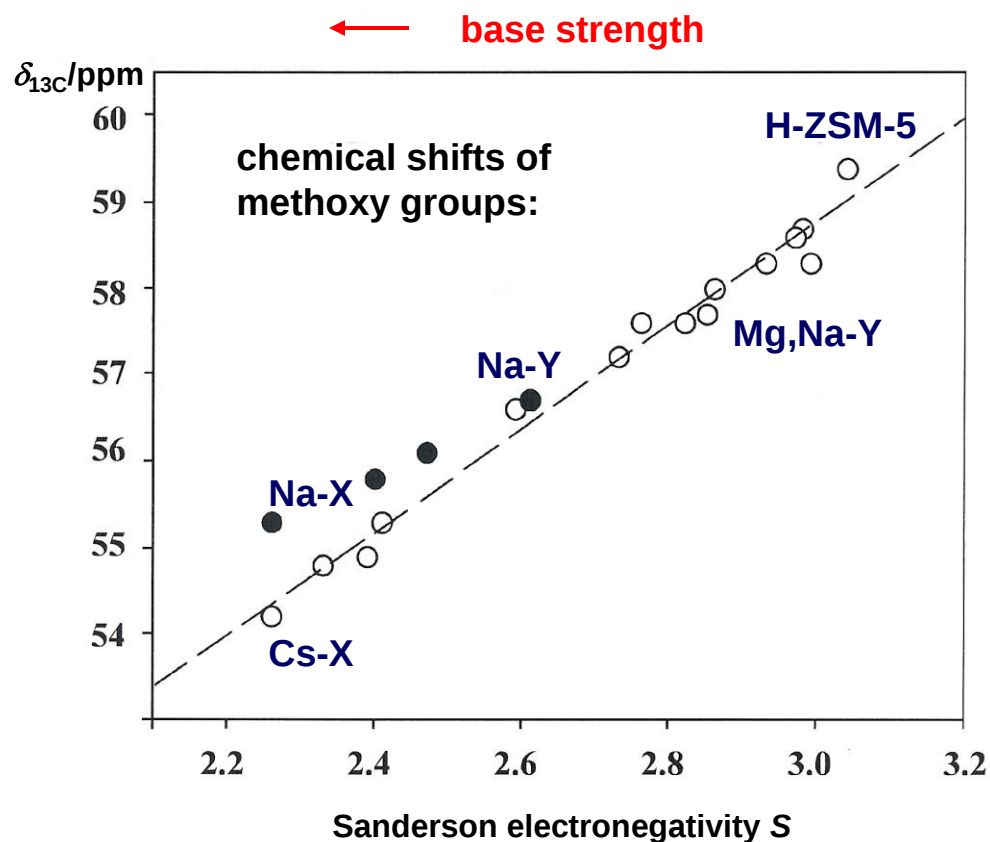


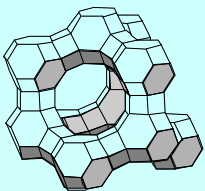
Characterization of basic zeolites under reaction conditions

- mean Sanderson electronegativity:

$$S = (S_{\text{Al}}^k S_{\text{Si}}^l S_{\text{O}}^m S_{\text{Me}}^n)^{1/(k+l+m+n)}$$

- decreasing ^{13}C NMR shift of surface methoxy groups with increasing base strength of the framework oxygen atoms

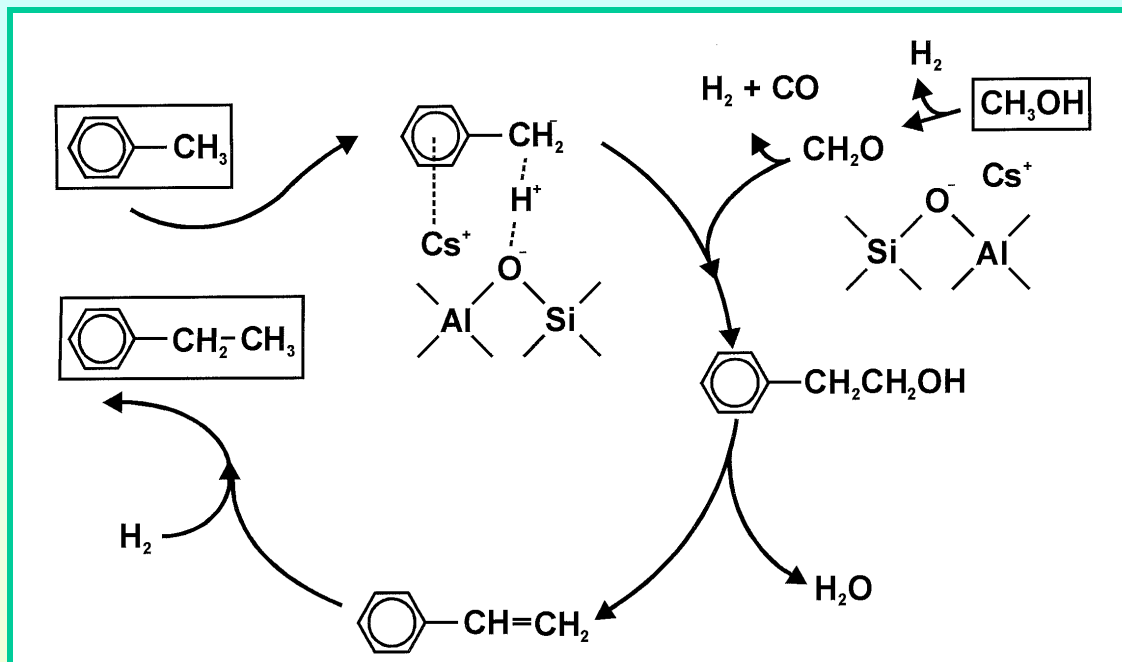




Side-chain alkylation of toluene with methanol on basic zeolites

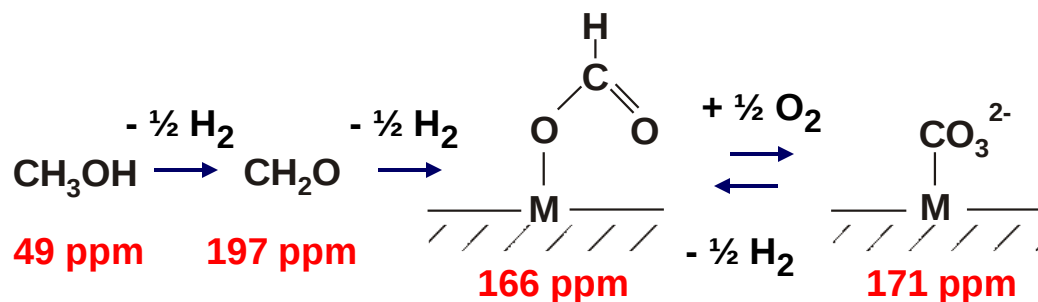
- reaction scheme proposed by Yashima et al. , J. Catal. 26 (1972) 303:

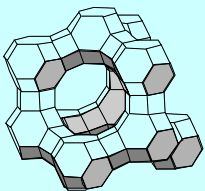
- activation of toluene by adsorption on the zeolite
- conversion of methanol to formaldehyde catalyzed by base sites



- proposed surface species:

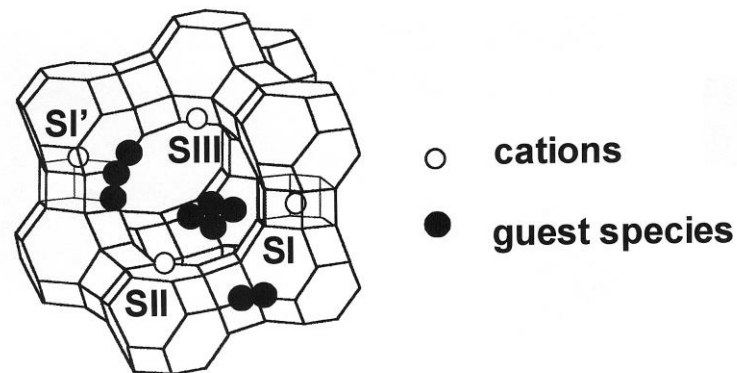
- formate ($\delta_{13C} = 166$ ppm)
- carbonate ($\delta_{13C} = 171$ ppm)





NMR characterization of the calcined zeolite CsOH/Cs,Na-X

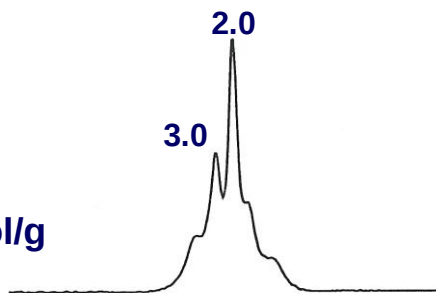
- zeolite Na-X ($n_{\text{Si}}/n_{\text{Al}} = 1.4$) exchanged with cesium cations (55 %) and impregnated with cesium hydroxide (24 CsOH/u.c.)



^1H MAS NMR

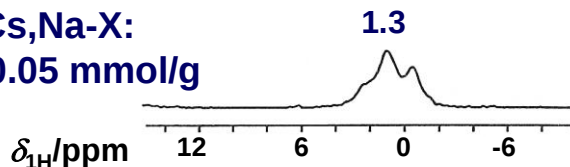
Cs,Na-X:

$c_{\text{OH}} = 0.3 \text{ mmol/g}$



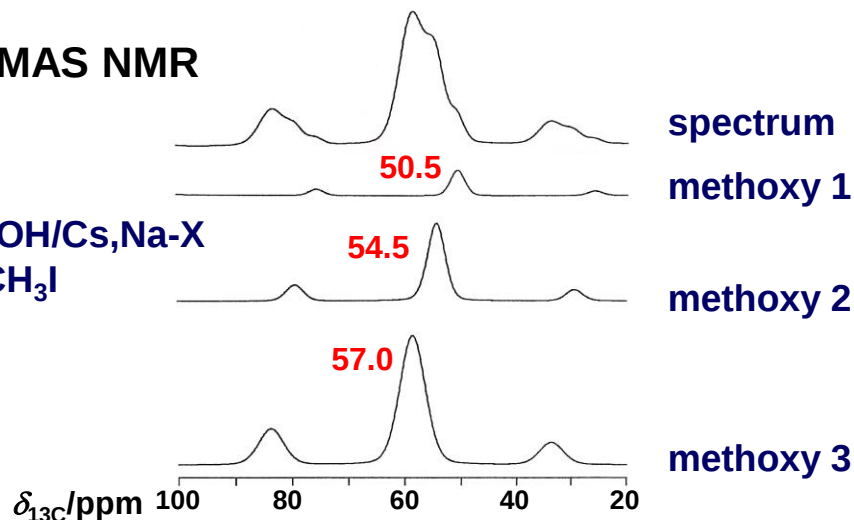
CsOH/Cs,Na-X:

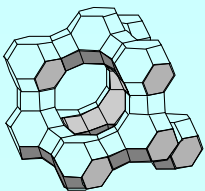
$c_{\text{OH}} = 0.05 \text{ mmol/g}$



^{13}C MAS NMR

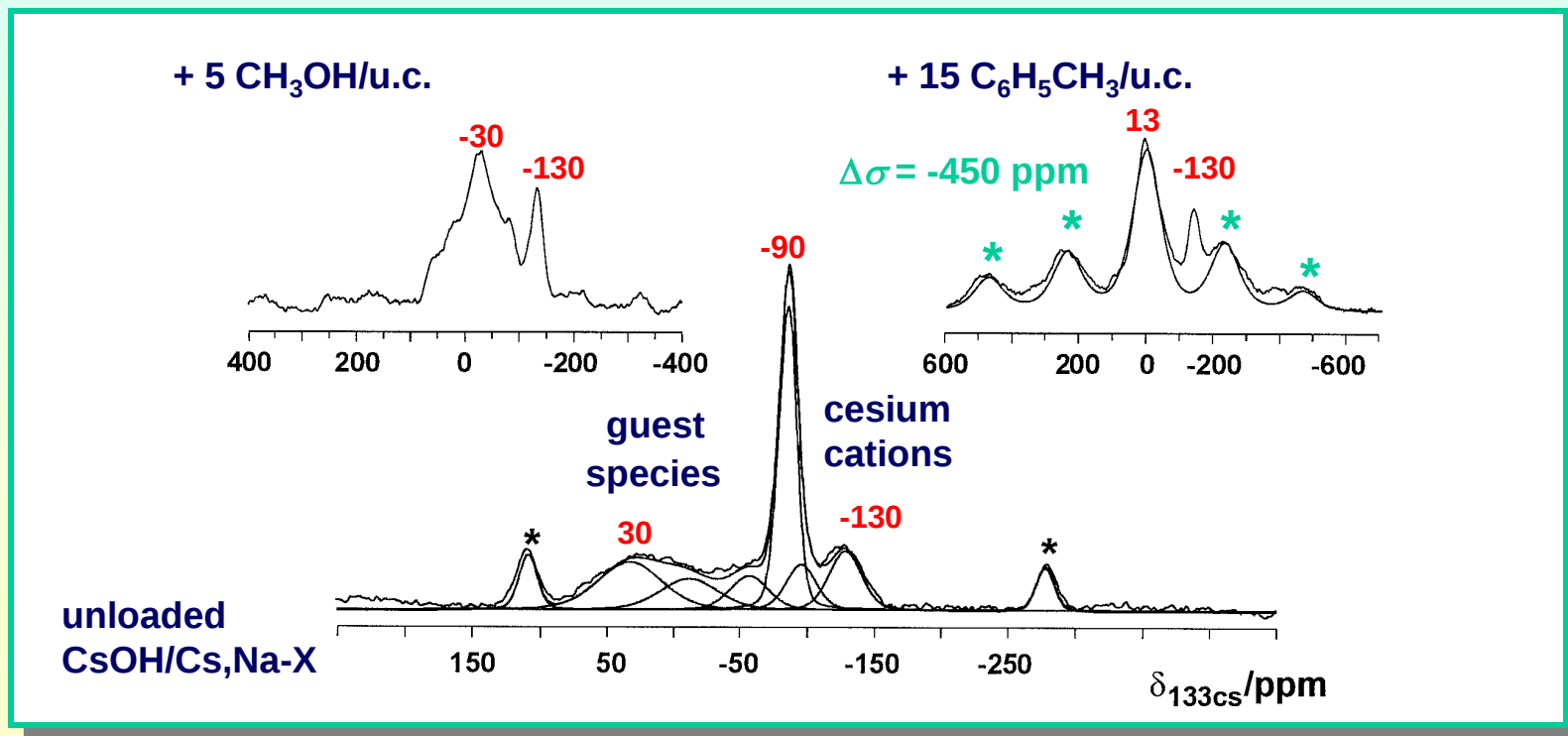
CsOH/Cs,Na-X
+ CH_3I

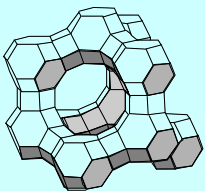




Adsorbate complexes formed by the reactants on zeolite CsOH/Cs,Na-X

- ^{133}Cs MAS NMR spectroscopy performed before and after adsorption of methanol and toluene



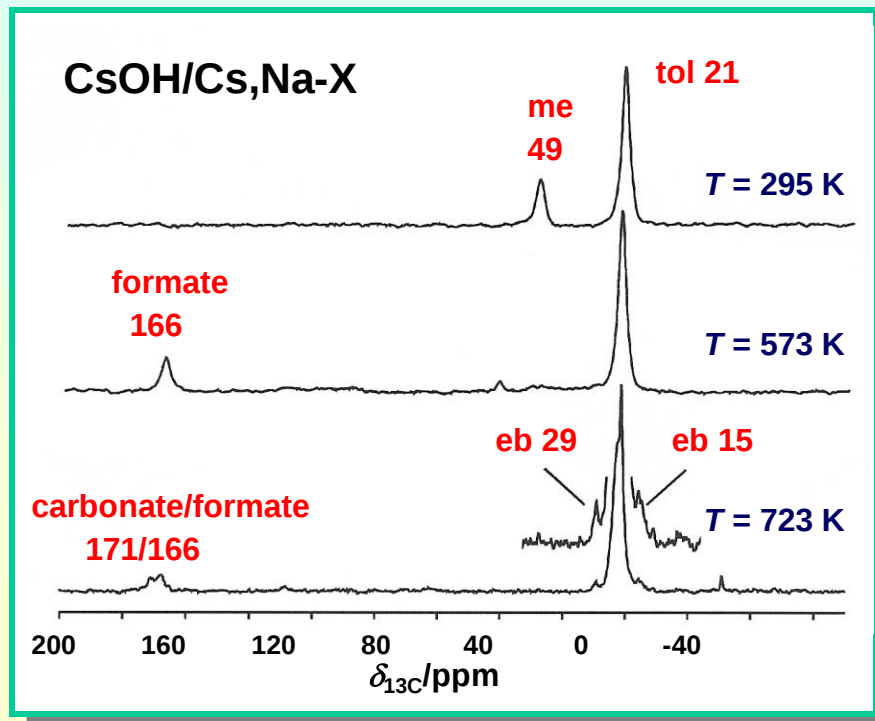
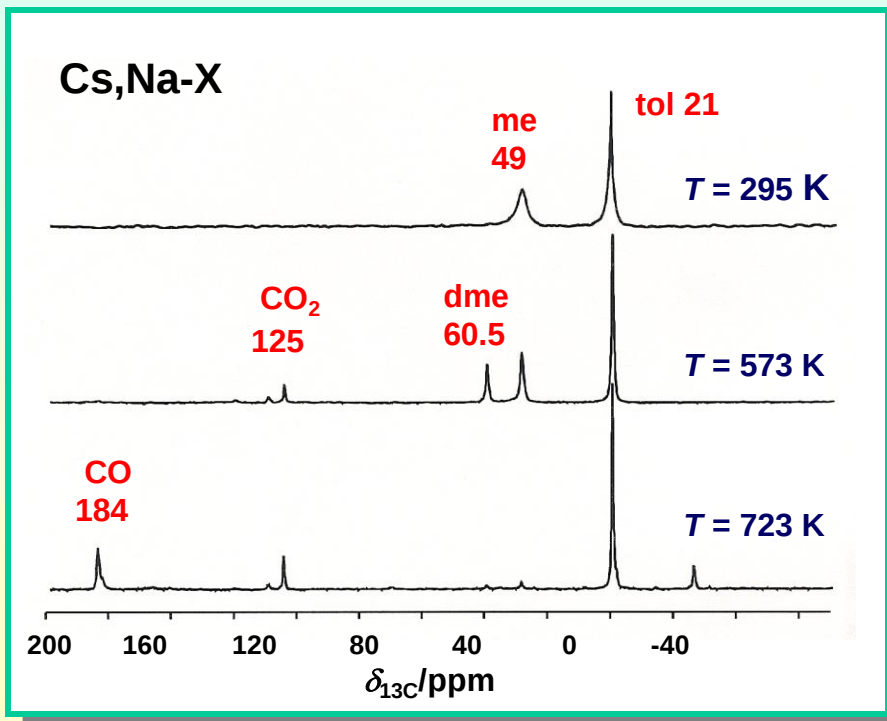


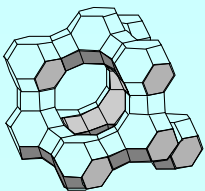
Side-chain alkylation of toluene on basic zeolites X under batch conditions

^{13}C MAS NMR spectroscopy:

15 $\text{C}_6\text{H}_5^{13}\text{CH}_3/\text{u.c.}$

5 $^{13}\text{CH}_3\text{OH}/\text{u.c.}$



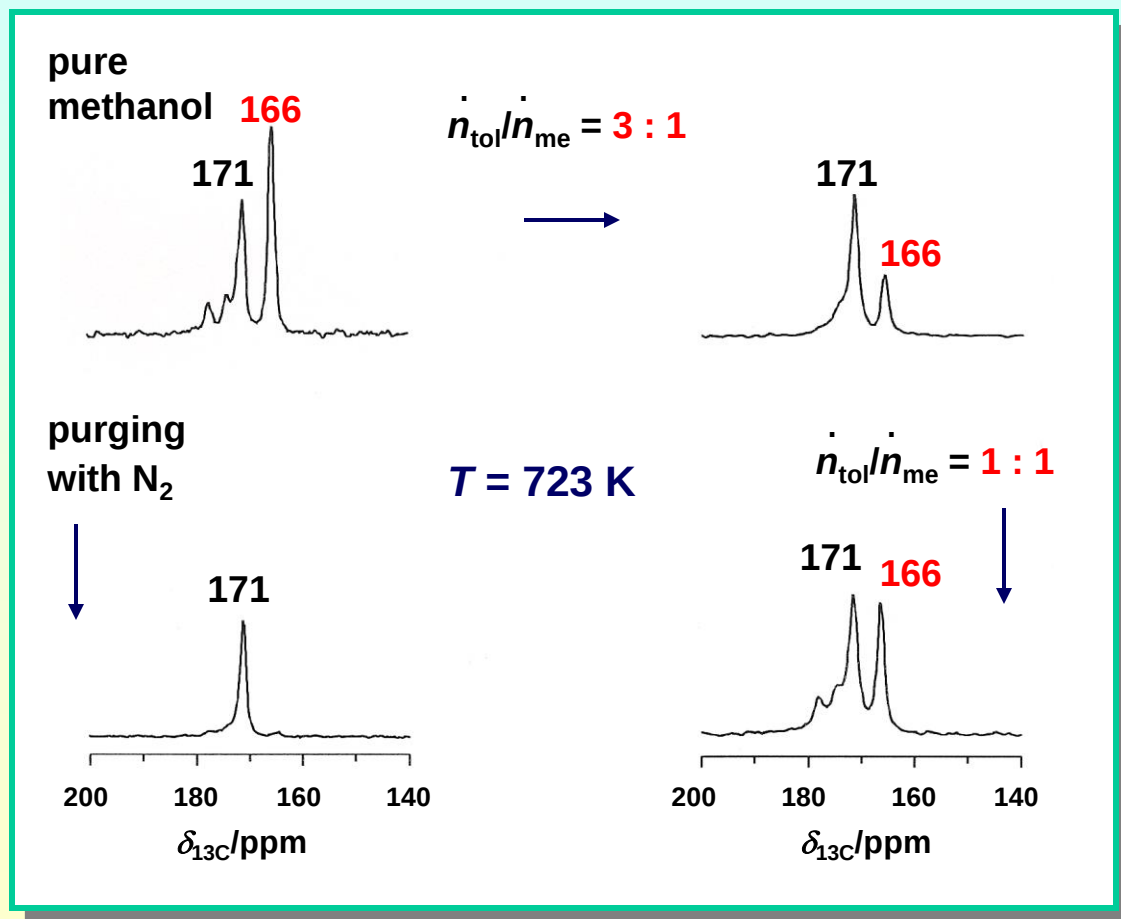


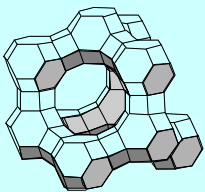
Reactivity of formate species on zeolite CsOH/Cs,Na-X under flow conditions

- *in situ* ^{13}C CF MAS NMR spectroscopy:

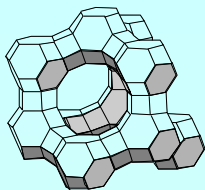
$$W_{\text{cat}}/F_{\text{me}} = 60 \text{ gh/mol}$$

- carbonate species are chemically stable
- formate species are consumed by toluene which indicates a high reactivity





***Investigation of reactions catalyzed
by acidic zeolites***



Investigation of reaction pathways by selectively labelled reactants

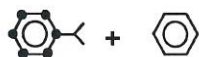
- isomerization of cumene to n-propylbenzene on zeolite H-ZSM-11 in the presence of benzene

experiment

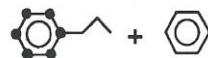
A:

B:

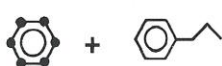
reactants



intramolecular
mechanism

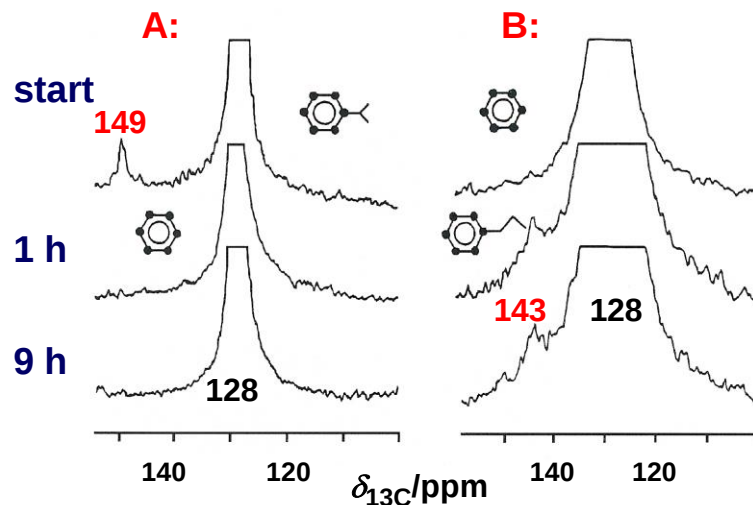


intermolecular
mechanism

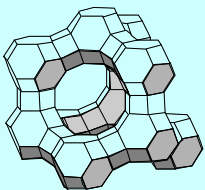


● : ^{13}C labelled carbon atoms

^{13}C MAS NMR at 473 K (batch)

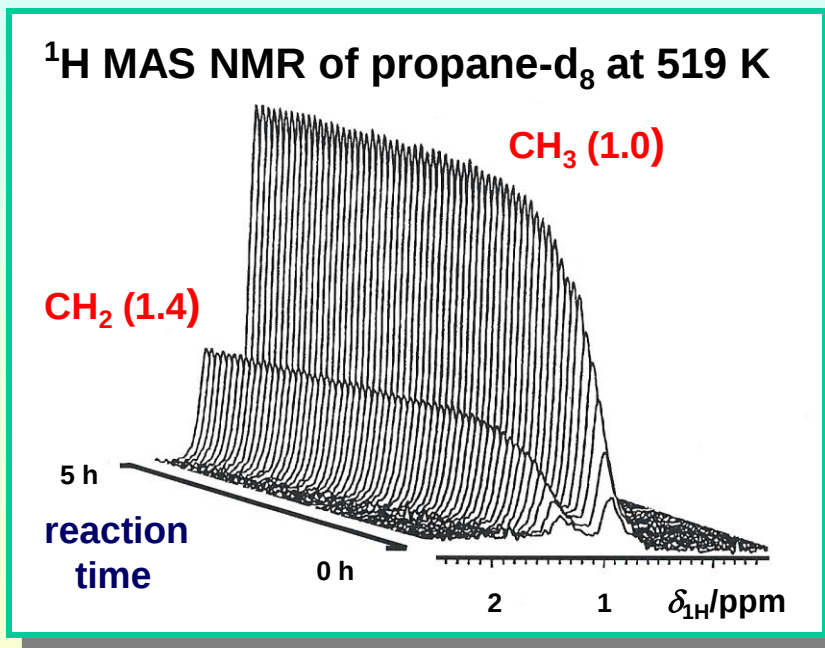


experiments **A** and **B** indicate an intermolecular reaction mechanism



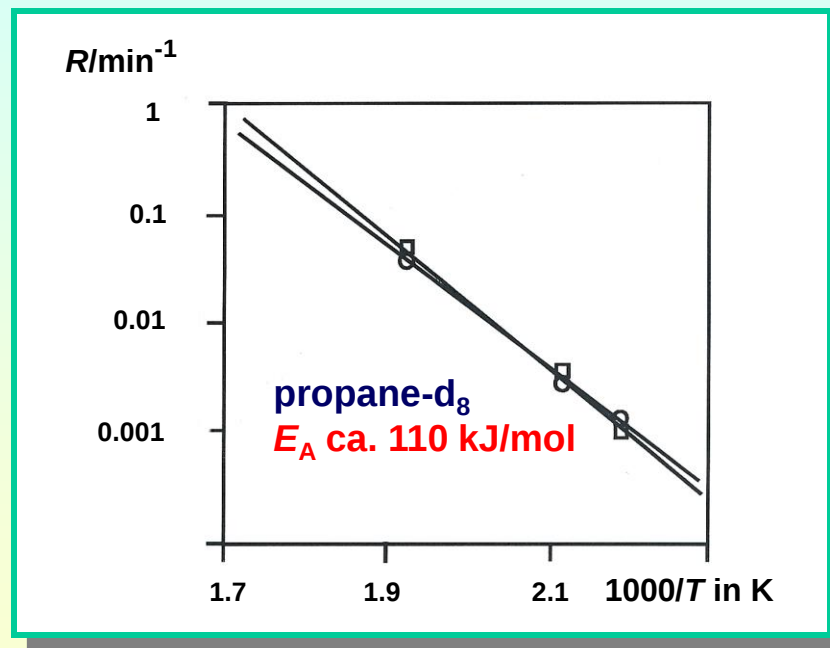
Evaluation of reaction mechanisms by H/D exchange on acidic zeolites

- H/D exchange of propane-d₈ (A) and isobutane-d₁₀ (B) with SiOHAl groups on H-ZSM-5



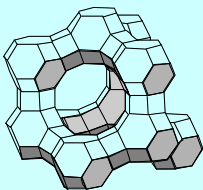
A:

- no regiospecific H/D exchange
 - E_A of ca. 110 kJ/mol
- no formation carbenium ions



B:

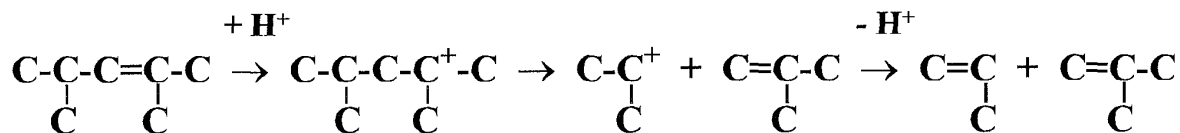
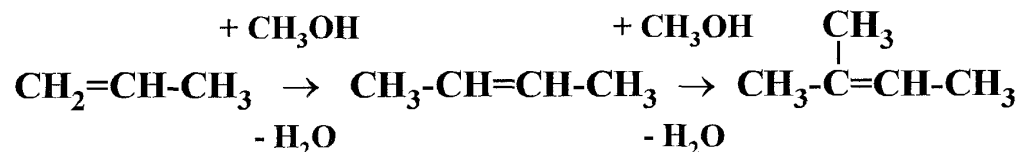
- regiospecific H/D exchange
 - E_A of ca. 50 kJ/mol
- formation carbenium ions

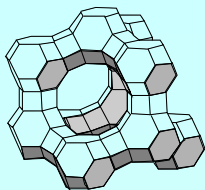


Methanol to olefin (MTO) conversion on acidic zeolites

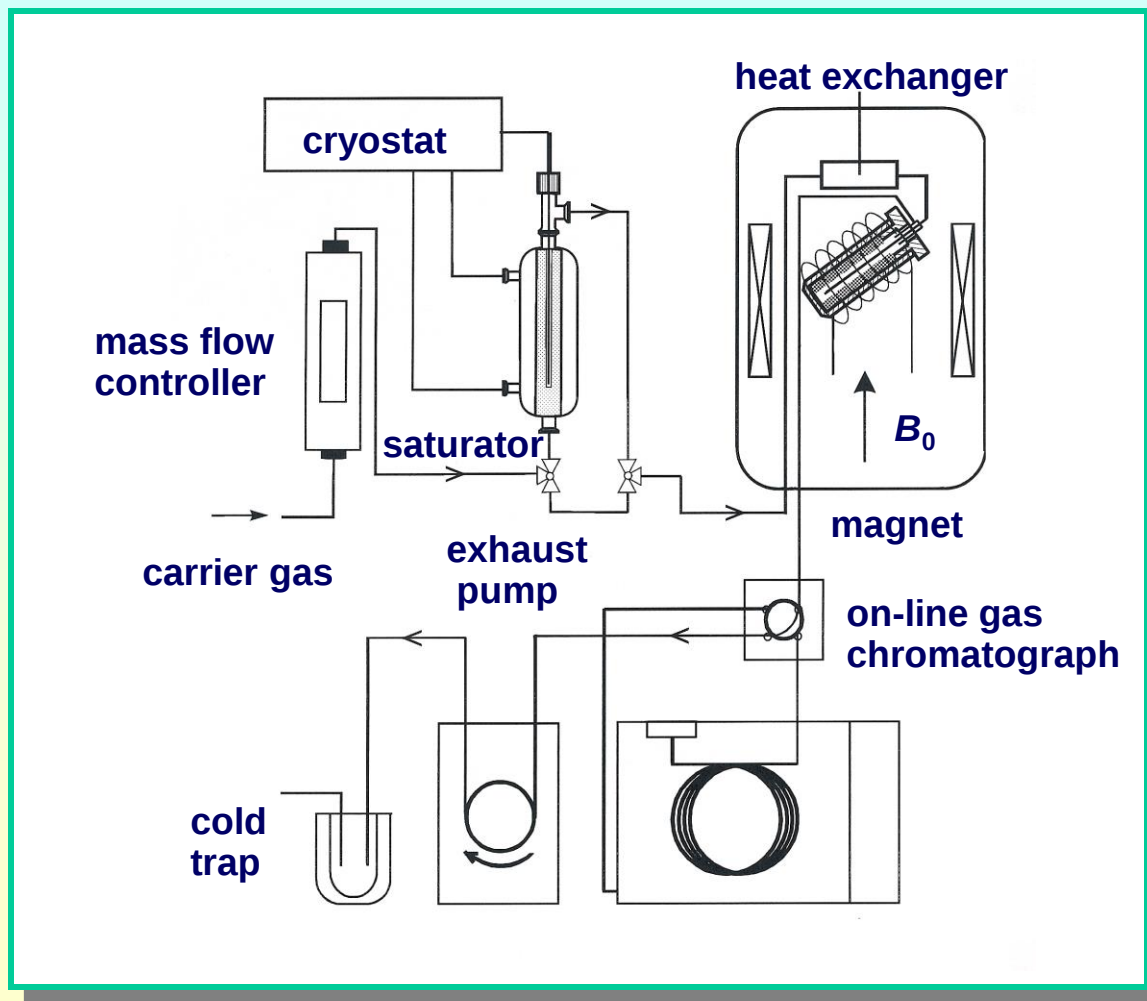
reaction mechanisms proposed in the literature:

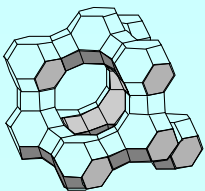
- carbene mechanism (Swabb and Gates)
- oxonium ylide mechanism (Berg and Olah)
- carbon-pool mechanism (Dessau, Hoelderich)





Coupling of in situ CF MAS NMR and on-line gas chromatography

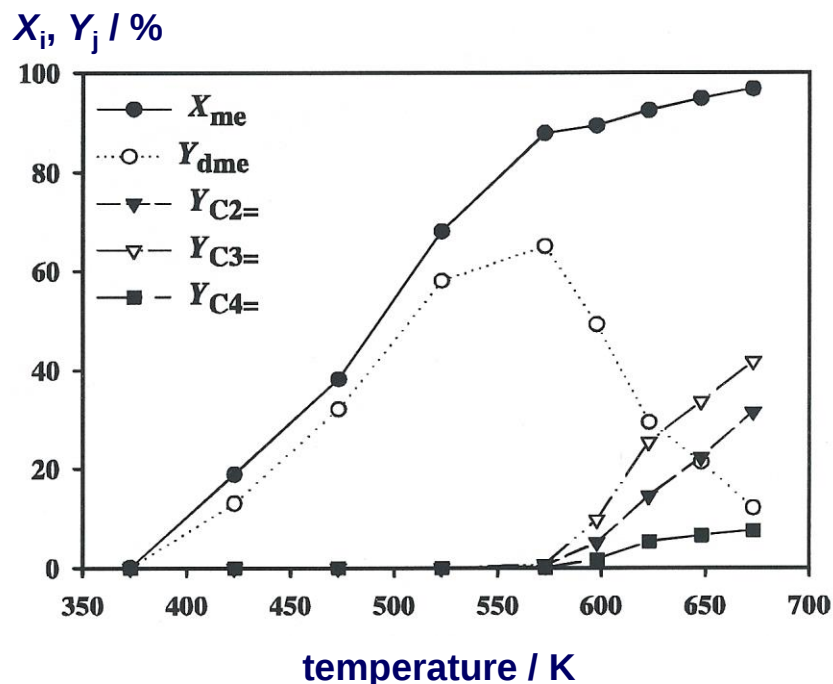




Conversion of methanol on H-ZSM-5 in a fixed-bed and in an MAS NMR rotor reactor

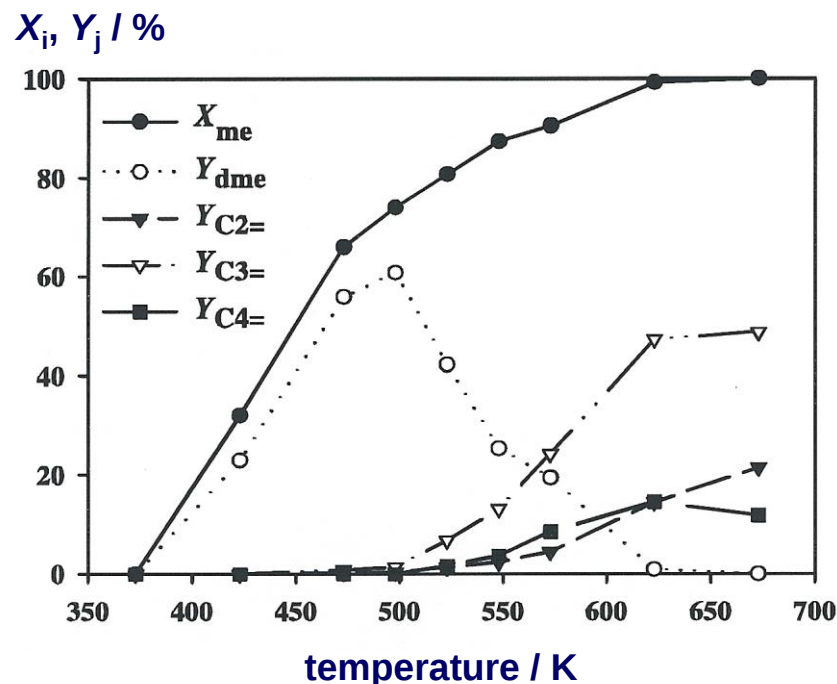
fixed-bed reactor

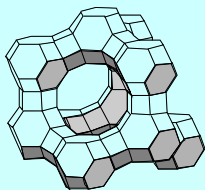
$W_{\text{cat}}/F_{\text{me}} = 25 \text{ gh/mol}$



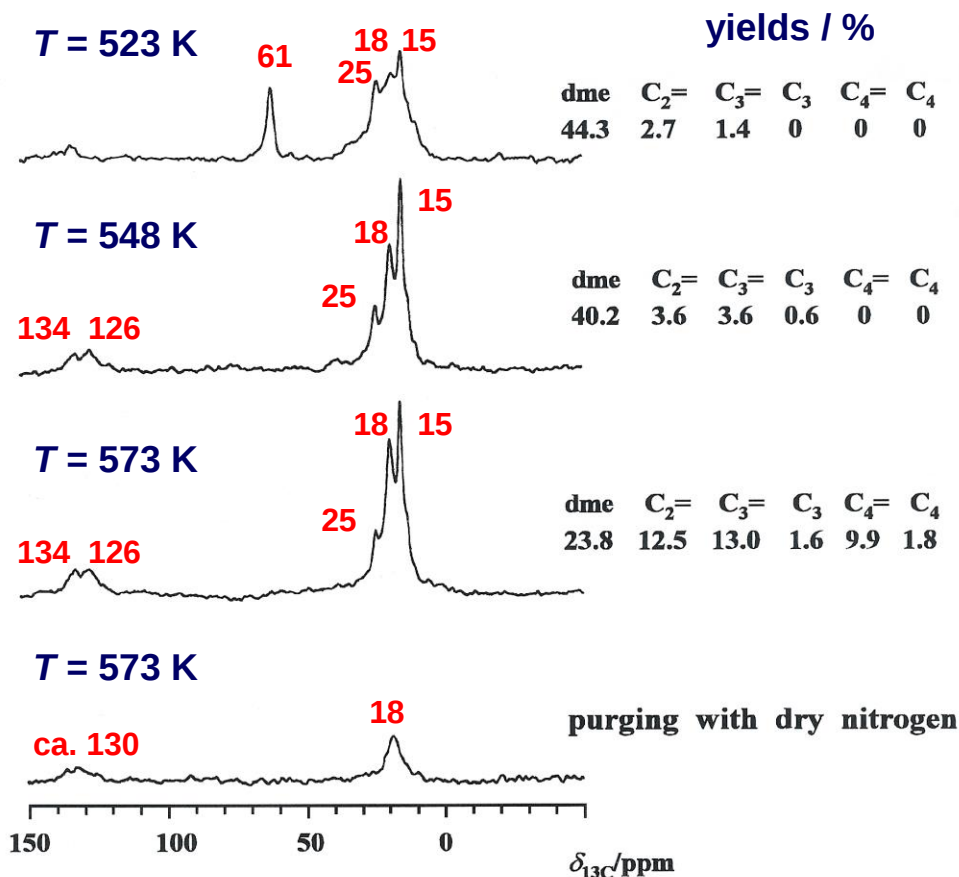
spinning (2 kHz) MAS NMR rotor reactor

$W_{\text{cat}}/F_{\text{me}} = 25 \text{ gh/mol}$





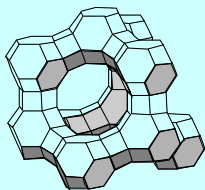
Conversion of methanol on H-ZSM-5 studied by in situ ^{13}C CF MAS NMR



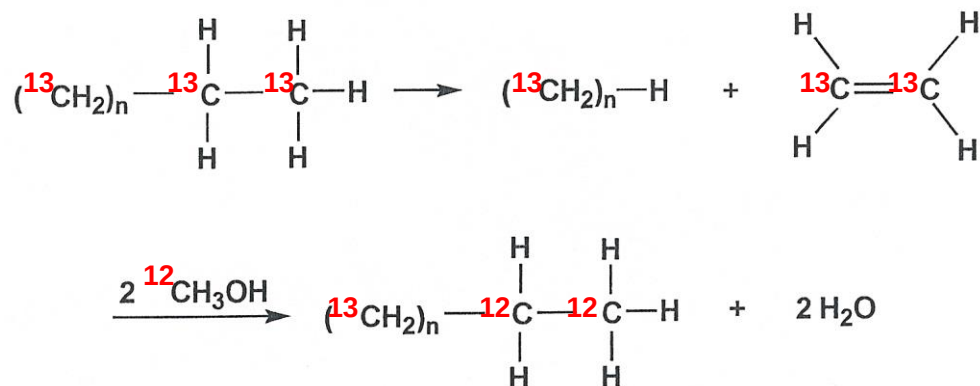
- aliphatic intermediates, e.g.:
 3-hexene (14.4, 25.9, 131.2 ppm)
 2,3-hexadiene (17.5, 126.2, 132.5 ppm)

- olefin pool with carbon numbers of $n > 6$
- aromatic adsorbates remaining after purging:
 benzene (128.6 ppm)

 hexamethylbenzene (17.6, 132.1 ppm)



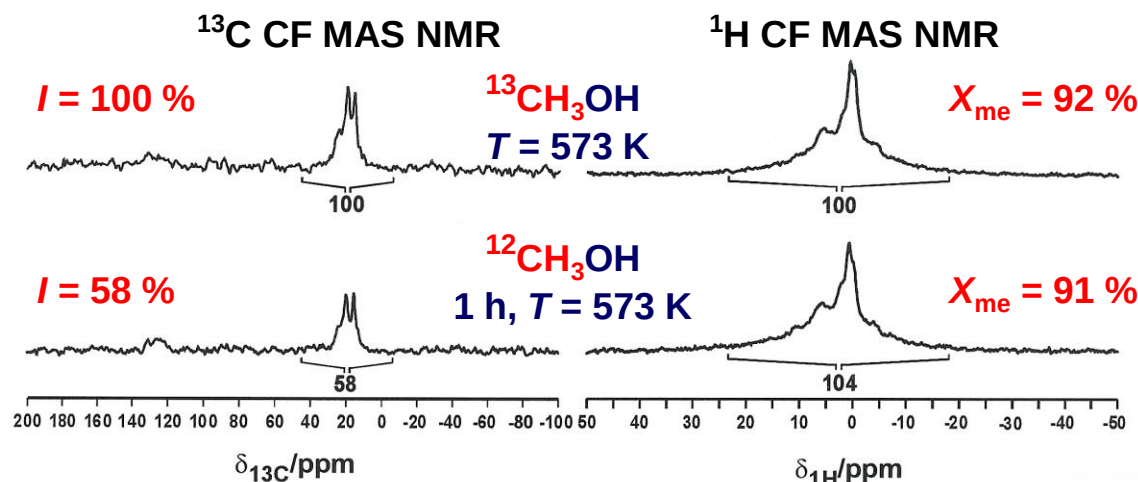
Role of the carbon pool in the MTO process on H-ZSM-5

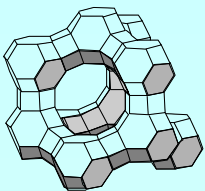


switching of the reactant flow induces a decrease of the ^{13}C -isotopes in the alkyl groups:

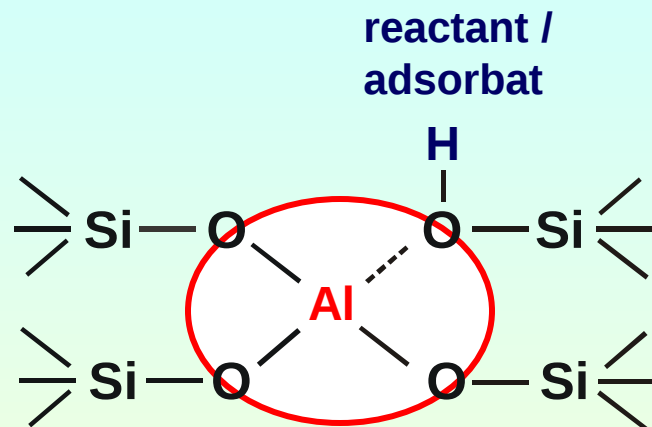
→ alkyl groups are involved in the formation of olefins

→ carbon pool plays an active role in the MTO process





State of SiOHAl groups in H-ZSM-5 during the MTO process



- electric field gradient :

$$V_{zz} = eq$$

- quadrupole coupling constant:

$$QCC = \frac{e^2qQ}{h}$$

²⁷Al spin-echo NMR experiments

purging with N₂
T = 295 K

QCC = 16 MHz

1 CH₃OH / SiOHAl
T = 295 K

QCC = 4.4 MHz

purging with N₂
T = 573 K

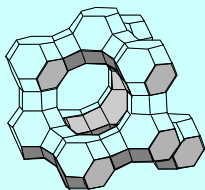
QCC = 12 MHz

1 CH₃OCH₃ / SiOHAl
T = 295 K

QCC = 11 MHz

1500 500 0 -500 -1500
 δ_{27Al}/ppm

1500 500 0 -500 -1500
 δ_{27Al}/ppm

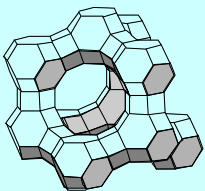


NMR parameters of ^{27}Al nuclei during the MTO process

reactant / adsorbate	QCC	$\Delta \nu_{1/2}^{\text{MAS}*}$
calcined H-ZSM-5	16 MHz	36 kHz / 350 ppm
methoxy/H-ZSM-5	13 MHz	25 kHz / 235 ppm
1 $\text{CH}_3\text{OCH}_3/\text{SiOHAl}$	11 MHz	17 kHz / 165 ppm
1 $\text{CH}_3\text{OH}/\text{SiOHAl}$	4.4 MHz	2.8 kHz / 26.5 ppm
n $\text{H}_2\text{O}/\text{H-ZSM-5}$	2.0 MHz	0.6 kHz / 5.5 ppm

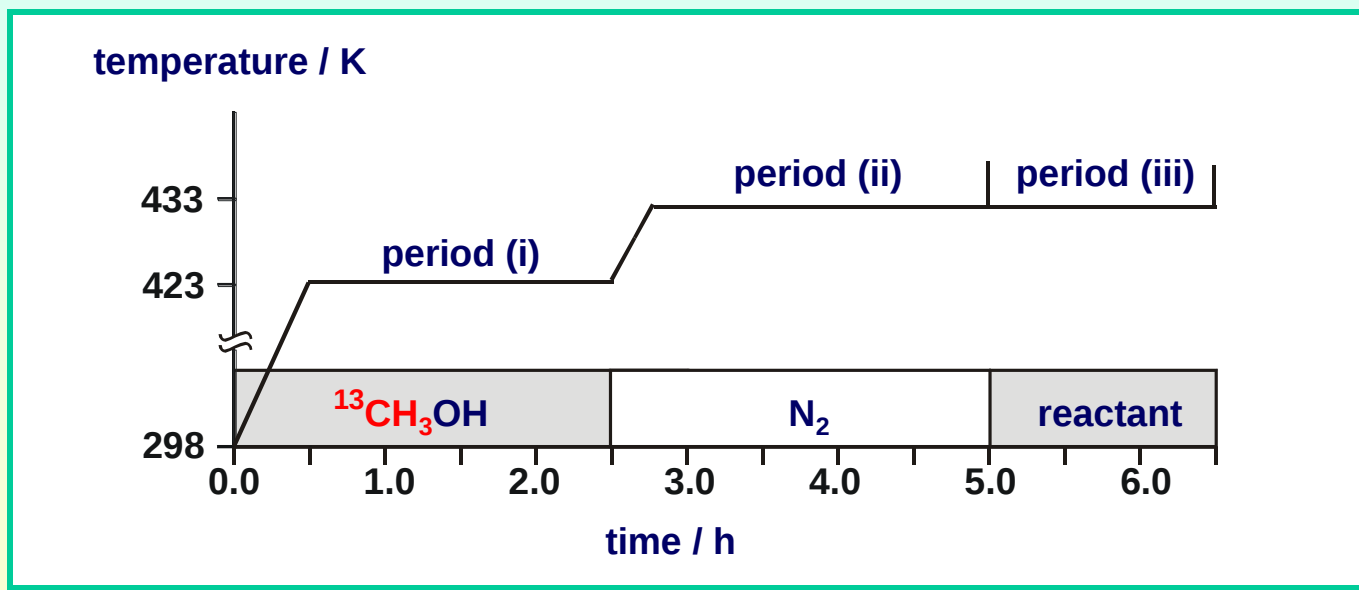
*: $B_0 = 9.4 \text{ T}$

→ absence of narrow ^{27}Al MAS NMR signals indicates that no adsorption of CH_3OH and H_2O occurs at SiOHAl groups under reaction conditions

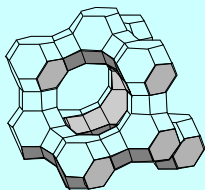


Study of surface methoxy groups by in situ SF (stopped-flow) MAS NMR

- selective preparation of adsorbate complexes by purging the volatile reactants in period (ii)

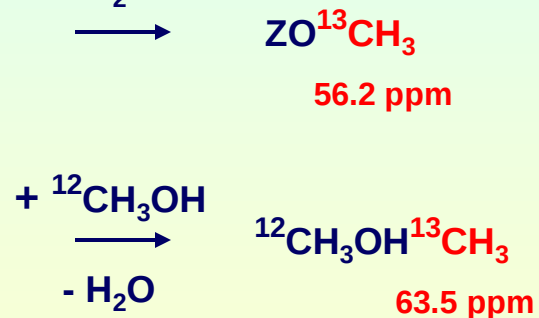
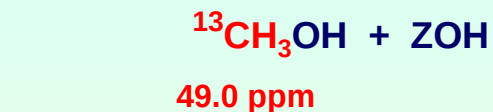
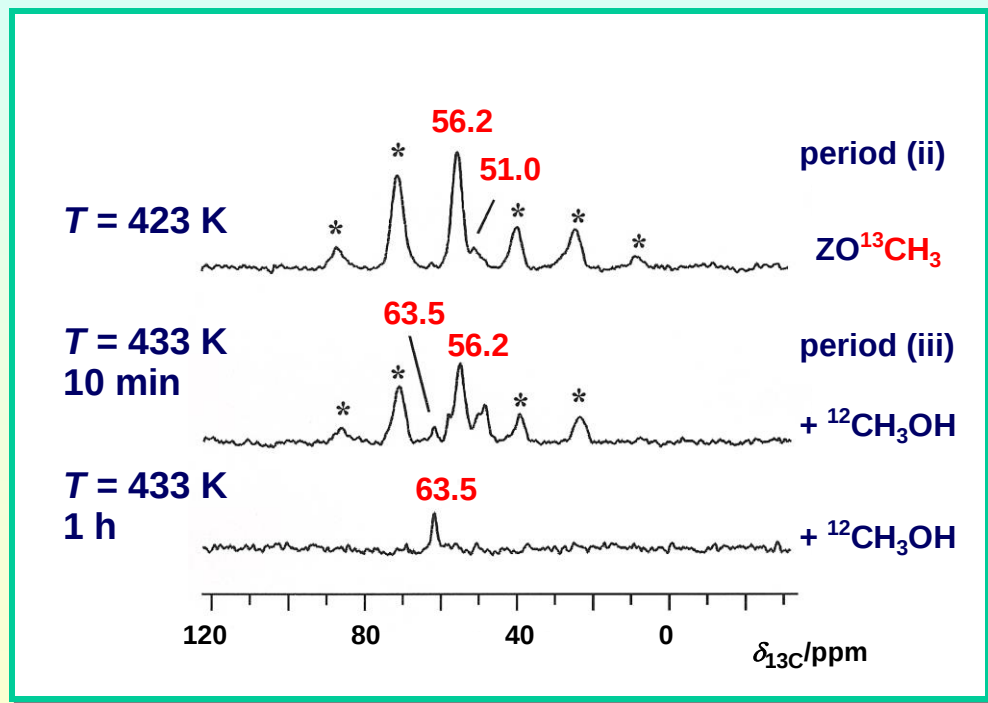


investigation of the reactivity of intermediates

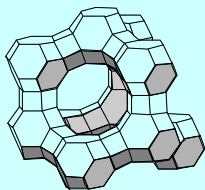


Reaction of methoxy groups with methanol on acidic zeolites

- ^{13}C SF MAS NMR investigation of methoxy groups on zeolite H-Y

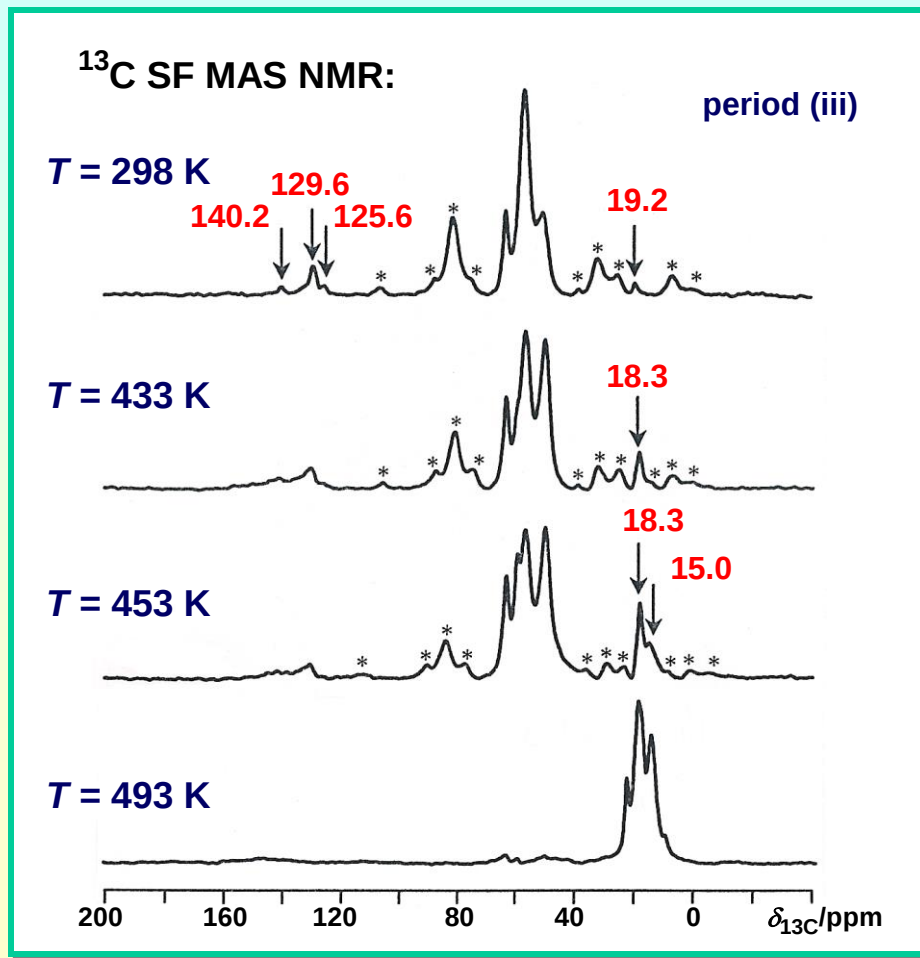


→ ^{13}C -labelled methoxy groups contribute to the formation of dimethyl ether



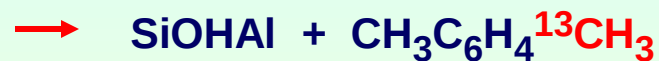
Methylation of aromatics by surface methoxy groups

- reaction of methoxy groups with toluene on zeolite H-Y



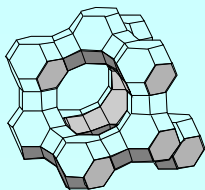
56.2 ppm

toluene



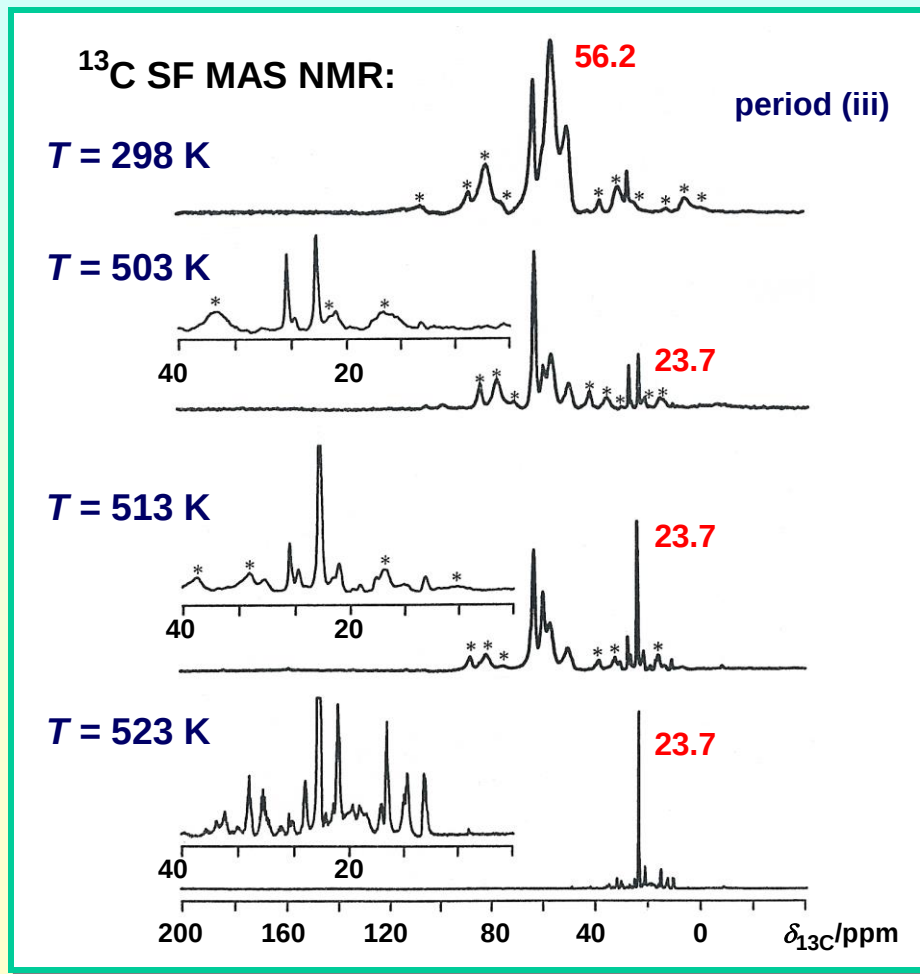
18.3 ppm

- methylation of aromatics by surface methoxy groups starts at $T = 433 \text{ K}$

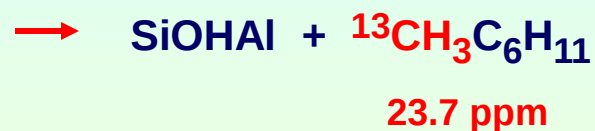


Methylation of alkanes by surface methoxy groups

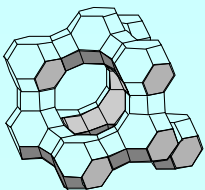
- reaction of methoxy groups with cyclohexane on zeolite H-Y



56.2 ppm cyclohexane

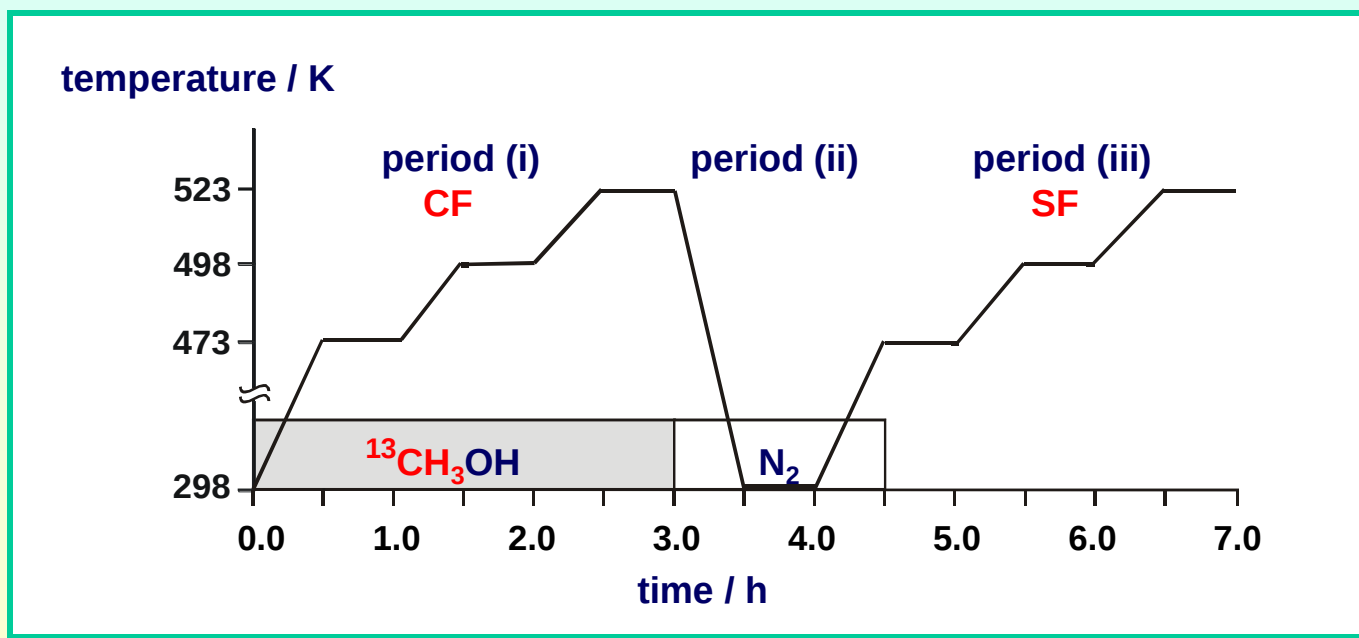


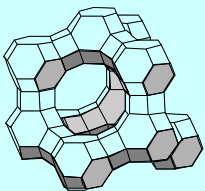
- methylation of alkanes by surface methoxy groups starts at $T = 503 \text{ K}$
- intermediates of ylide or carbene nature



Initiation of the MTO process by surface methoxy groups on acidic zeolites

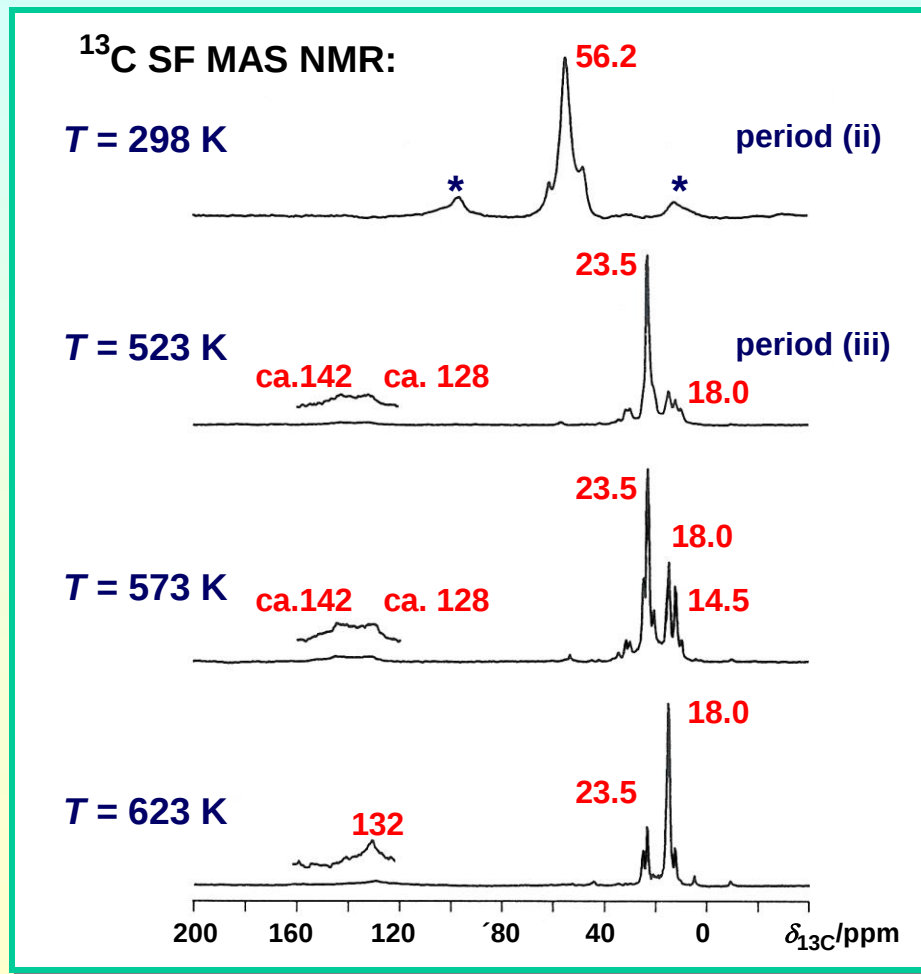
- reaction of pure methoxy groups on zeolite H-Y at elevated temperatures





Initiation of the MTO process by surface methoxy groups on acidic zeolites

- stopped-flow conversion of methoxy groups on zeolite H-Y



- initiation of the hydrocarbon formation at $T = 523\text{ K}$

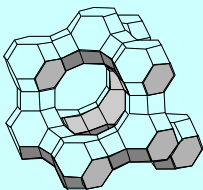
- formation of aliphatics:

→ isobutane (23.3, 24.6 ppm)
 isobutene (23.7, 119.5, 141.4 ppm)
 dimethylbutadiene (20.1, 111.3, 142.1 ppm)

and aromatic compounds:

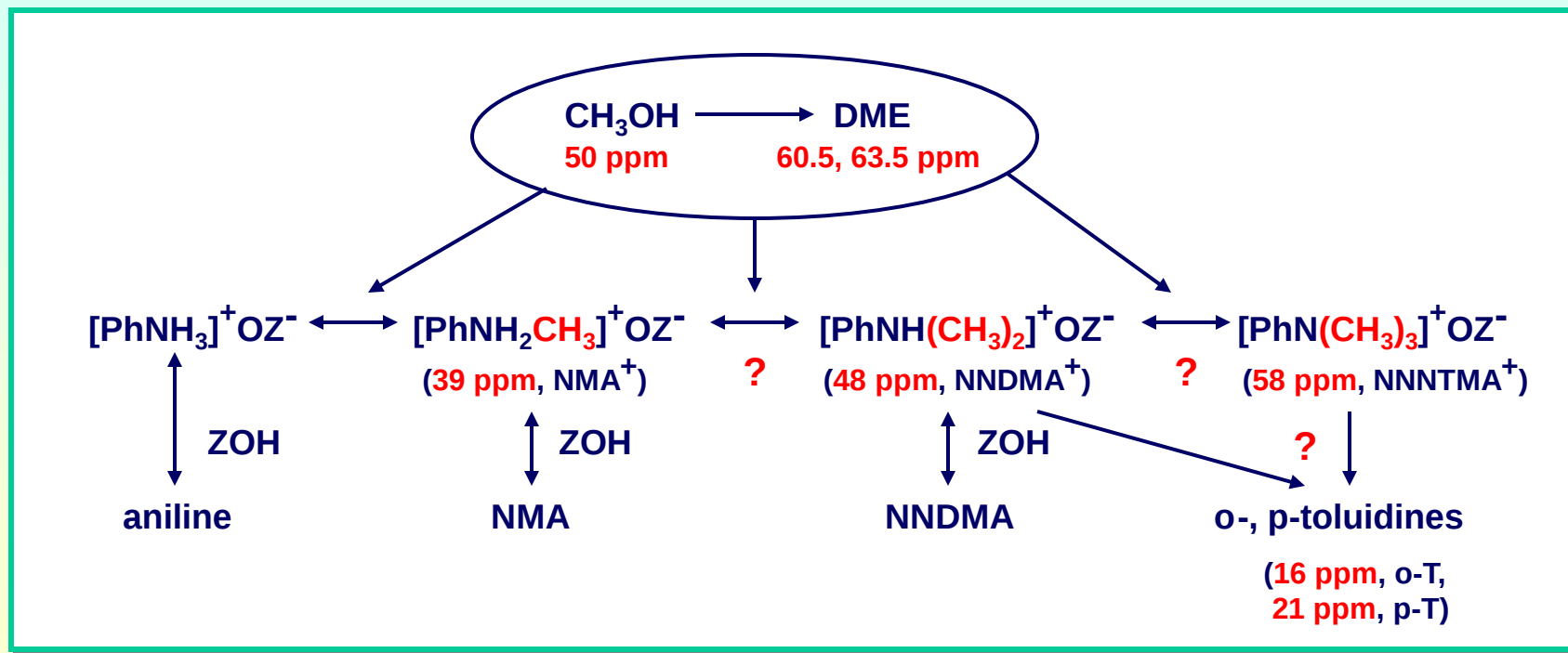
→ benzene (128.6 ppm)

 hexamethylbenzene (17.6, 132.1 ppm)

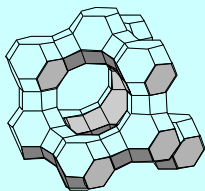


Methylation of anilin by methanol on acidic zeolites

- protonation of methylated anilines by strong acid sites (SiOHAl) in zeolite H-Y

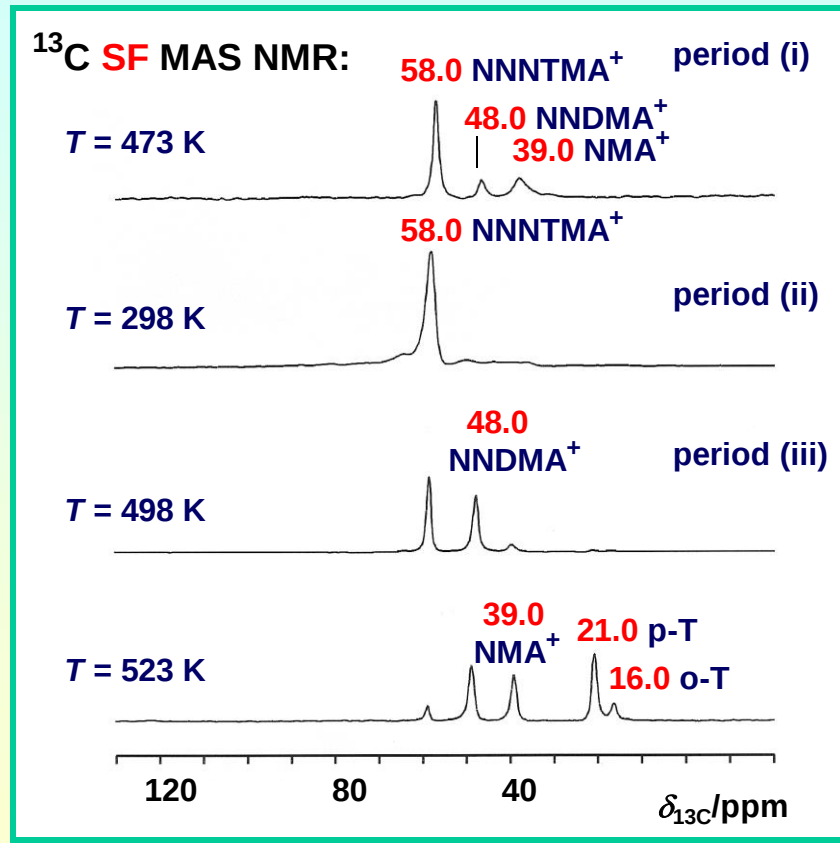
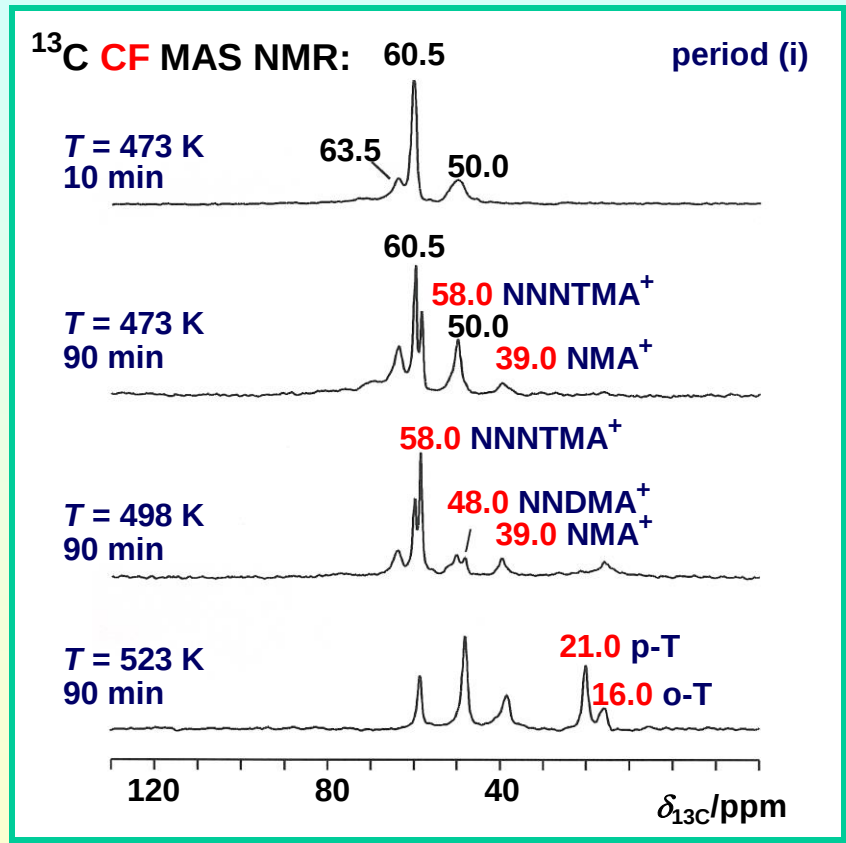


→ are the N,N,N-trimethylanilinium cations non-reactive spectators ?

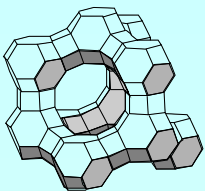


Reactivity of anilinium cations on zeolite H-Y

$W_{\text{cat}}/F_{\text{me}} = 40 \text{ gh/mol}$, $^{13}\text{CH}_3\text{OH} / \text{aniline} = 2 : 1$



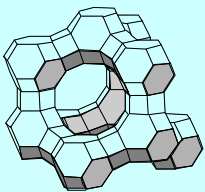
all reaction products can be formed by a decomposition of NNNTMA⁺ → chemical equilibrium



Summary I

applications of *in situ* NMR spectroscopy in zeolite catalysis:

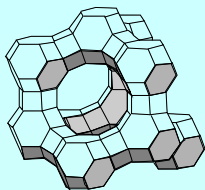
- **chemical behavior and local structure of active sites under reaction conditions**
- **origin of the catalyst deactivation under steady state conditions**
- **reaction pathways using labelled reactants**
- **activation energies of reaction steps**
- **reactivity of surface complexes and intermediates formed under reaction conditions**



Summary II

further developments in the field of *in situ* NMR spectroscopy:

- increase of the temperature range up to 1023 K
- application of modern solid-state NMR techniques such as MQMAS
- significant enhancement of signal intensities by a continuous injection of Laser-polarized ^{129}Xe into CF MAS NMR probes
- improvement of the time-resolution of *in situ* NMR investigations by an introduction of pulsed-flow experiments
- combination of NMR spectroscopy with other spectroscopic techniques such as UV-Vis



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Hannover**

Max-Buchner-Forschungsstiftung

**Fonds der Chemischen
Industrie**